# Polysulphate: A New EOR Additive To Maximize The Oil Recovery From Carbonate Reservoirs At High Temperature

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### **RESERVOIR CHEMISTRY**

Reservoirs consist of pore systems with Mineral surfaces, Brine, and Crude Oil.



Classical reservoir engineering:

• Limited knowledge .....if any

- ✓ Improved understanding of Reservoirs are needed
- ✓ Crude oil Brine Rock (CoBR) integrations controls:
  - Initial Reservoir wettability
  - Wettability in core restoration
  - Wettability alterations by «Smart Water»
  - Fluid flow in heterogeneous reservoirs
  - Scaling





#### Formation Water ≠ Injection Water



### SEAWATER (SW) AS A «SMART WATER» IN CARBONATES:





### INTRODUCTION

EOR by modified water injection:

- Injection water ≠ Formation water
- Chemical equilibrium between crude oil, brine and rock must be disturbed.
- Smart Water is an injection brine with modified ionic composition.
  - No expensive chemicals are added
  - Environmentally friendly
  - Composition is dependent on reservoir mineralogy
  - Causes wettability alteration and improved sweep
- In carbonate/chalk seawater is a Smart Water





### SMART WATER EOR IN CHALK



- ➢ Low SI with FW (VBOS):
- ➢ Higher SI with SW:
- Improved SI with SW0Na:
- Highest SI with SW0Na4S:

initial wetting is mixed/slightly water wetSW behaves as a «Smart Water» inducing wettability alterationSmarter water compared to SWMost efficient brine for wettability alteration







- Both Gulf seawater (GSW) and modified Gulf seawater (GSW0Na) behave as «Smart Water»:
  - Significant improved recovery compared to formation water
  - Modified GSW gave 52 % extra oil after FW

Smart Wate EOR Group

### EFFECT OF SULFATE ON SMART WATER



- $\succ$  SO<sub>4</sub><sup>2-</sup> in SW has a dramatic effect on oil recovery
- $\blacktriangleright$  «Smart Water» EOR effect is catalyzed by SO<sub>4</sub><sup>2-</sup>



### EFFECT OF CALCIUM ON SMART WATER



- 5 equally restored outcrop chalk cores
  - S<sub>wi</sub> = 0 % FW
  - Crude oil and aging
- Oil recovery by spontaneous imbibition 70 °C
  - Modified SW with increasing Ca<sup>2+</sup> concentration Note that SO<sub>4</sub><sup>2-</sup> is present in all brines





Ca<sup>2+</sup> in SW has a significant effect on oil recovery by spontaneous imbibition

Model proposed by Zhang and Austad, University of Stavanger, 2006:



- Chemical interaction between surface active ions at the rock surface
- Acidic polar organic components (carboxylates) need to be "unsticked"
- Wettability alteration is temperature dependent more efficient at higher temperatures



> Both  $Ca^{2+}$  and  $SO_4^{2-}$  are needed for wettability alteration

## **OBJECTIVE OF STUDY**

### SMART WATER PRODUCTION



- Expensive / Technical challenging
- Retentate/Reject:
  - High salinity
  - High conc. of sulfate
  - Reduced conc. of Mg and Ca
  - Sulphate will precipitate at high temperatures
- Needs for making cheap Smart Water
  - Easily preparable
  - No precipitate at higher temperatures.



- Polysulphate/Polyhalite is a naturally occurring salt  $(K_2Ca_2Mg(SO_4)_4 \cdot 2H_2O)$
- Deposited 260 million years ago during the Permian period ٠
- Can be mined near the North Yorkshire coast, UK ٠
- Dissolves easily in water with low residue ٠
- Provides the essential ions for inducing wettability alteration;  $SO_4^{2-}$  and  $Ca^{2+}$ ٠



EOR Group

Catio	ons	Anions		
Element	Atomic weight %	Element	Atomic weight %	
Sodium	9.3	Sulfur	85.4	
Magnesium	21.9	Chloride	14.6	
Aluminium	3.2			
Silica	3.3			
Potassium	25.5			
Calcium	36.9			

Can polysulphate be used as a water additive for EOR-purposes?

Can polysulphate be used to make Smart Water with potential for wettability alteration and enhanced oil recovery?





### MATERIALS AND METHODS

### Outcrop Stevns Klint chalk cores

Core		SK1	SK2	SK3	SK4	SK5	SK6	SK7	SK8	SK9
Length	(cm)	7.1	7.1	7.1	7.2	7.0	6.9	7.1	7.0	7.0
Diameter	(cm)	3.8	3.8	3.8	3.8	3.8	3.8	3.8	3.8	3.8
PV	(ml)	38.6	39.1	39.1	40.1	41.3	38.6	37.9	40.0	37.9
Porosity	(%)	48.6	48.6	48.8	49.2	49.3	49.2	47.4	50.2	47.2
Permeability	(mD)	4.1	4.7	3.8	3.8	4.1	4.7	3.8	3.8	4.0
BET	m²/g	2.0								
Used ir experime	n ent	SIFW @90°C	SISW @90°C	SIDW-PS @90°C	SISW-PS @90°C	SIFW @110°C	SISW @110°C	SIDW- PS@110°C	SISW- PS@110°C	CWT @25 & 90 °C
					·			·		



- Stevns Klint (SK) Outcrop chalk
  - Around 65 million years
  - The same chalk deposit as the North Sea chalk reservoirs
  - Analog to both Ekofisk and Valhall chalk reservoirs



• Heterogeneous pore size distribution



### BRINES

	FW	SW	DW-PS	SW-PS	DWoT	DW1T
Ions	(mM)	(mM)	(mM)	(mM)	(mM)	(mM)
Na <sup>+</sup>	997.0	450.1	6.3	466.2	6.3	6.3
K+	5.0	10.1	17.4	28.2	17.4	17.4
Li <sup>+</sup>	-	-	-	-	-	24.0
Ca+	29.0	13.0	15.2	29.6	15.2	15.2
$Mg^{2+}$	8.0	44.5	5.8	47.9	5.8	5.8
Cl-	1066.0	525.1	9.2	528.5	9.2	33.2
HCO <sub>3</sub> -	9.0	2.0	-	-	2.0	2.0
SO42-	0.0	24.0	31.5	55.9	-	31.5
TDS(g/L)	62.83	33.38	4.9	38.14	6.5	6.1
Density (g/cm <sup>3</sup> )	1.04	1.02	1.0	1.02	1.0	1.0
Bulk-pH	7.3	7.8	7.5	8.1	7.8	7.8

• Brines:

- FW - Formation water

- SW – Seawater

- DW – Distilled water

- Imbibition brines:

- FW

- SW

- SW-PS: 5000 mg/L polysulfate

- DW-PS: 5000 mg/L polysulfate

Surface reactivity by chromatography

Li<sup>+</sup> / SCN- as non-reactive tracers

- SO<sub>4</sub><sup>2-</sup> as surface reactive tracer

• Oil recovery by spontaneous imbibition

- 90 °C

- 110 °C

All cores equally restored for same initial wettability:

- 5 PV DW to remove dissolvable salts (Puntervold et al., 2007)
- S<sub>wi</sub> = 10 % FW by desiccator (Springer et al. 2003)
- 4 PV crude oil, AN ~0.58 mgKOH/g, 0.81 g/cm<sup>3</sup>, 2.4 cP
- Aging at 90 °C for 2 weeks





# RESULTS

### SURFACE REACTIVITY

![](_page_18_Figure_1.jpeg)

• Sulphate from polysulphate salt has affinity toward chalk mineral surfaces

• The affinity increases with an increase in temperature

![](_page_18_Picture_4.jpeg)

> Polysulphate reactivity toward chalk surfaces – promising for wettability alteration!

### POLYSULFATE BRINES AS SMART WATER AT 90°C

![](_page_19_Figure_1.jpeg)

- FW does not disturb chemical equilibrium
  - Baseline recovery without wettability alteration
- > Polysulfate added to the imbibition brine leads to increased oil mobilization

![](_page_19_Picture_5.jpeg)

• SW-PS > SW  $\approx$  DW-PS

### EFFECT OF POLYSULFATE AT 110°C

![](_page_20_Figure_1.jpeg)

- 4 similarly prepared chalk cores
- $S_{wi}$ = 10% with FW
- Exposed to 4 PV oil (AN = 0.58 mgKOH/g)
- Aged 2 weeks at 90°C
- Spontaneous imbibition at 110 °C
  - FW
  - SW
  - DW-PS
  - SW-PS

	FW	SW	DW-PS	SW-PS
Ions	(mM)	(mM)	(mM)	(mM)
Ca <sup>+</sup>	29.0	13.0	15.2	29.6
Mg <sup>2+</sup>	8.0	44.5	5.8	47.9
$SO_4^{2-}$	0.0	24.0	31.5	55.9

- FW does not alter wettability
- Sulphate in the imbibition brine leads to wettability alteration!
  - SW-PS  $\approx$  SW > DW-PS

![](_page_20_Picture_15.jpeg)

Imbibition fluid	OOIP % T = 90°C	$\Delta$ OOIP % related to FW T = 90°C	OOIP % T = 110°C	$\Delta \text{ OOIP \%}$ related to FW $T = 110^{\circ}C$
FW	22	-	31	-
SW	37	15	50	19
DW-PS	35	13	48	17
SW-PS	45	23	54	23

- Sulphate dissolved from polysulphate can react with the chalk minerals aiding wettability alteration.
- Increased oil mobilization was observed with brines containing sulphate.
- SW-PS was the most effective brine, thus effectiveness of SW can be further increased by adding PS.
- DW-PS was able to alter wettability similar to SW.

Onshore, where seawater is not readily available: Smart Water can be prepared by mixing polysulphate with surface water

In areas where produced water is required re-injected:

Polysulphate can be added to produced water and become Smart Water

![](_page_21_Picture_9.jpeg)

![](_page_22_Figure_1.jpeg)

#### Polysulphate as an additive to produced water for re-injection?

• Produced water is not a Smart Water in Chalk or Limestone

> ~20 %OOIP extra oil produced by adding polysulphate to produced water!

![](_page_22_Picture_5.jpeg)

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![](_page_23_Figure_2.jpeg)

![](_page_23_Picture_3.jpeg)

![](_page_24_Picture_0.jpeg)