

# EOR - Introduction

Arne Skauge

Centre for Integrated Petroleum Research

EOR fundamentals and toolbox

Force workshop 6-7 Nov 2013

## **Structure of presentation**

EOR basics

EOR experience North Sea reservoirs

Gas injection EOR

Waterflood EOR

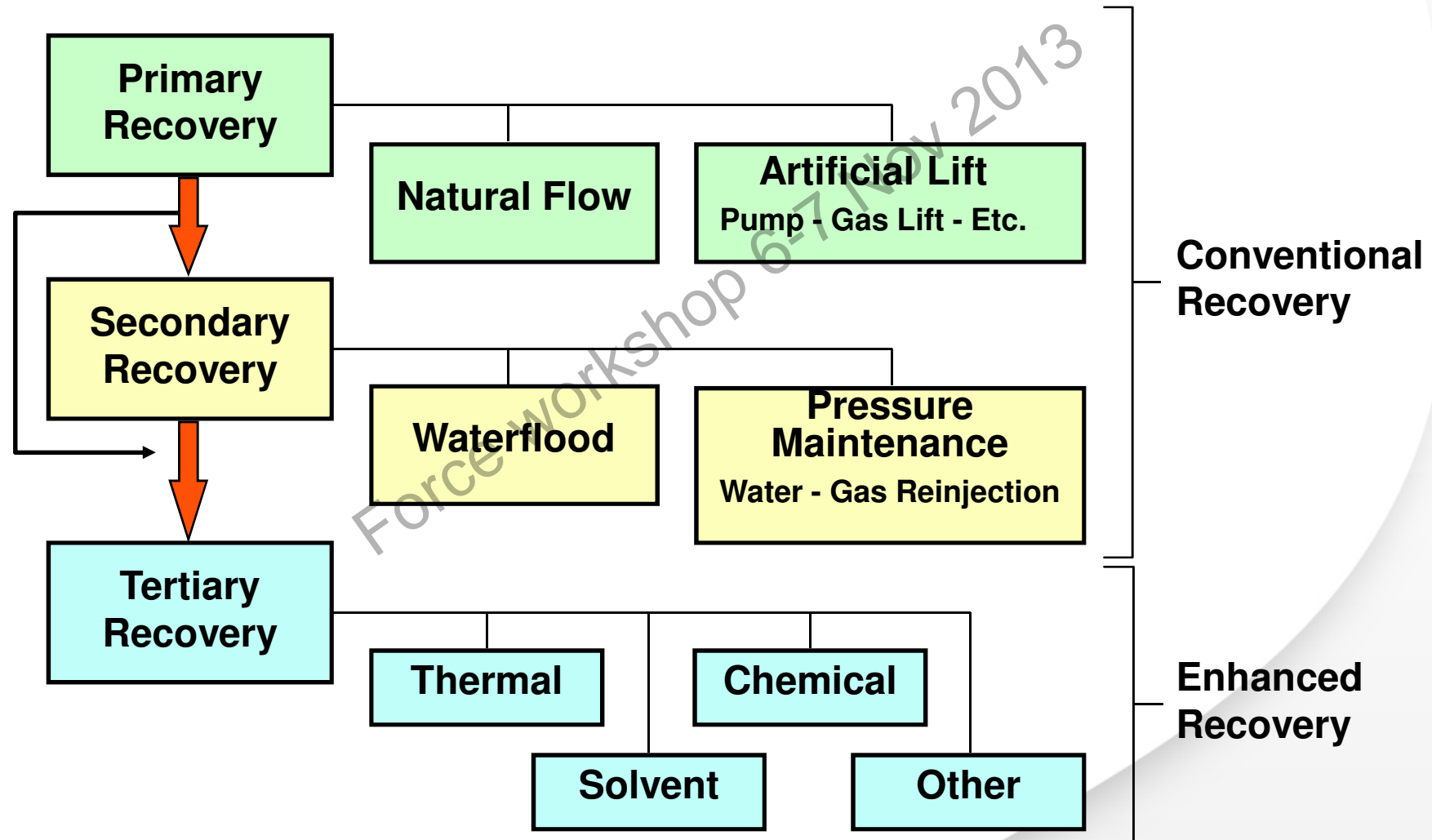
Way forward

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# EOR basics



# Recovery Mechanisms (conventional view)

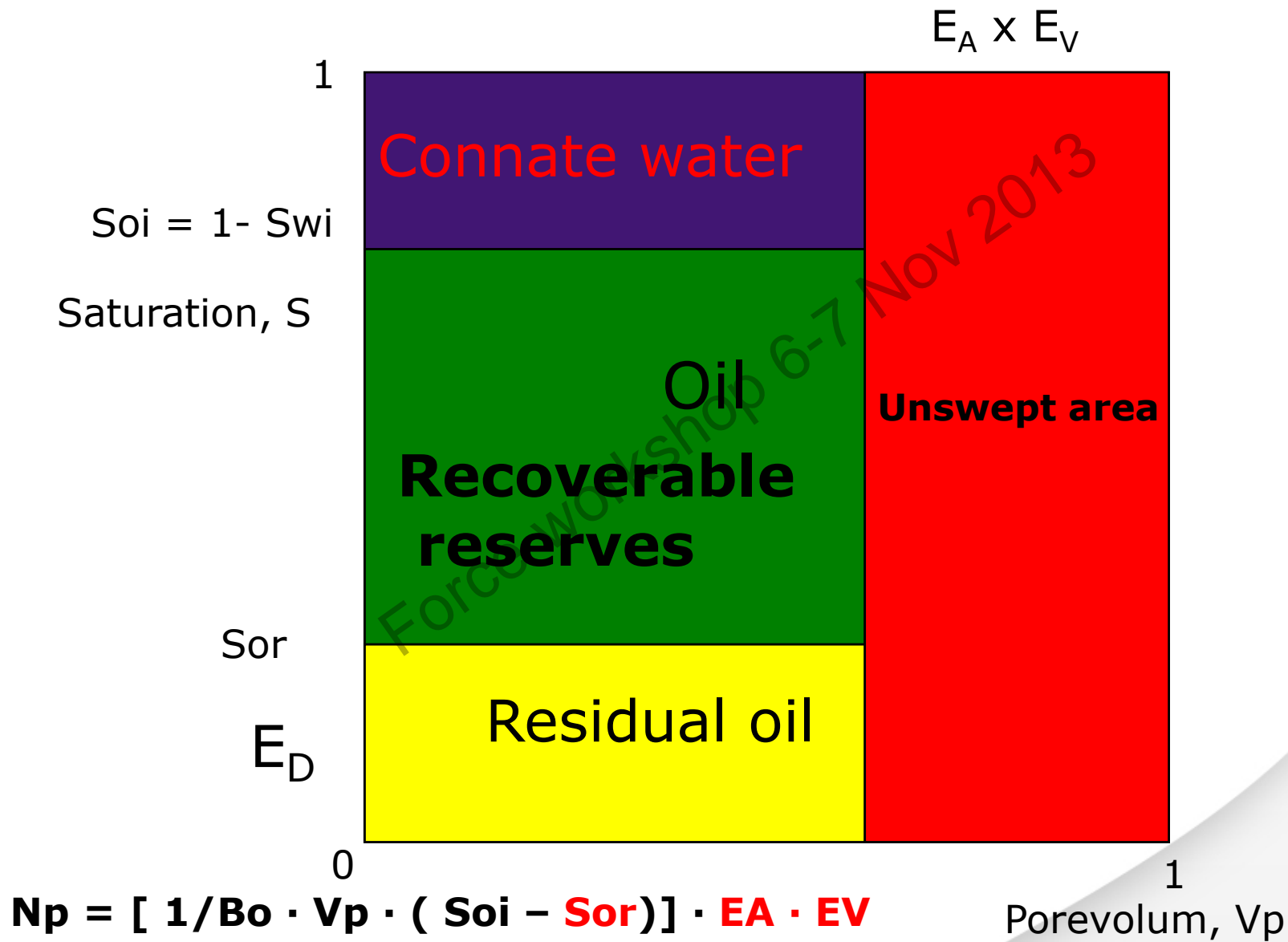


# Target Oil for EOR

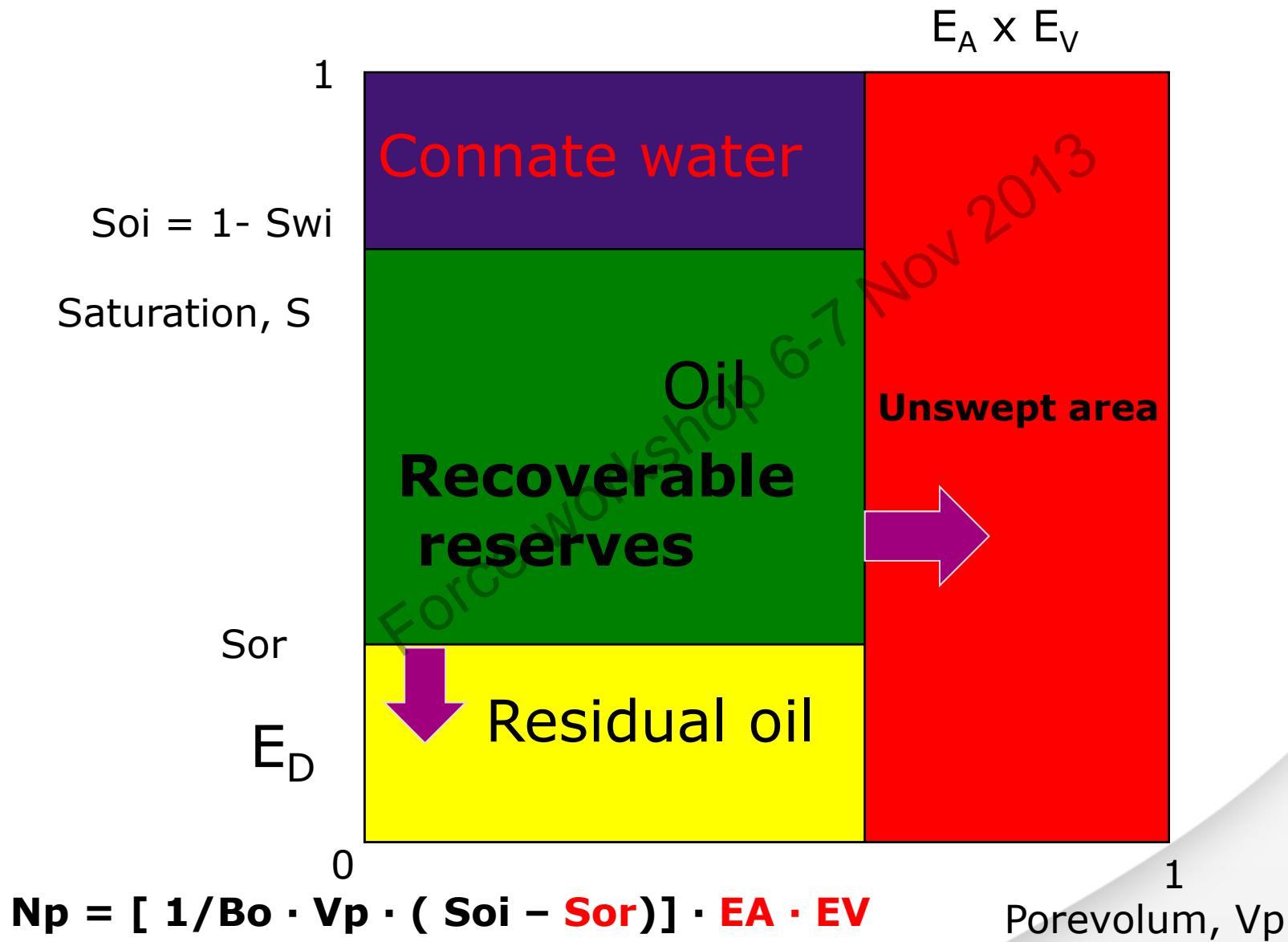
## Some definitions:

- **Primary oil recovery** is where the wells in a reservoir produce under the natural reservoir energy (pressure)
  - typical oil recovery from 1-10% of oil in place
- **Secondary oil recovery** is where we inject water (nearly always) to displace the oil = waterflooding; same effect if strong aquifer drive
  - typical oil recovery from 15-60% of oil in place
- **Improved or Enhanced oil recovery** (EOR; IOR) is where we do something more advanced to obtain the oil left in the reservoir after secondary recovery

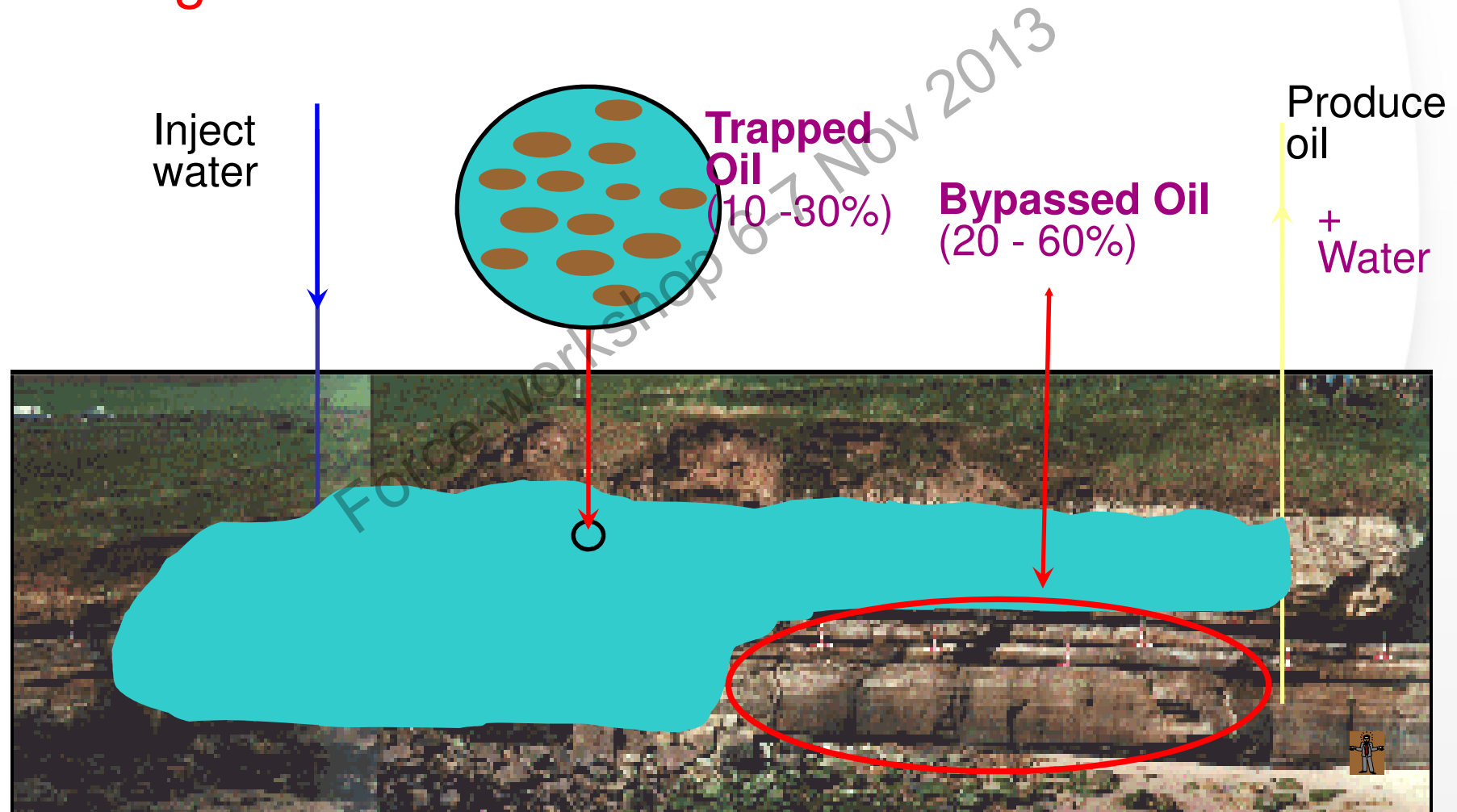
# Oil recovery efficiency = $E_D \times E_A \times E_V$



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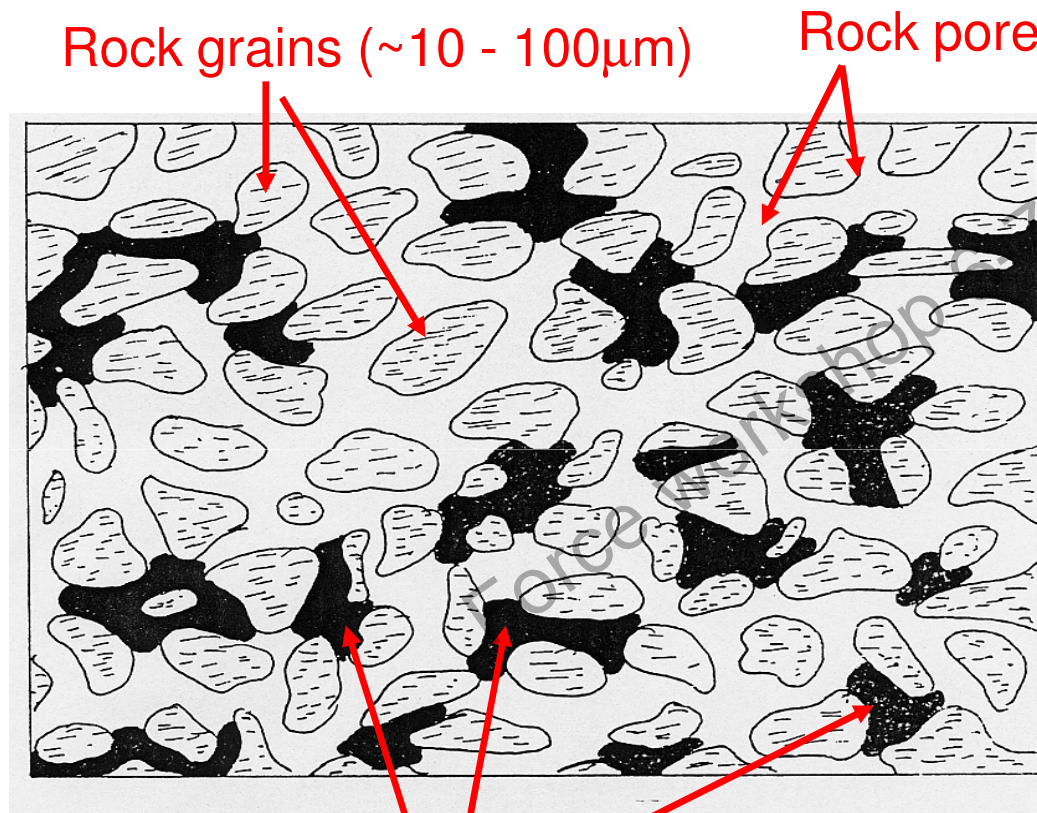
# Trapped (residual) oil & Bypassed Oil: the targets for EOR





## Residual oil saturation

### Trapped Oil at the Pore Scale in a Rock



trapped oil "ganglia" (or blobs)

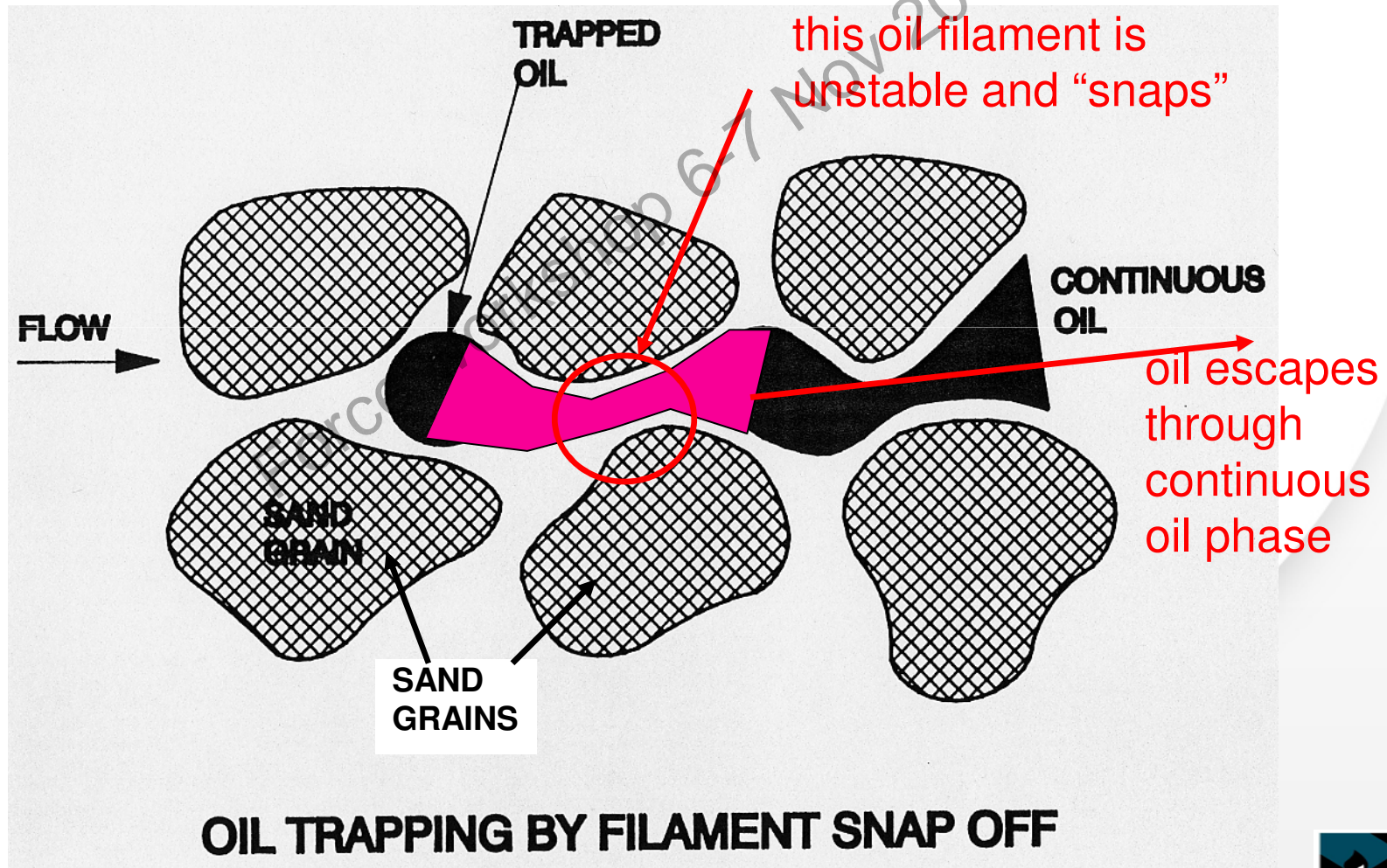
This is the capillary trapped oil or **residual oil,  $S_{or}$**  ... consider the *mechanism* of trapping

N.B. lengthscales  
Particularly ...

Rock pores ~0.1 - 100μm

## Residual oil saturation

### Trapped Oil at the Pore Scale in a Rock: trapping by “snap-off”

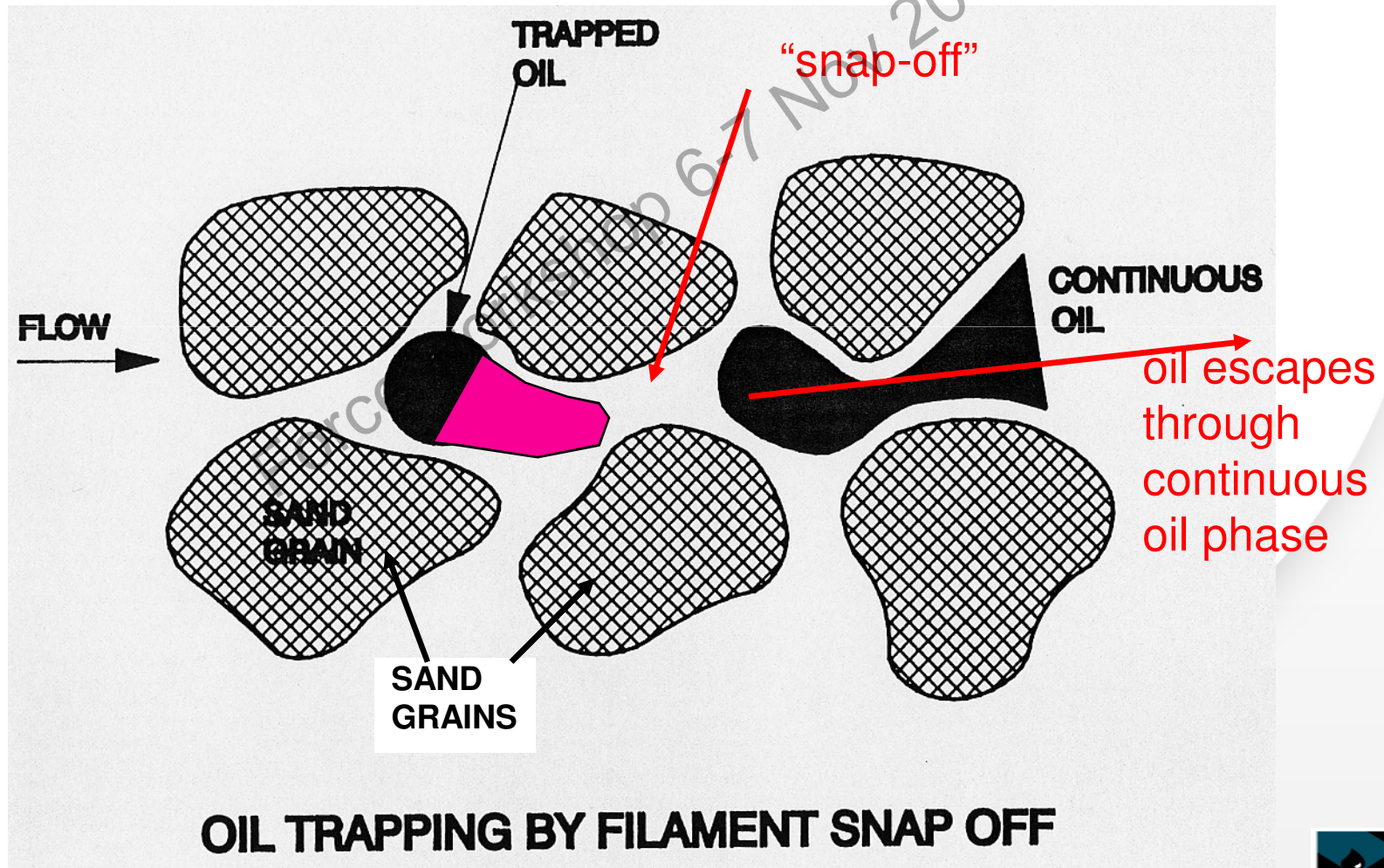


### OIL TRAPPING BY FILAMENT SNAP OFF



## Residual oil saturation

### Trapped Oil at the Pore Scale in a Rock: trapping by “snap-off”



## Residual oil saturation

### Trapped Oil at the Pore Scale in a Rock: pressure to mobilise oil into a smaller pore

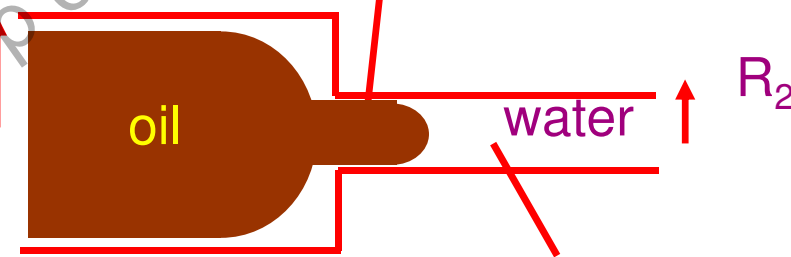
SO WHAT CAN WE CHANGE TO  
MOVE RESIDUAL OIL ??

$$\frac{\Delta P}{\Delta x} = \frac{2 \sigma}{\Delta x} \left( \frac{1}{R_2} - \frac{1}{R_1} \right)$$

Pressure **gradient** to mobilise oil

Oil pressure =  $P_{o2}$

$R_1$



$R_2$

Water pressure =  $P_w$

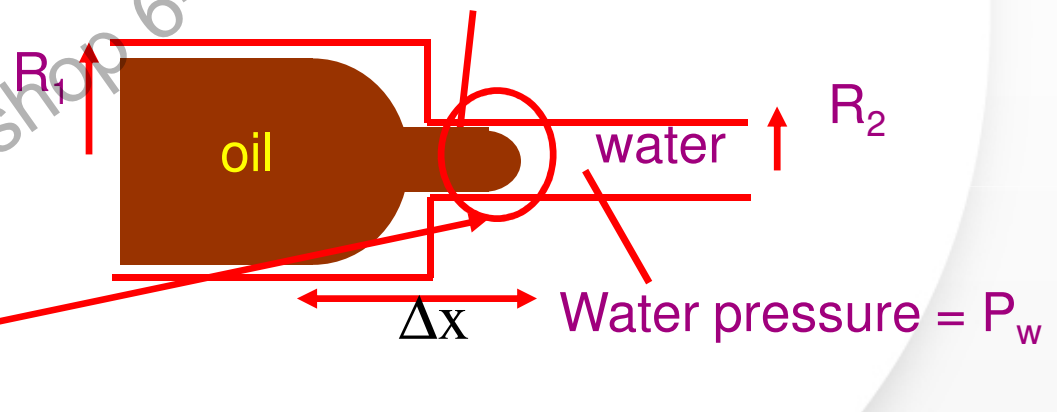
# Trapped Oil at the Pore Scale in a Rock: pressure to mobilise oil into a smaller pore

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Pressure **gradient** to mobilise oil

Oil pressure =  $P_{o2}$



Possibly LOWER interfacial tension,  $\sigma$ , but HOW ??

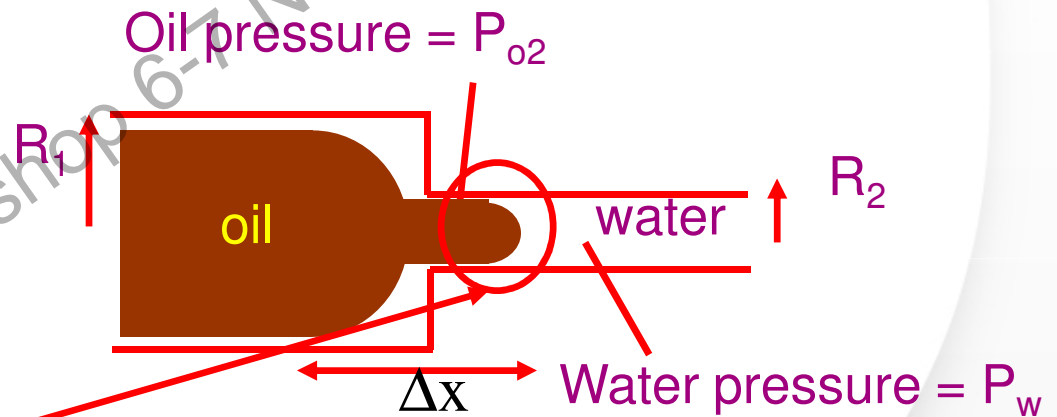
- Surfactant - “soaps” lower  $\sigma$
- Inject gas ( $\text{CH}_4$ ,  $\text{CO}_2$  etc..) which can lower  $\sigma$  and do other things

# Trapped Oil at the Pore Scale in a Rock: pressure to mobilise oil into a smaller pore

SO WHAT CAN WE CHANGE TO  
MOVE RESIDUAL OIL ??

Pressure **gradient** to mobilise oil

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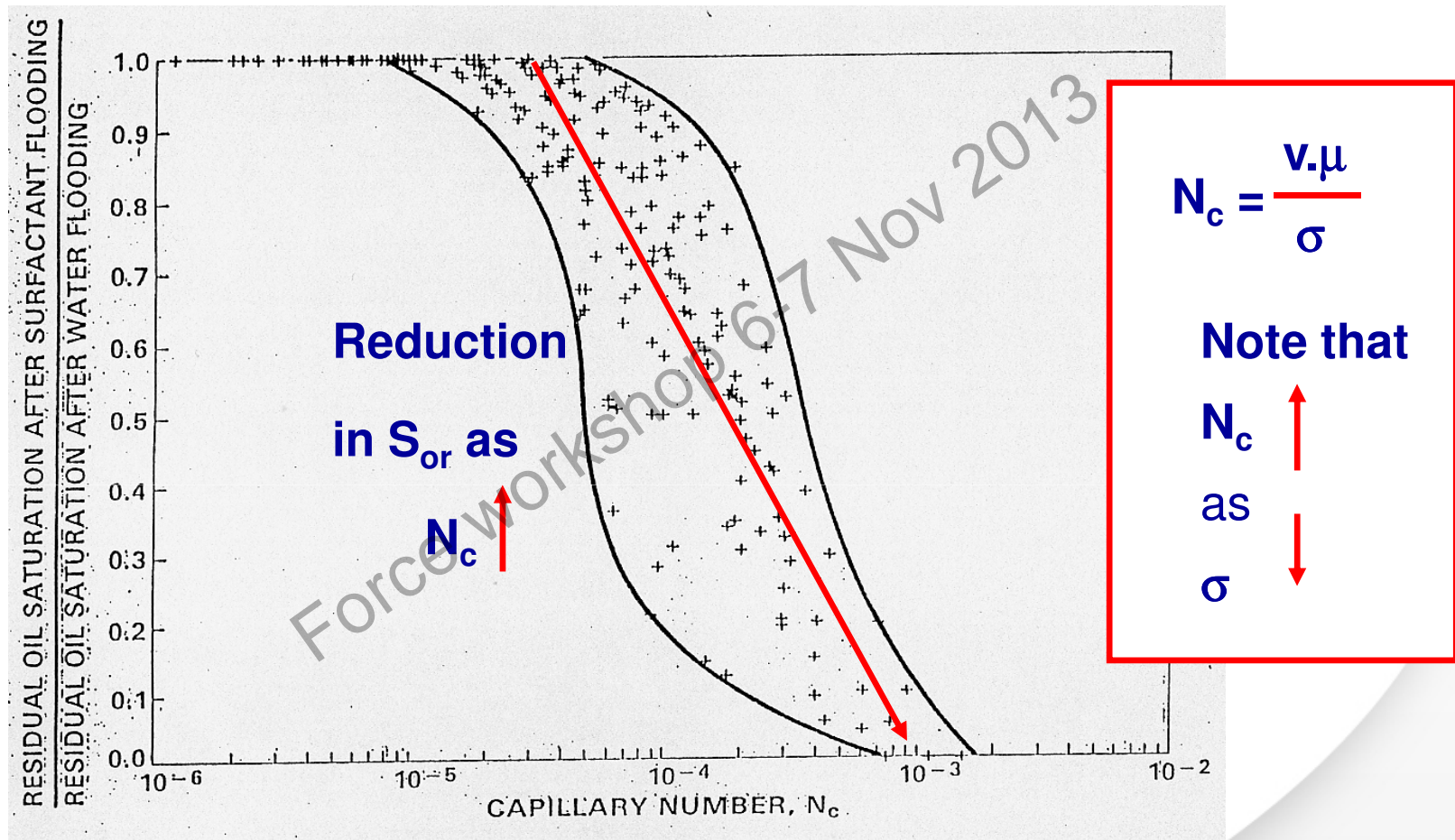
LOWER interfacial tension,  $\sigma$ , but BY HOW MUCH ??

Define Capillary Number,  $N_c$ , as -  $N_c = \frac{v \cdot \mu}{\sigma}$

( $v$  = velocity;  $\mu$  = viscosity;  $\sigma$  = interfacial tension)



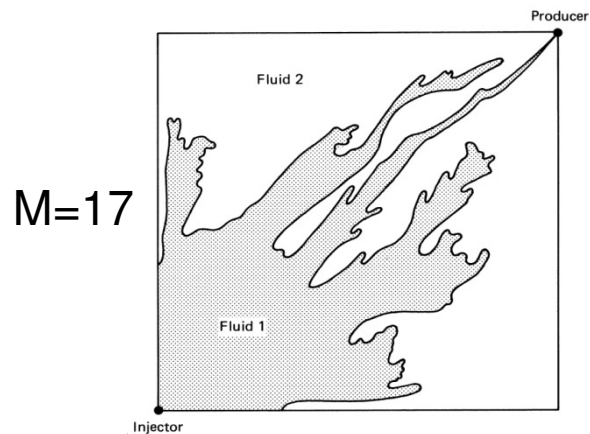
# Residual oil mobilisation at increased Capillary No.



(After Morrow & Chatzis)

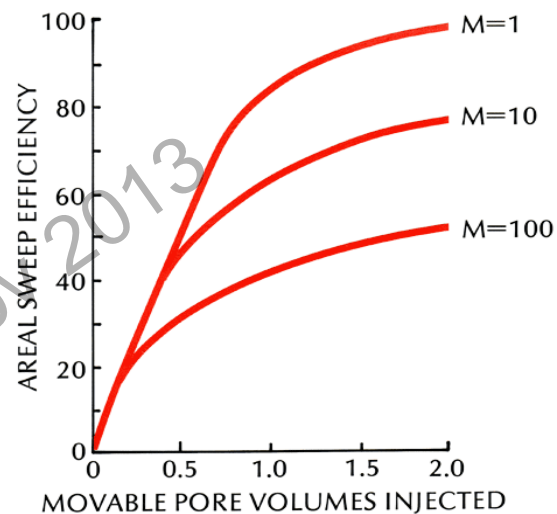
# Sweep

## Areal sweep

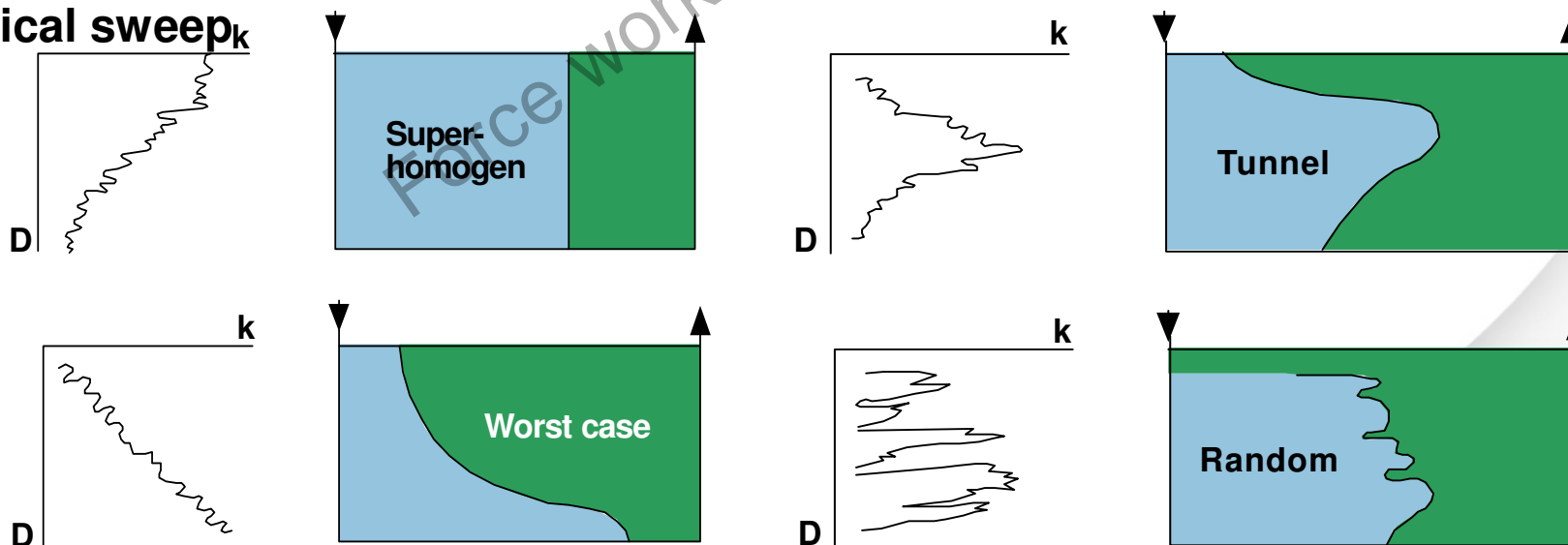


$$M = \frac{K'_{rw}/\mu_w}{K'_{ro}/\mu_o}$$

$M < 1$  stable front

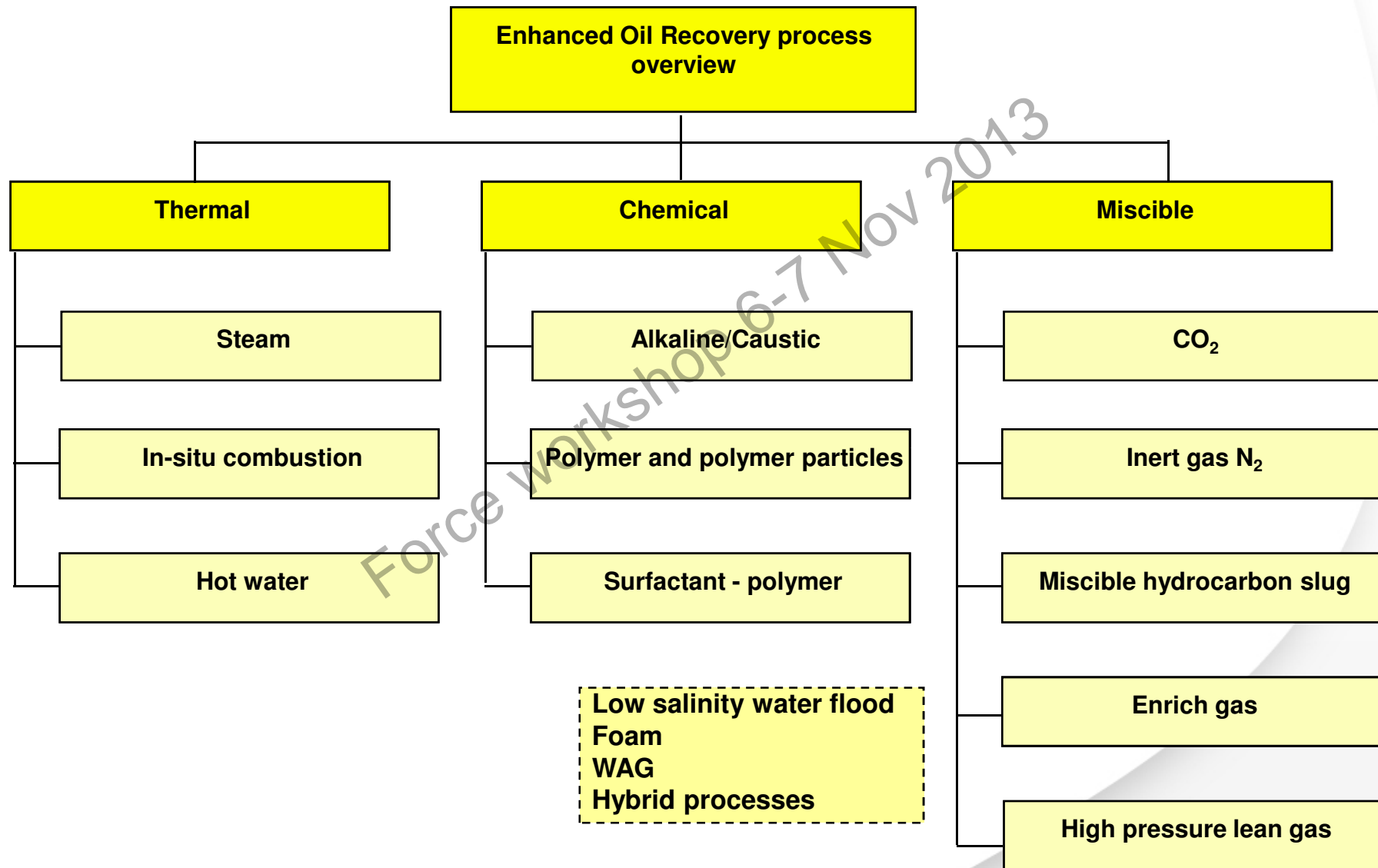


## Vertical sweep<sub>k</sub>





# Enhanced Oil Recovery (EOR)



# EOR experience North Sea reservoirs

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# Maximizing oil recovery for Norwegian oil and gas fields

## Challenges

Identify undrained area

Well distance

Well placement

Logistics

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# Maximizing oil recovery for Norwegian oil and gas fields

## Challenges

Identify undrained area

Well distance

Well placement

Logistics

## Actions

4D seismic and EM

drill cheap/fast new wells

sidetrack injectors into the oil zone

minimize the amount of chemicals for EOR

# Maximizing oil recovery for Norwegian oil and gas fields

## Challenges

Identify undrained area

Well distance

Well placement

Logistics

## Actions

4D seismic and EM

drill cheap/fast new wells

sidetrack injectors into the oil zone

minimize the amount of chemicals for EOR

**Use solved challenges to activate EOR**

# Experience with field implementation of EOR

## Surfactant

Single Well Tracer Tests (Gullfaks, Oseberg)

Surfactant Single Well Test (Gullfaks, Oseberg)

## Other SWTT

Gas Single Well Tracer Test (implemented on Oseberg)

Low salinity SWTT

(Heidrun, Snorre)

Conformance control

(Gullfaks, Snorre, ++)

WAG

(many fields)

Foam and FAWAG

(Brage, Oseberg, Snorre, Veslefrikk, ++)

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# Gas injection EOR



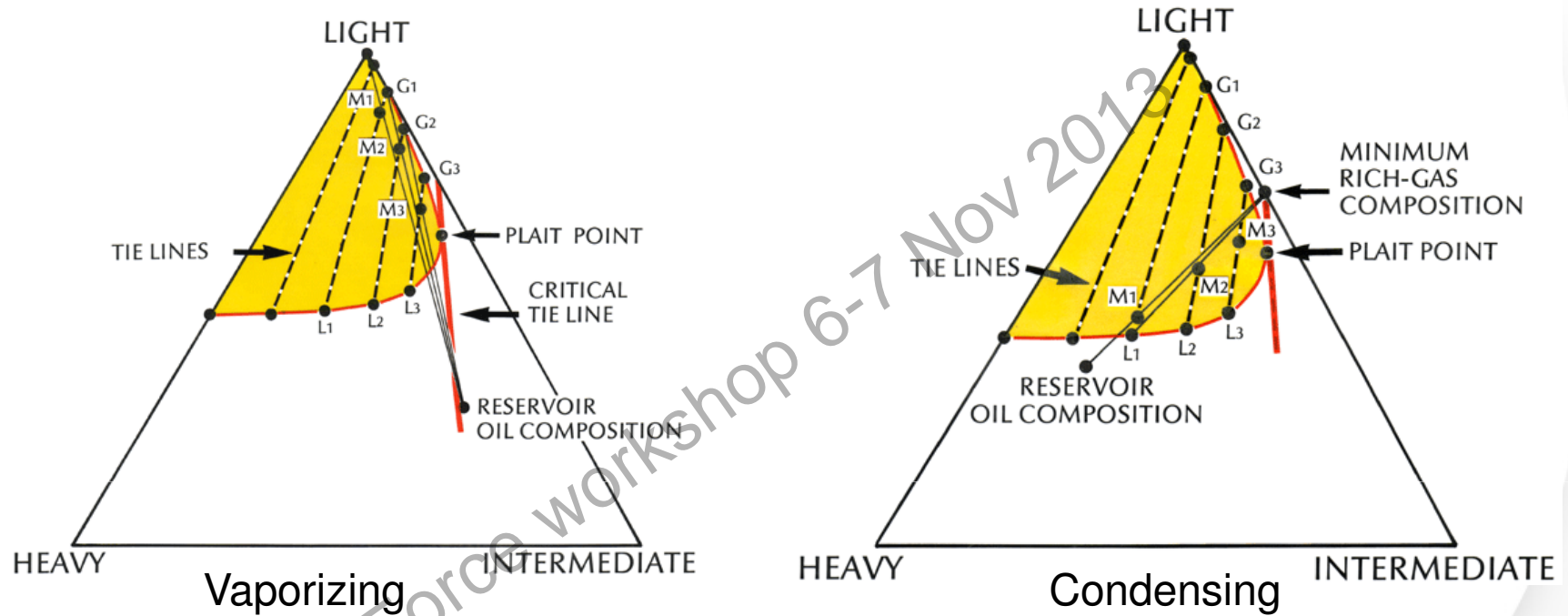
# Gas processes

- Miscible gas
- WAG
- Foam
- CO<sub>2</sub> (EOR and sequestration)

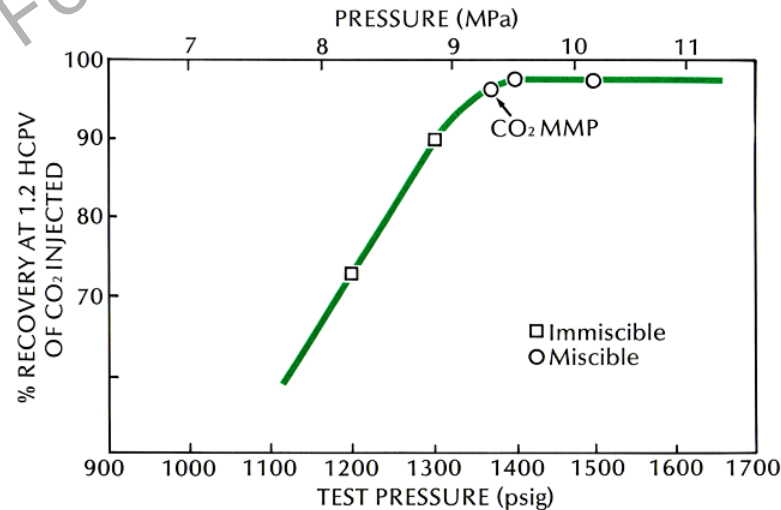
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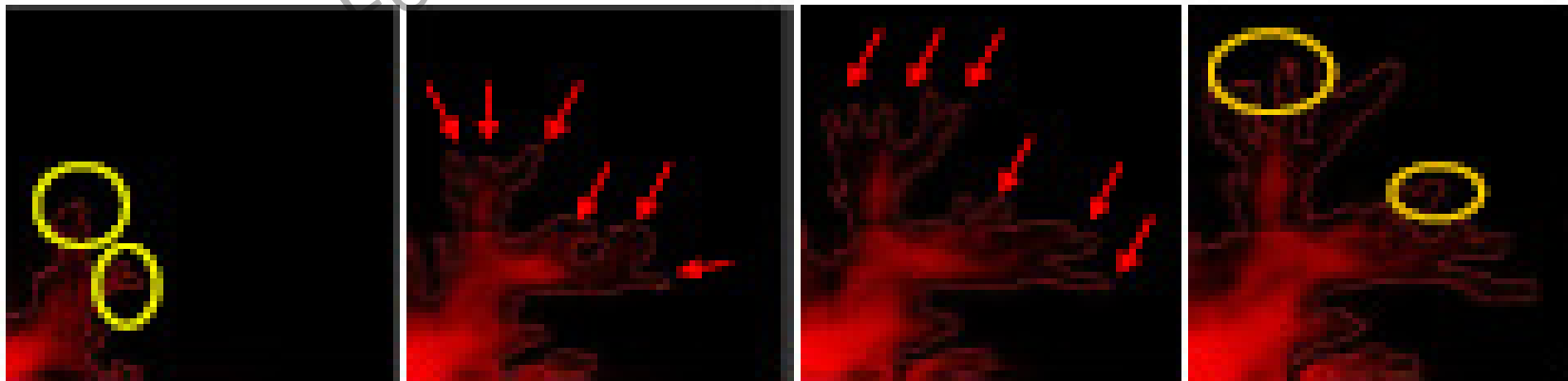
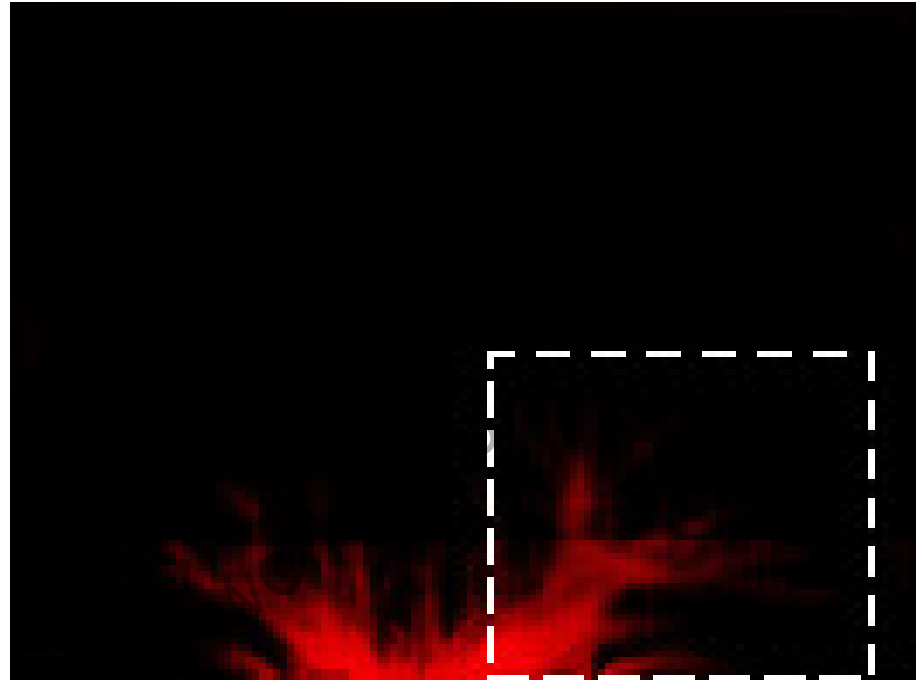
# Multi-contact miscible gas injection



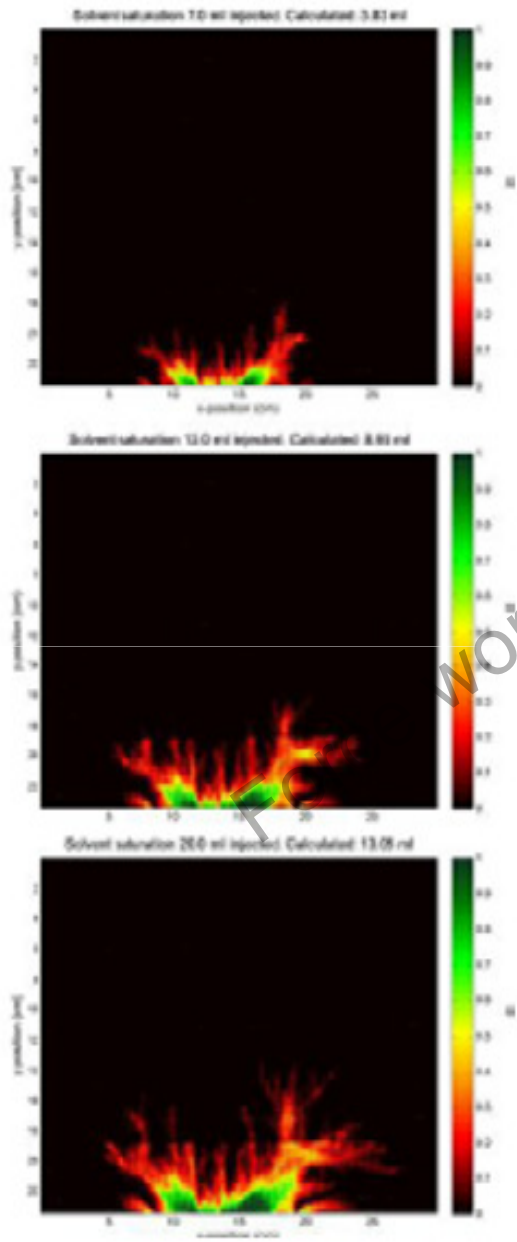
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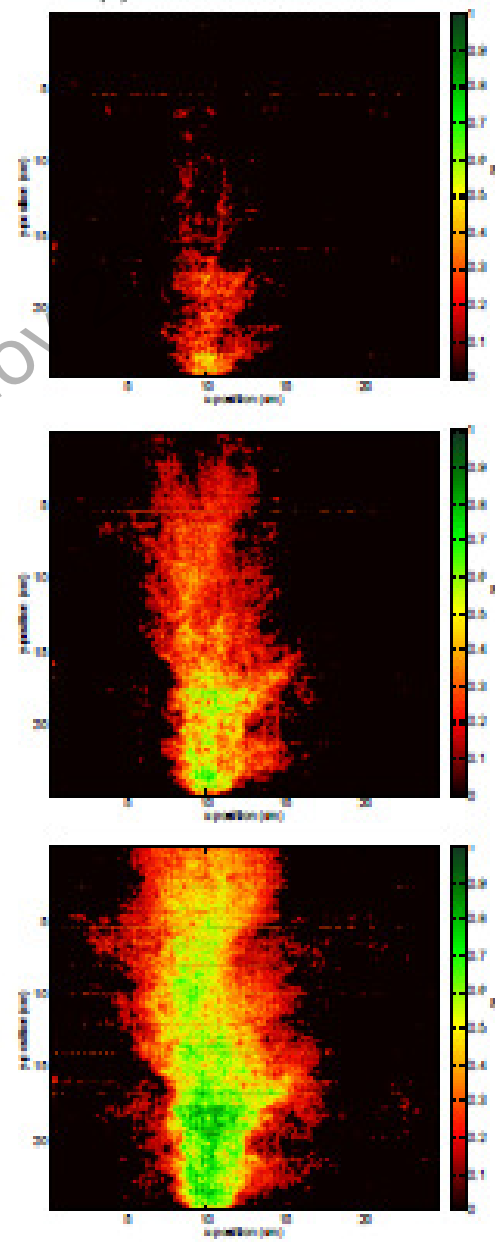
# Viscous fingering



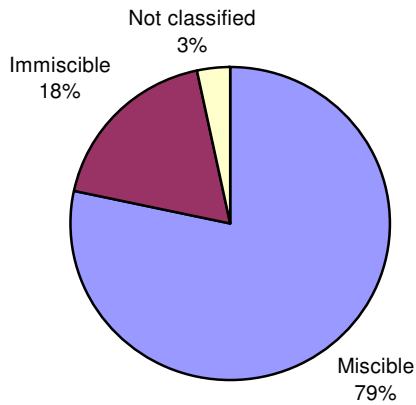
# Sandstone



# Carbonates



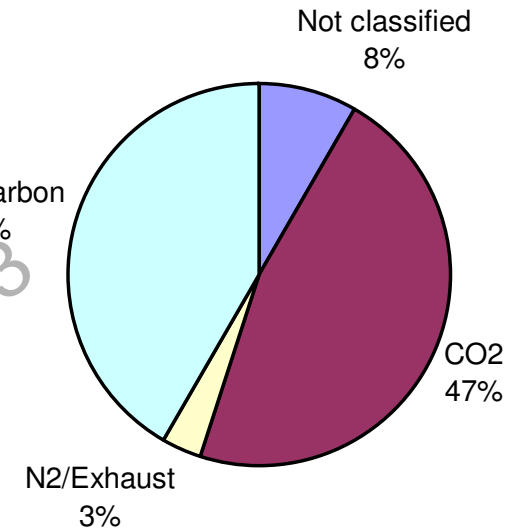
### WAG field applications



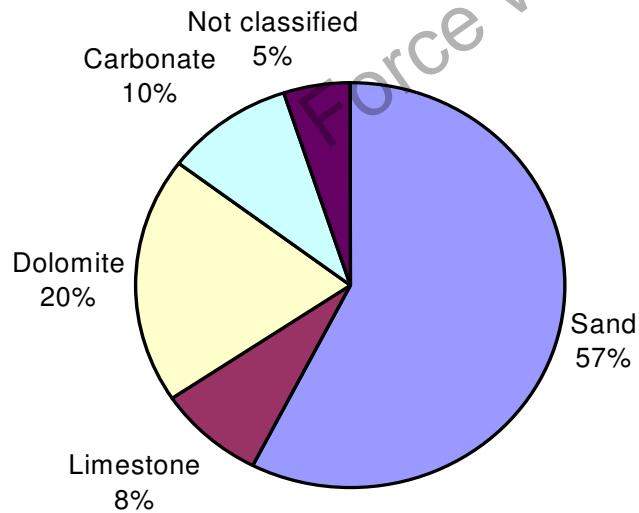
Average increased recovery : 5-10 % OOIP

Miscible applications : 9.7 %

Immiscible applications : 6.4 %



## WAG



### Gases injected in WAG

Average increased recovery : 5-10 % OOIP

CO<sub>2</sub> applications : 8 %

Hydrocarbon applications : 5 %

Carbonates / Dolomites have higher average recovery than sandstones

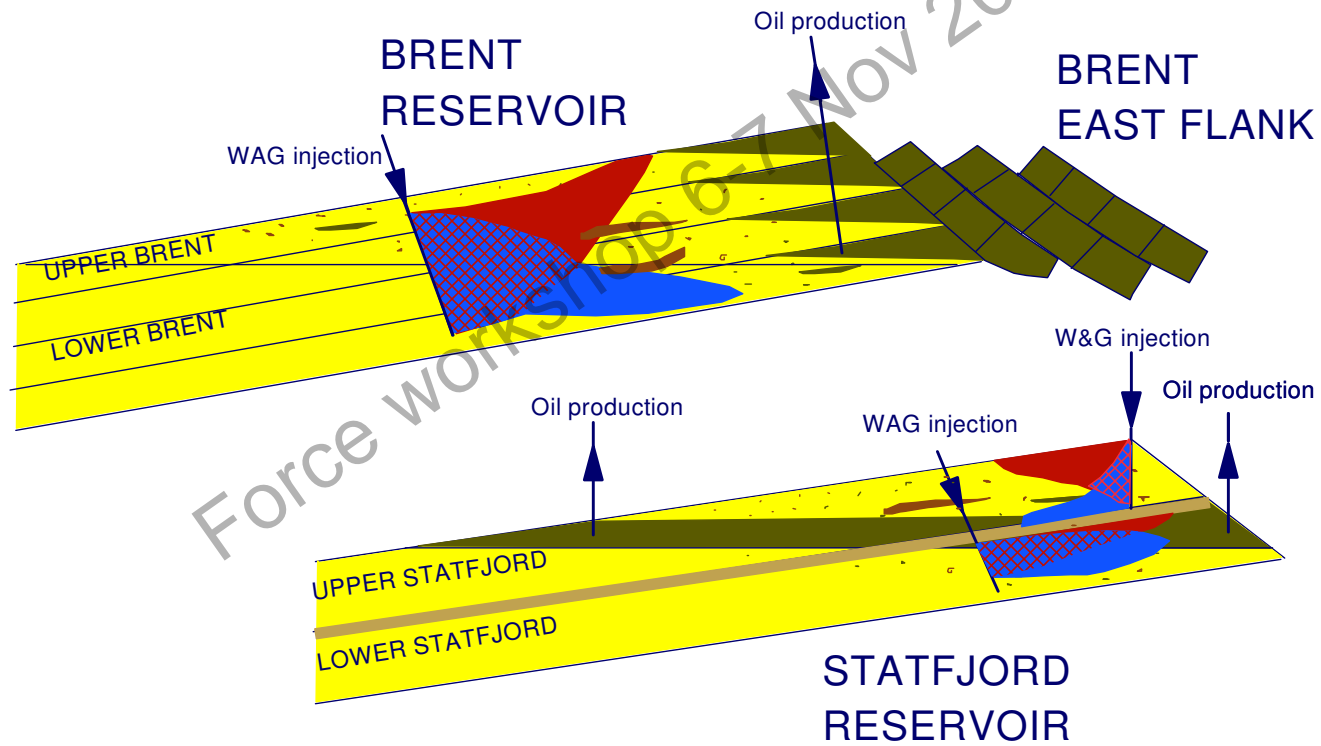
### Formation



# Gas based methods, example

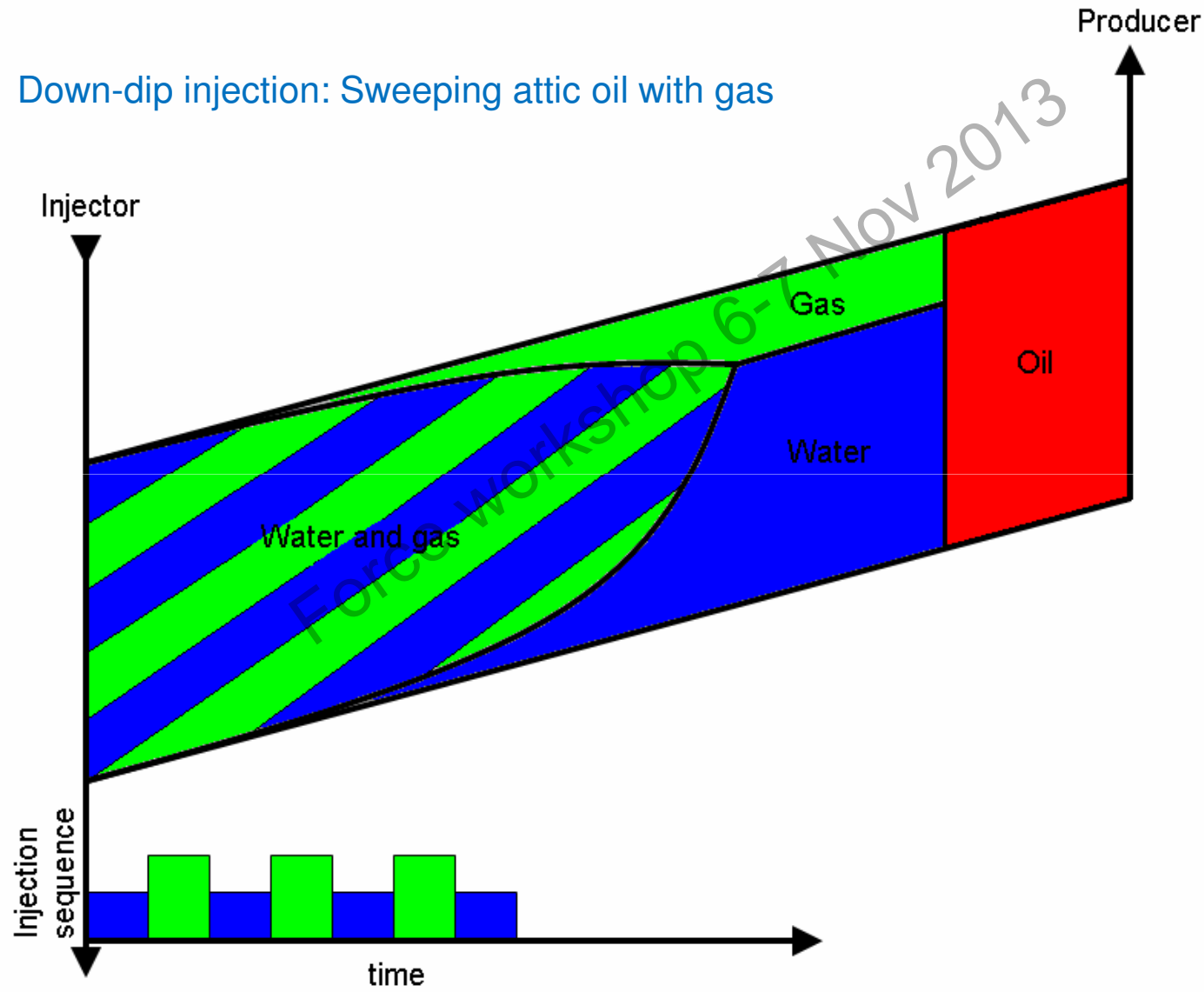


## STATFJORD RECOMMENDED FUTURE DRAINAGE STRATEGY

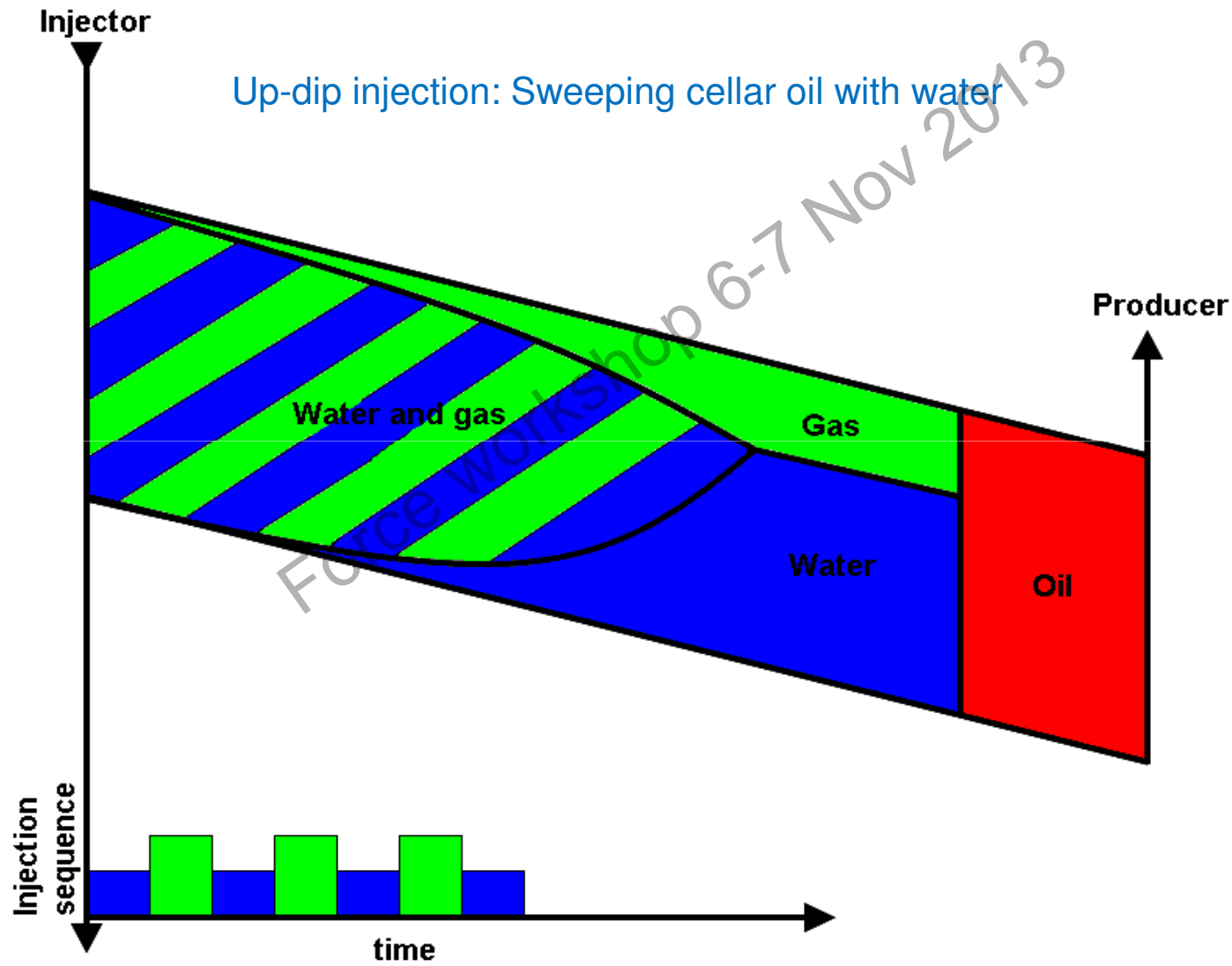


# Gas and water improving vertical sweep

Down-dip injection: Sweeping attic oil with gas



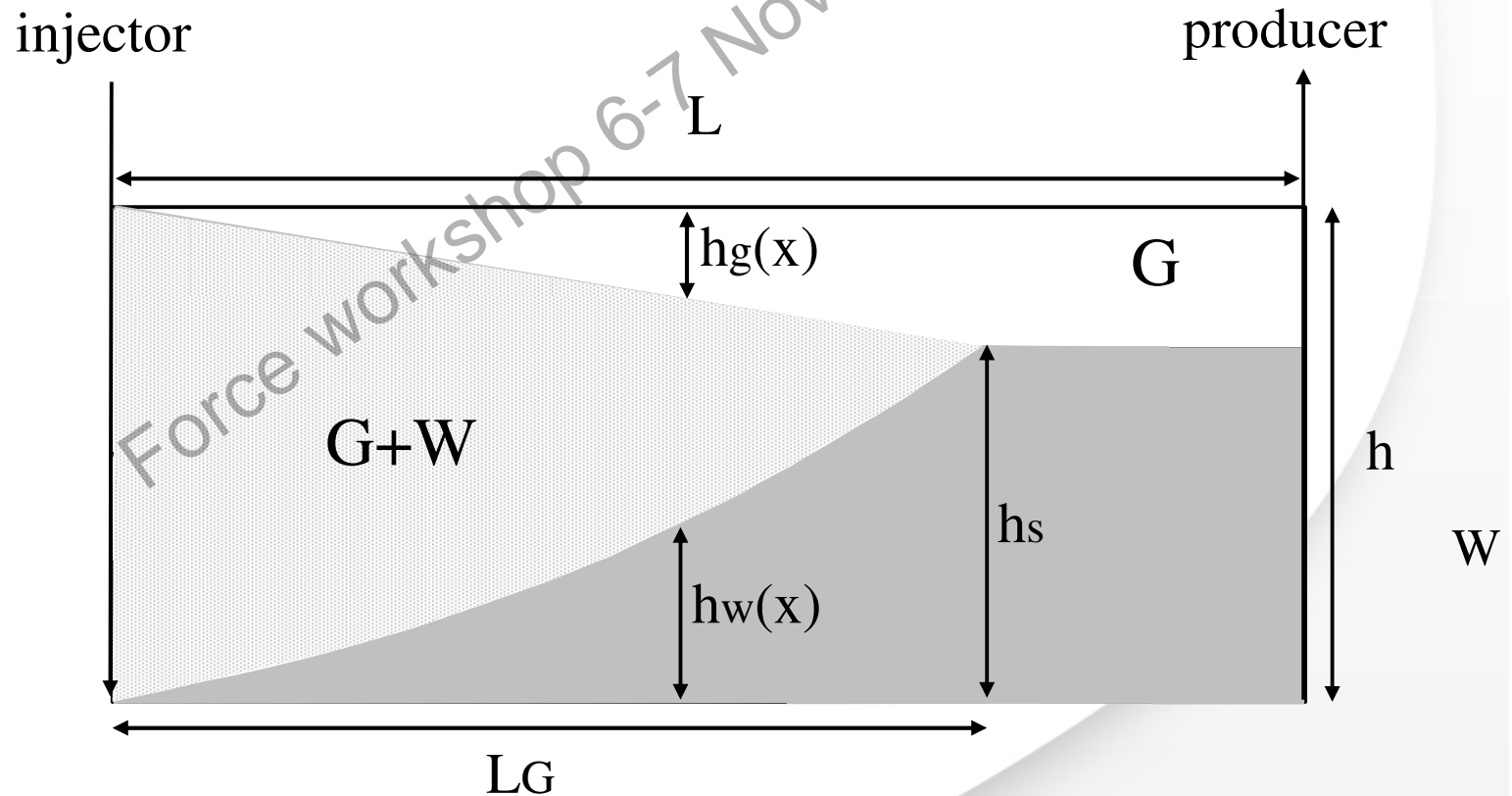
# Gas and water improving vertical sweep



# Stone - Jenkins

Calculation of extent of the WAG three-phase zone based on two-phase flow only

Statement: Jenkins analytical model underestimates the WAG three-phase zone when compared to three-phase flow simulation results



**BUT  $S_{om} (3ph) \ll S_{or} (2ph)$**



# WAG Model requirement

## - Gas modeling

must include gas trapping

gas rel perm must be able to vary with:

- increasing / decreasing gas saturation
- water saturation
- gas trapping history

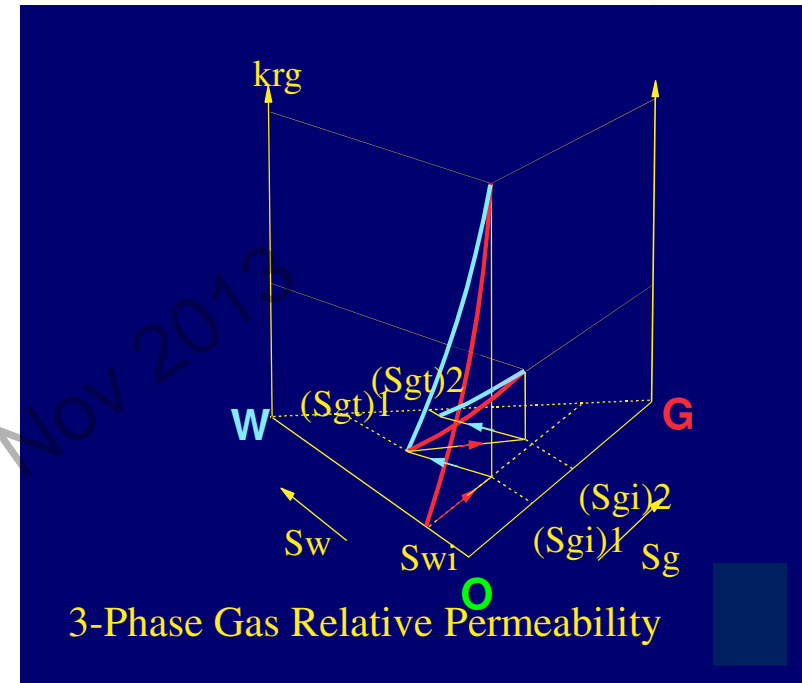
## - Water modeling

water relative permeability must vary with:

- increasing/decreasing water saturation
- gas saturation

## - Oil modeling

residual oil must be allowed to change with **trapped gas**  
**oil relative permeability should be history dependent**



WAG Hysteresis model recommended (developed by Larsen and Skauge)

Available in ECLIPSE

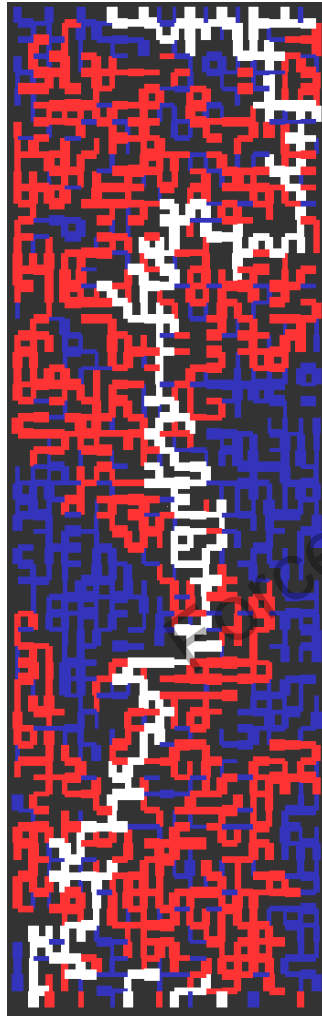
# Immiscible WAG: mechanism - redistribution

RED  
- oil

BLUE  
- water

WHITE/  
YELLOW  
- gas

$\sigma_{go} = 15 \text{ mN/m}$

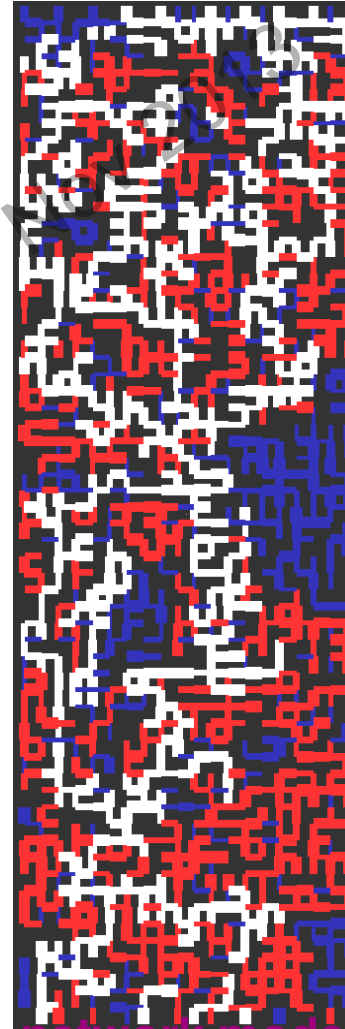


network model

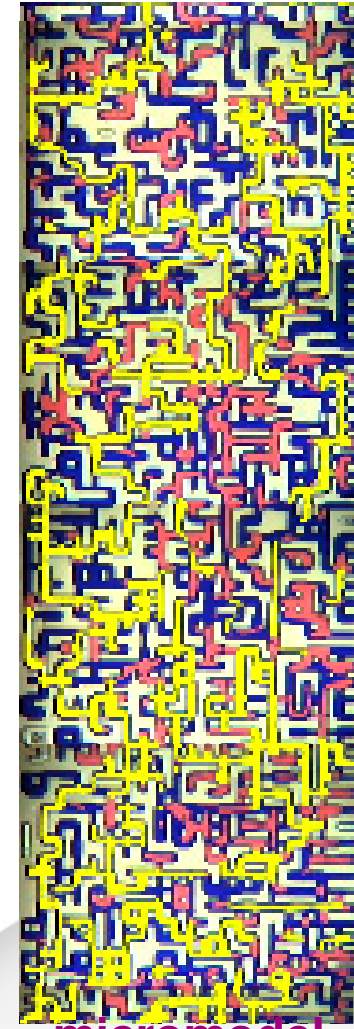


micromodel

first gas flood



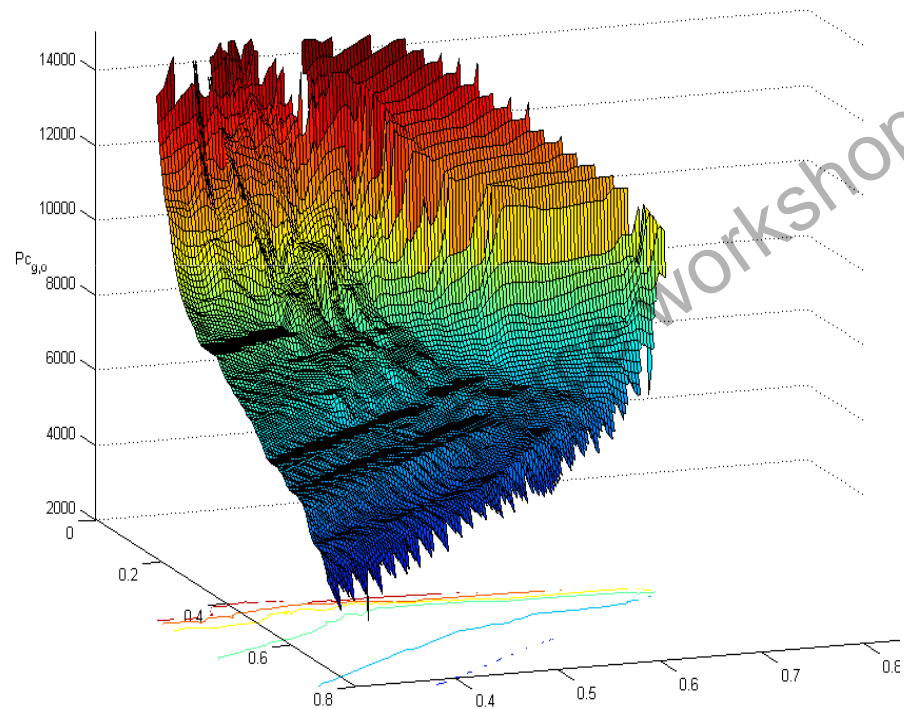
network model



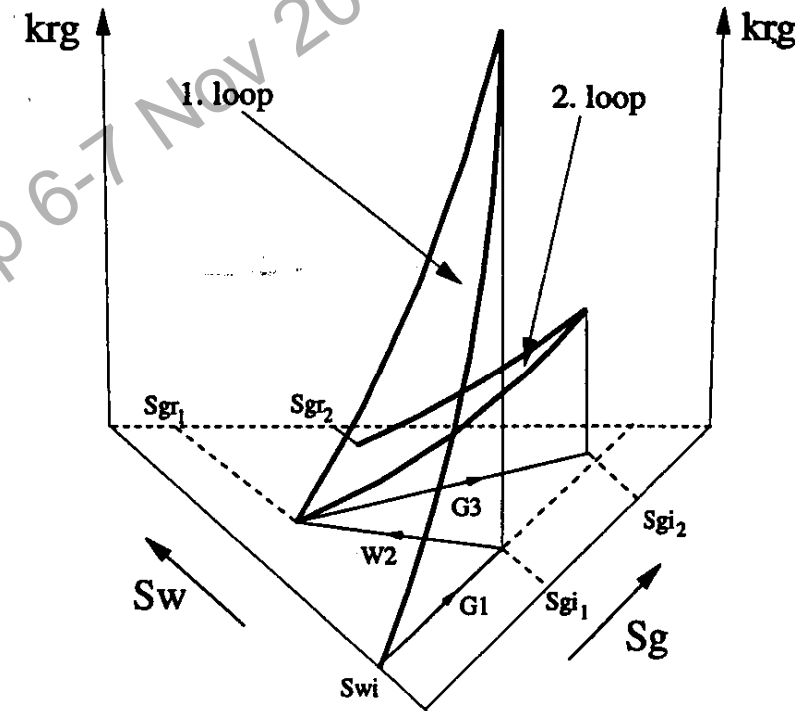
micromodel

fifth gas flood

# WAG modelling



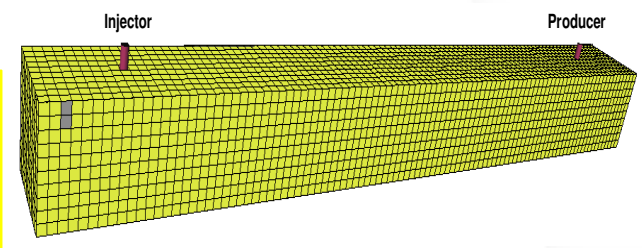
three-phase  $P_c$  (go)



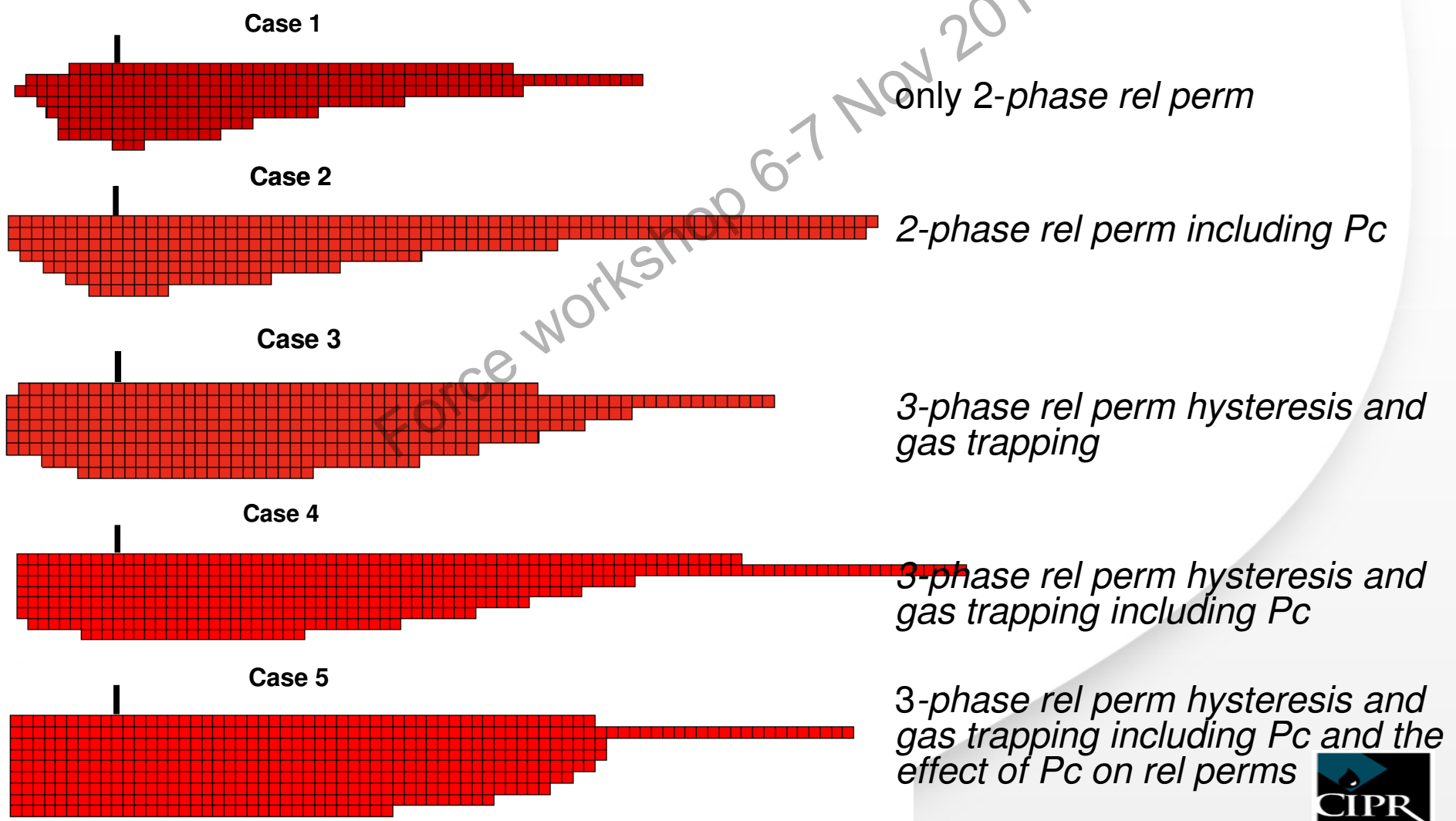
Larsen and Skauge, SPEJ  
Skauge and Dale, SPE 111435

# Example - Extension of three-phase zone

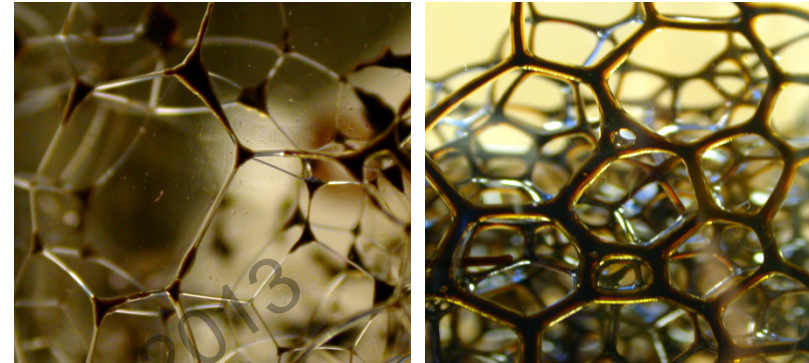
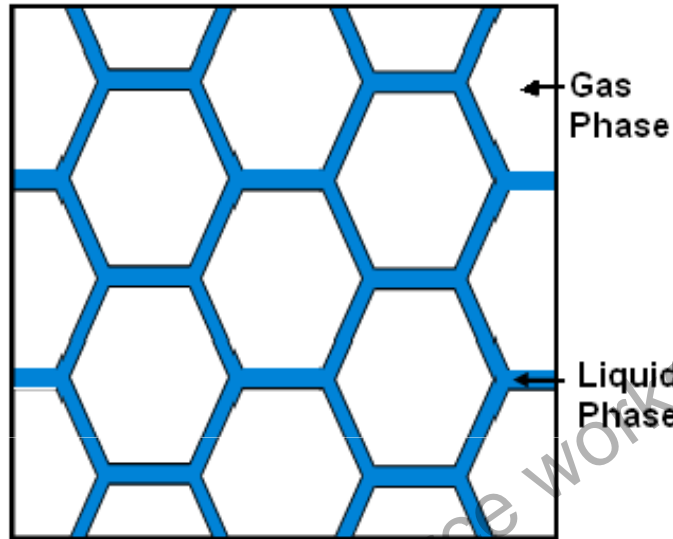
More detailed fluid flow description  
Leads to:  
Larger three-phase zone  $S_{om} \ll S_{or}$   
115% increase in three phase zone, 35% increase in recovery



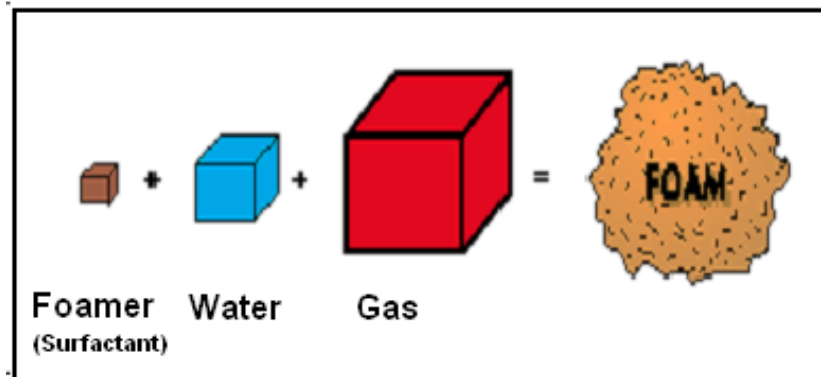
Skauge and Dale, SPE 111435



# Foam



- Structured two phase, compressible fluid
- Hexagonal foam texture
- Large gas volume dispersed as bubbles in a continuous liquid phase
- Liquid film is stabilized by surfactants to prevent bubble coalescence



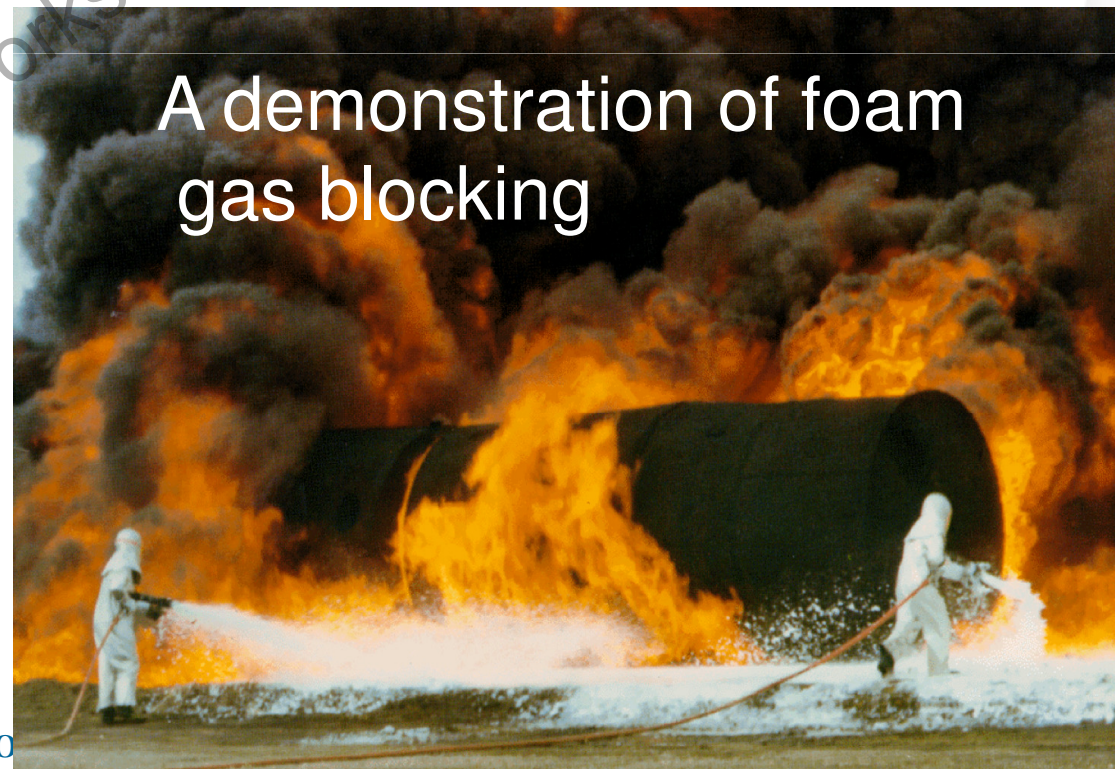
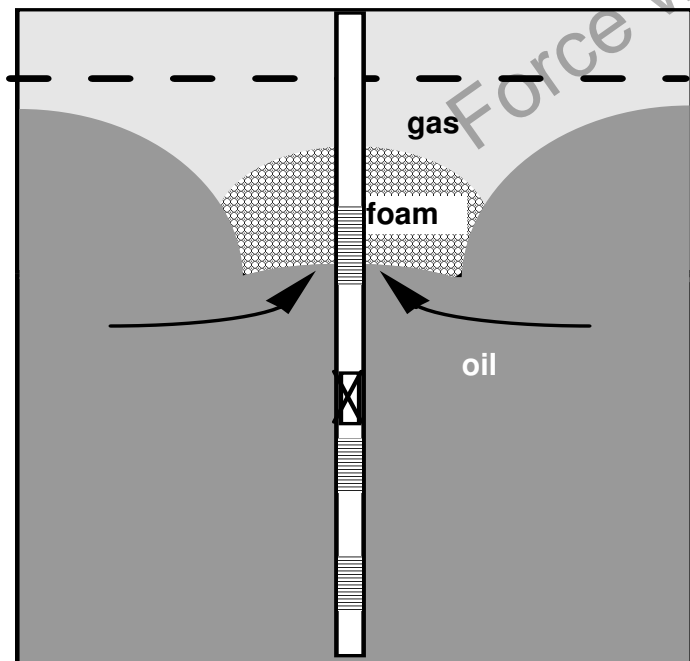
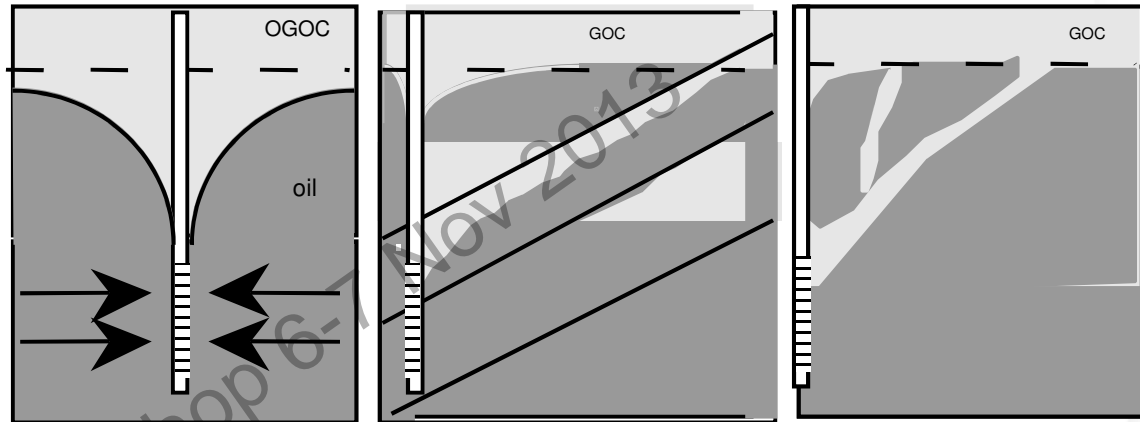


# Foam Applications

Near the producer:

- a) Gas coning.
- b) Gas cusping.
- c) Gas channelling in fractures

**Foam blocking  
a gas cone**



# Foam trials North Sea Area

## Production well treatments

- ✓ Oseberg
  - ✓ B-27 1994
  - ✓ B-38 1996
  
- ✓ Beryl
  - ✓ B-30z 1994
  
- ✓ Snorre
  - ✓ P-18 1996

## Foam for mobility control

- ✓ Snorre
  - ✓ Central Fault Block
  - ✓ (P-25-P18A) 1997/98
  
- ✓ Western Fault Block
  - ✓ (P32-P39) 1999/2000
  
- ✓ Brage 1998

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# Waterflood EOR





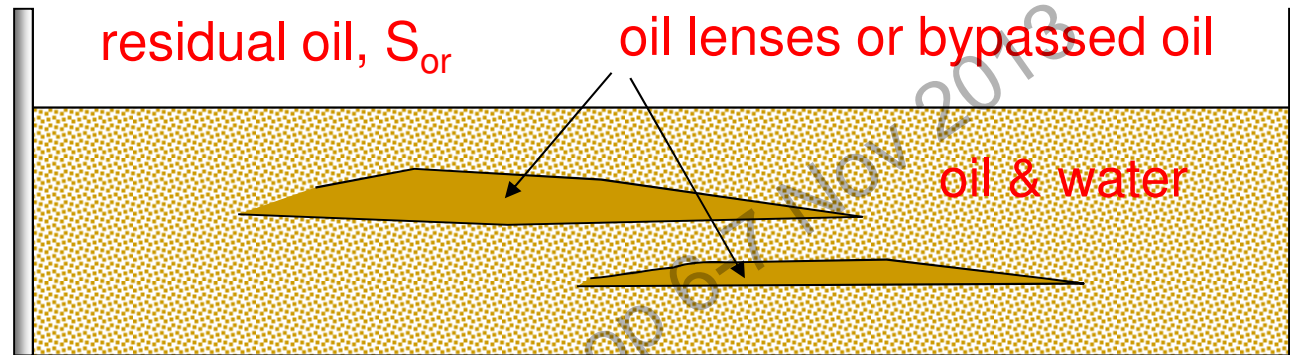
# Waterflooding EOR

- Low salinity
- Hybrid EOR
- Surfactants (lower IFT)
- Polymer flooding (sweep ++)
- LPS (microscopic diverging)
- Diverging techniques
- MIOR
- and more

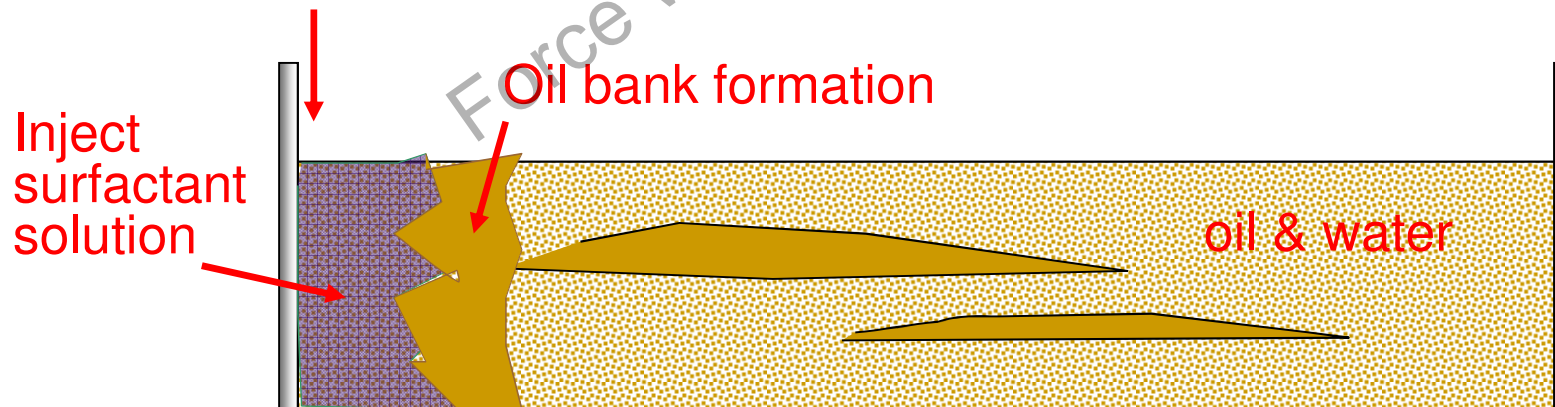
# Conventional Chemical Methods for Enhanced Oil Recovery

- Surfactants to lower the interfacial tension between the oil and water or change the wettability of the rock
- Water soluble polymers to increase the viscosity of the water
- Polymer gels for blocking or diverting flow
- Combinations of chemicals and different methods

# How surfactant floods are applied in the field

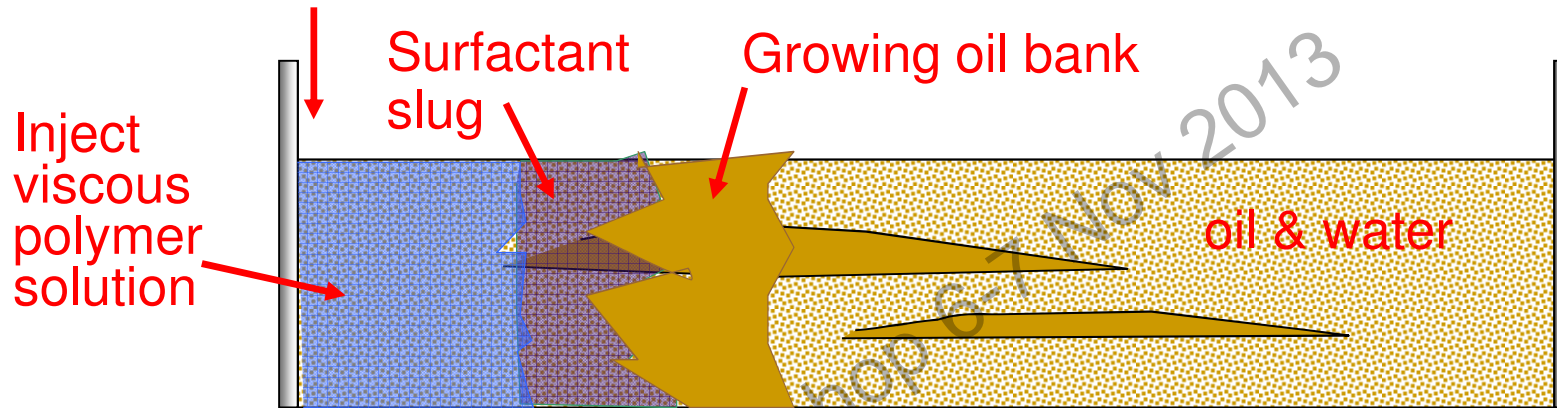


1. Situation after some time of waterflooding;  $S_{or}$  and bypassed oil

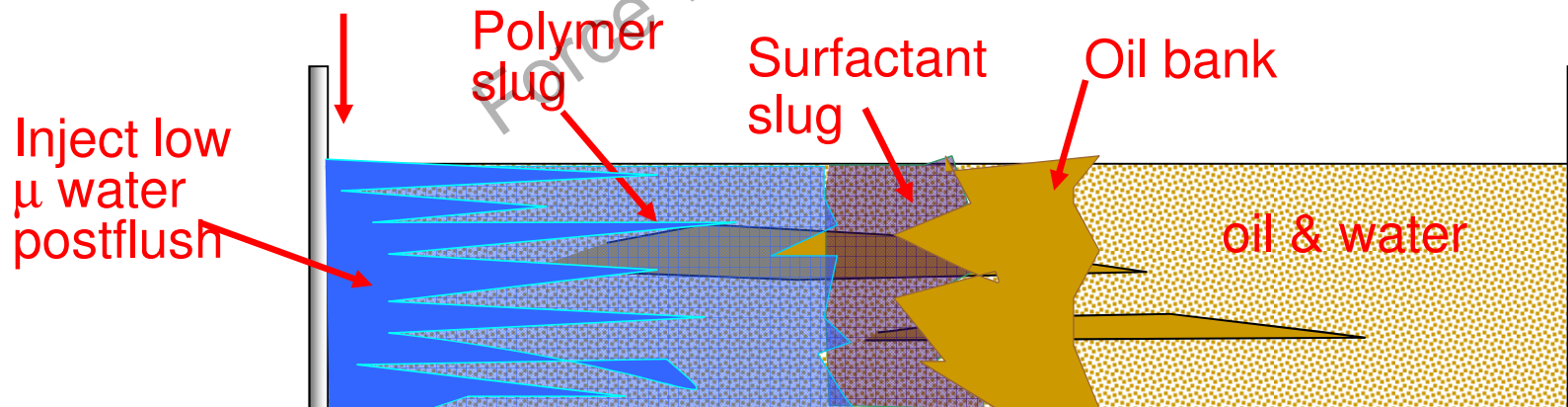


2. Inject aqueous surfactant solution - mobilise oil - form "oil bank"

# How surfactant floods are applied in the field



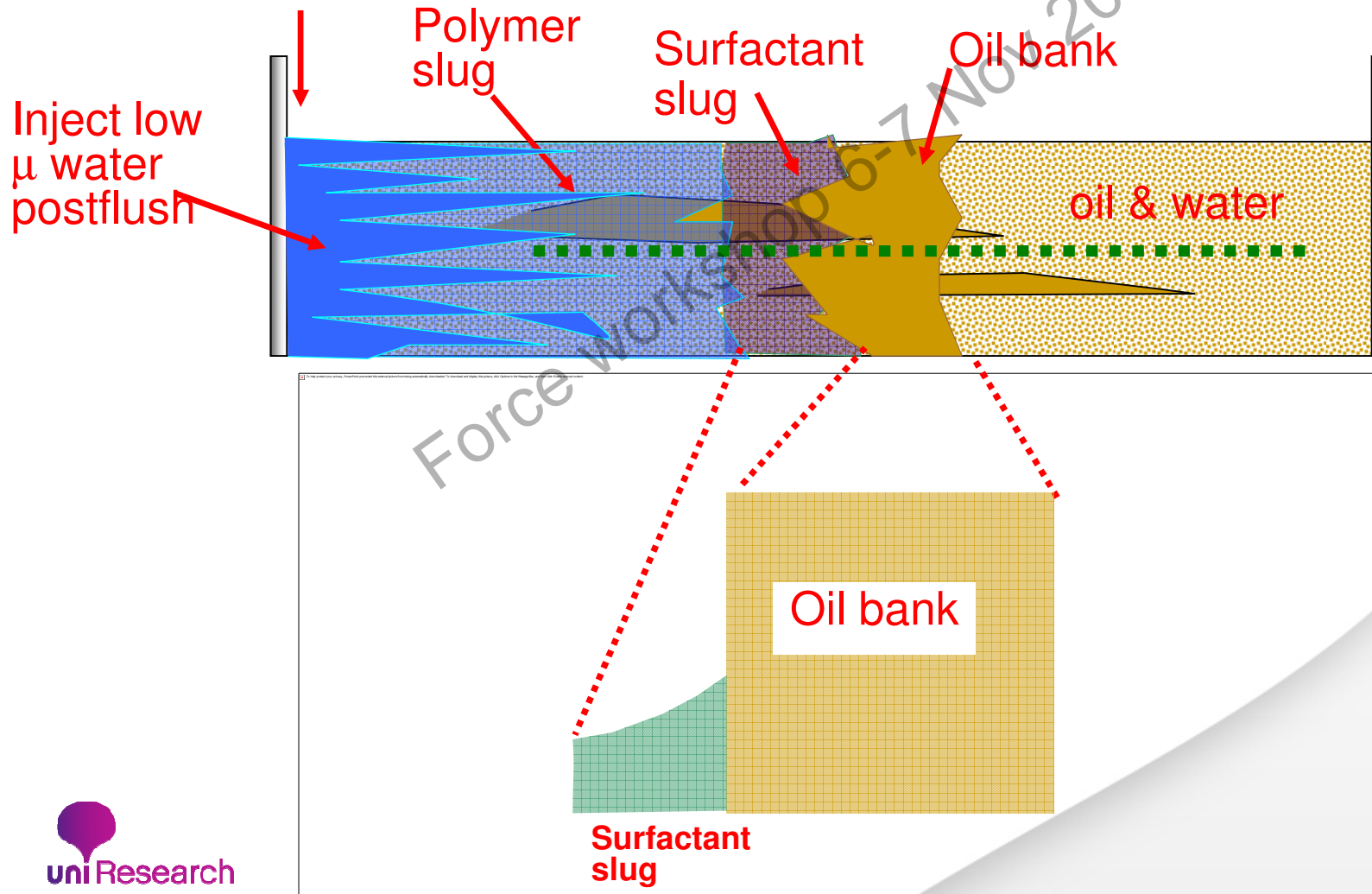
3. Post-flush with viscous polymer solution for mobility control



4. Later water injection may lead to some fingering through polymer

# Surfactant floods - frontal structure of oil bank

Note the profile of the oil saturation in 1D



# Classical Surfactant Enhanced Oil Recovery

- Surfactants has been used to lower the interfacial tension between the oil and water and / or change the wettability of the rock
- Water soluble polymers to increase the viscosity of the water
- Alkaline chemicals such as sodium carbonate to react with crude oil and generate surface activity plus increase pH
- Combinations of chemicals and methods

MF - MPF - SF - SPF - LTPF - AF - APF - ASPF .....

# Conventional Surfactant Polymer (SP) Flooding & Alkali (A) Flooding

- **Surfactant + Cosurfactant (S):** applied to give a low o/w IFT at some optimal salinity;  
=> high Capillary Number  
=> mobilises previously trapped oil – reduces Sor
- **Polymer (P):** viscosifies the injected brine and give mobility control behind the surfactant slug
- **Alkali (A):** high pH alkali solution applied to cause “soap” formation (saponification) with acids in oil – these “soaps” reduce o/w IFT and cause reduced Sor

# Alkali (A) Surfactant (S) Polymer (P) Flooding ASP

## KEY aspects of ASP flooding SHORT SUMMARY

1. In situ “soap” generation by Alkali + crude oil – natural surfactants
2. Appropriate phase behaviour with Crude/brine/”soap”+Surfactant
3. LOW IFTs with Crude/brine/”soap”+Surfactant – optimal salinity affected by both [Surfactant] and [“Soap”]
4. LOWER surfactant Adsorption at higher pH
5. OTHER Reservoir Chemistry
  - The **CARBONATE/ALKALI System**
  - **ION EXCHANGE** with clays – mainly  $H^+/Na^+$  ,  $Ca^{2+}$  etc..
  - **MINERAL REACTIONS** dissolution/precipitation



# Surfactant Types

- Anionic surfactants preferred
  - Low adsorption at neutral to high pH on both sandstones and carbonates
  - Can be tailored to a wide range of conditions
  - Widely available at low cost in special cases
  - Sulfates for low temperature applications
  - Sulfonates for high temperature applications
  - Cationics can be used as co-surfactants
- Non-ionic surfactants have not performed as well for EOR as anionic surfactants

**I will argue why:**

**Conventional surfactant flooding never will become a widely used EOR process for North Sea oil reservoirs**

***Statement:***

**Ultralow interfacial tension is counteracted by poor flow properties and high surfactant loss (retention)**

**The presentation will give evidence to this statement and indicate a way forward**

# Some challenges related to field applications

- Finding a suitable surfactant (and polymer)
  - Low cost (polymer and surfactant)
  - Manageable logistics (polymer and surfactant)
  - Good injectivity (polymer)
  - Low adsorption / loss (polymer and surfactant)
  - Optimal phase behaviour at reservoir conditions (surfactant)
    - Salinity
    - Temperature
    - Pressure

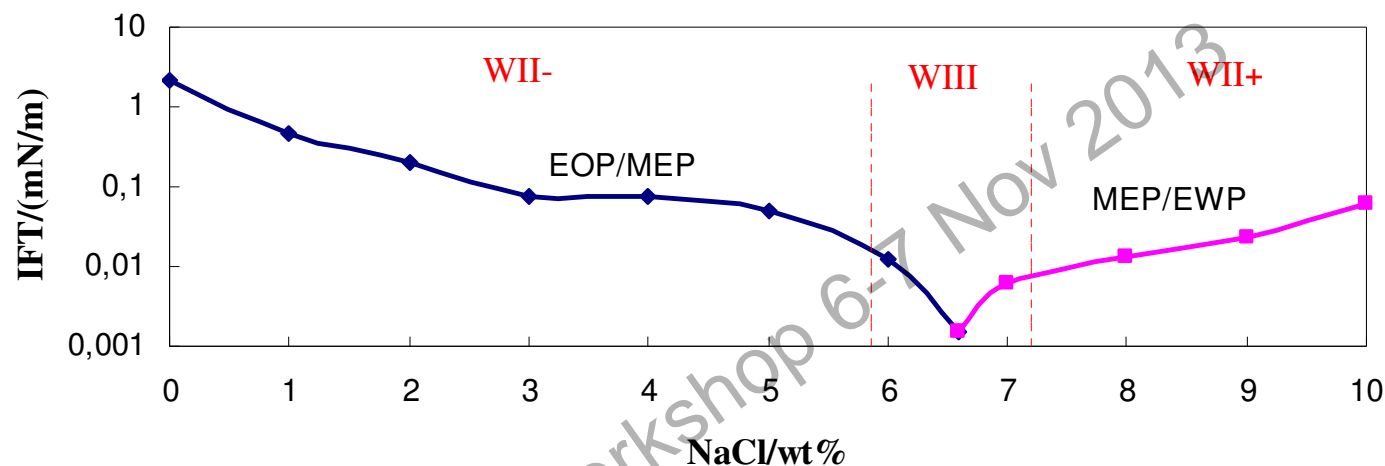
# Classical Micellar Polymer Flooding

- Optimizing a surfactant flooding process is a compromise between
- Ultralow IFT
- Low retention
- Injectivity (solution properties)
- phase viscosity

Is it possible to have good solution properties at conditions where we can achieve ultralow IFT?

Can we achieve low adsorption/retention at conditions where we can achieve ultralow IFT?

## Phase behaviour and IFT as functions of salinity



NaCl %	0	1	2	3	4	5	6	6,6	7	8	9	10
Phase behaviour	II-	II-	II-	II-	II-	II-	III	III	III	II+	II+	II+
IFT/(mN/m)	2,18	0,46	0,21	0,075	0,077	0,05	~0,013	0,0015	~0,006	0,013	0,023	0,061

Phase behaviour against heptane follows usual trends.

**II- phase behaviour gives low IFT near the three-phase region**

EOP: excess oil phase  
MEP: microemulsion phase



# Correlation between solubility, retention and phase behaviour

NaCl wt%	0	1	2	3	4	5	6	7	8	9	10
Appearance	C	C	C	C	P	P	T	P	P	P	O
Activity	100	100	100	100	79	97	100	98	98	98	11
Retention (mg/g)		0,14		0,15			1,5			1,76	
IFT (mN/m)	2,18	0,46	0,21	0,075	0,077	0,05	0,0015*		0,013	0,023	0,061
Phase behaviour				WII-			WIII	WIII	WII+	WII+	WII+

\* IFT at  $S^* = 6.6$

Alternative?

Ultralow IFT, BUT poor solution properties and high retention

Other use of surfactants for reducing IFT may be more efficient and economical than classical MPF or surfactant flooding

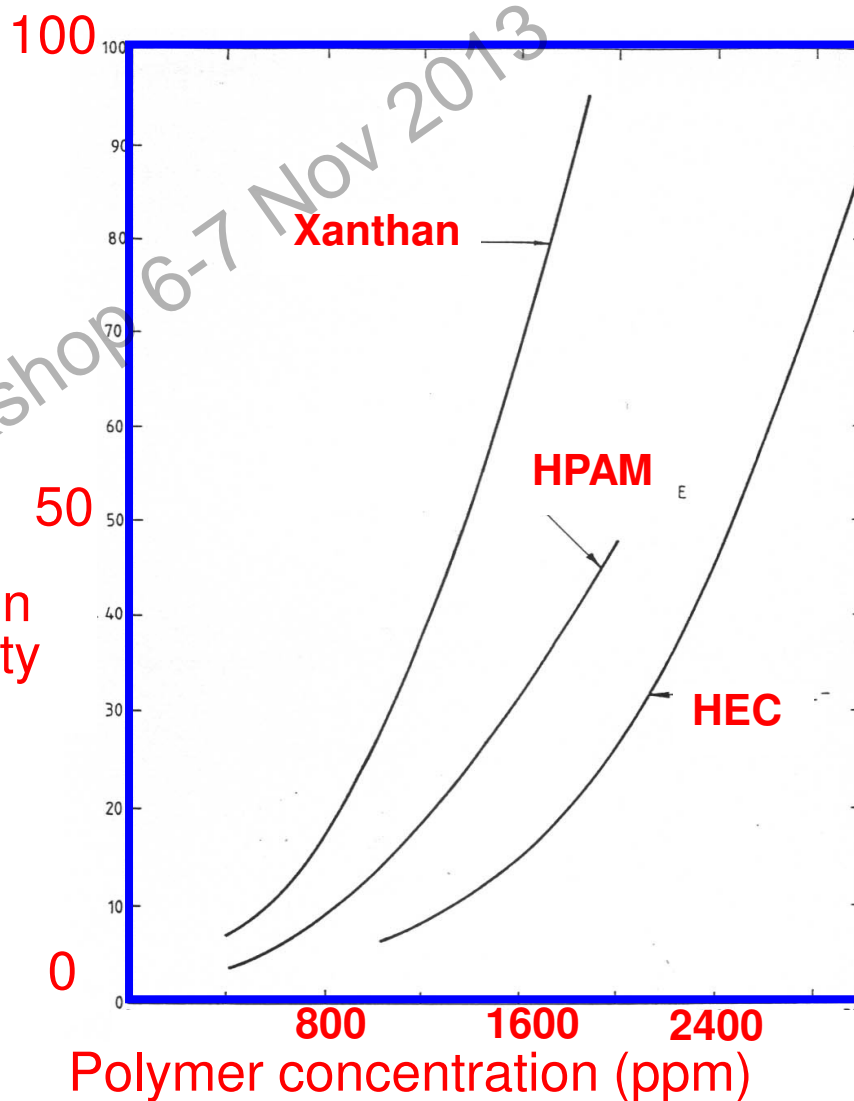


# Improving Vertical and Areal Sweep Efficiency: by increasing water viscosity using polymers

Comparison of viscosities of  
three types of polymers in  
1.0% NaCl at 74°F

- Xanthan - a biopolymer
- HPAM - hydrolysed polyacrylamide
- HEC - hydroxy ethyl cellulose

Solution  
viscosity  
(cp)



# Daqing Polymer Injection

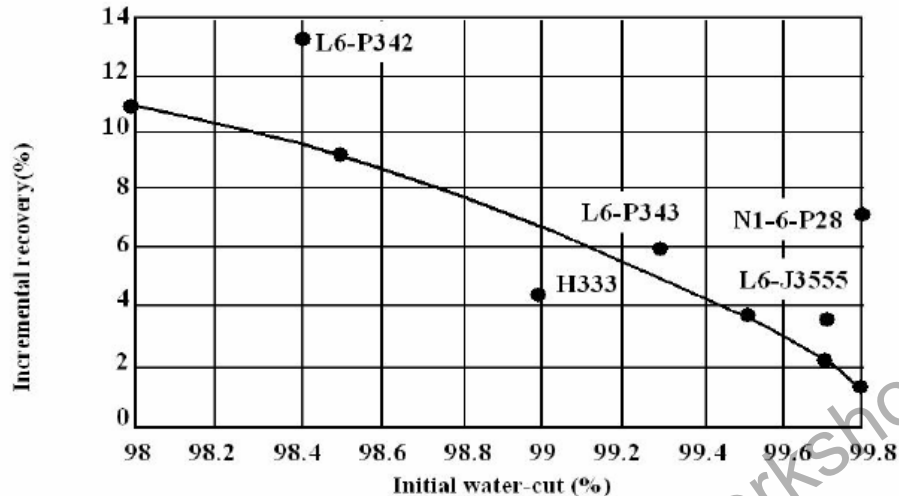


Fig. 7 Relationship of incremental recovery by polymer flood versus initial water-cut

## Project Description:

- Over 2000 wells now injecting polymer at Daqing
- Typical slug size is 0.6 PV
- Most well patterns are 5-spot
- about 30-50% of injected polymer is produced
- maximum produced polymer conc. is approx. 2/3 of injected

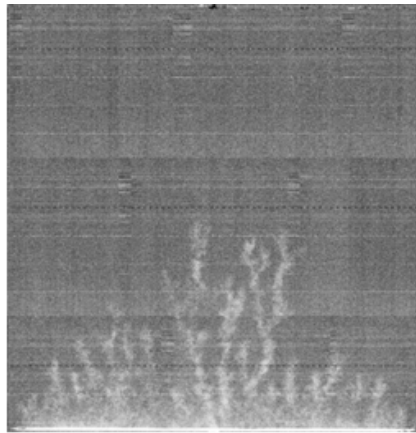
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## Lessons Learned:

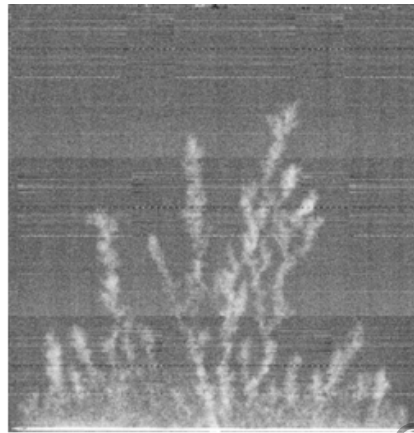
- Higher initial water cut results in lower incremental gains in recovery (see figure to left)
- The total cost of polymer flooding (\$6.60/bbl inc. oil) is actually less than for waterflooding (\$7.85/bbl inc. oil) due to decreased water production and increased oil production.
- More heterogeneous reservoir:
  - larger increase in sweep efficiency
  - shorter response time to polymer flooding
  - strongest influence on recovery is connectivity of pay zones
- To obtain higher recovery with polymer flooding:
  - lower producer WHP
  - stimulate producers
  - increase polymer concentration
  - increase polymer molecular weight



# Waterflooding at high adverse mobility ratio



0.01 PV



0.02 PV



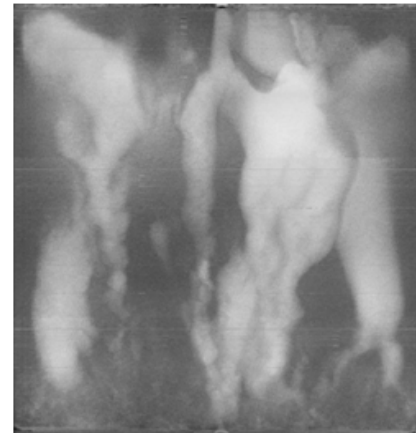
0.04 PV



0.14 PV



0.53 PV



2.3 PV

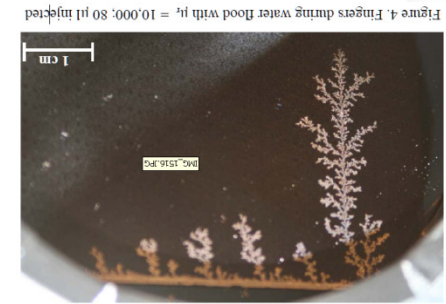
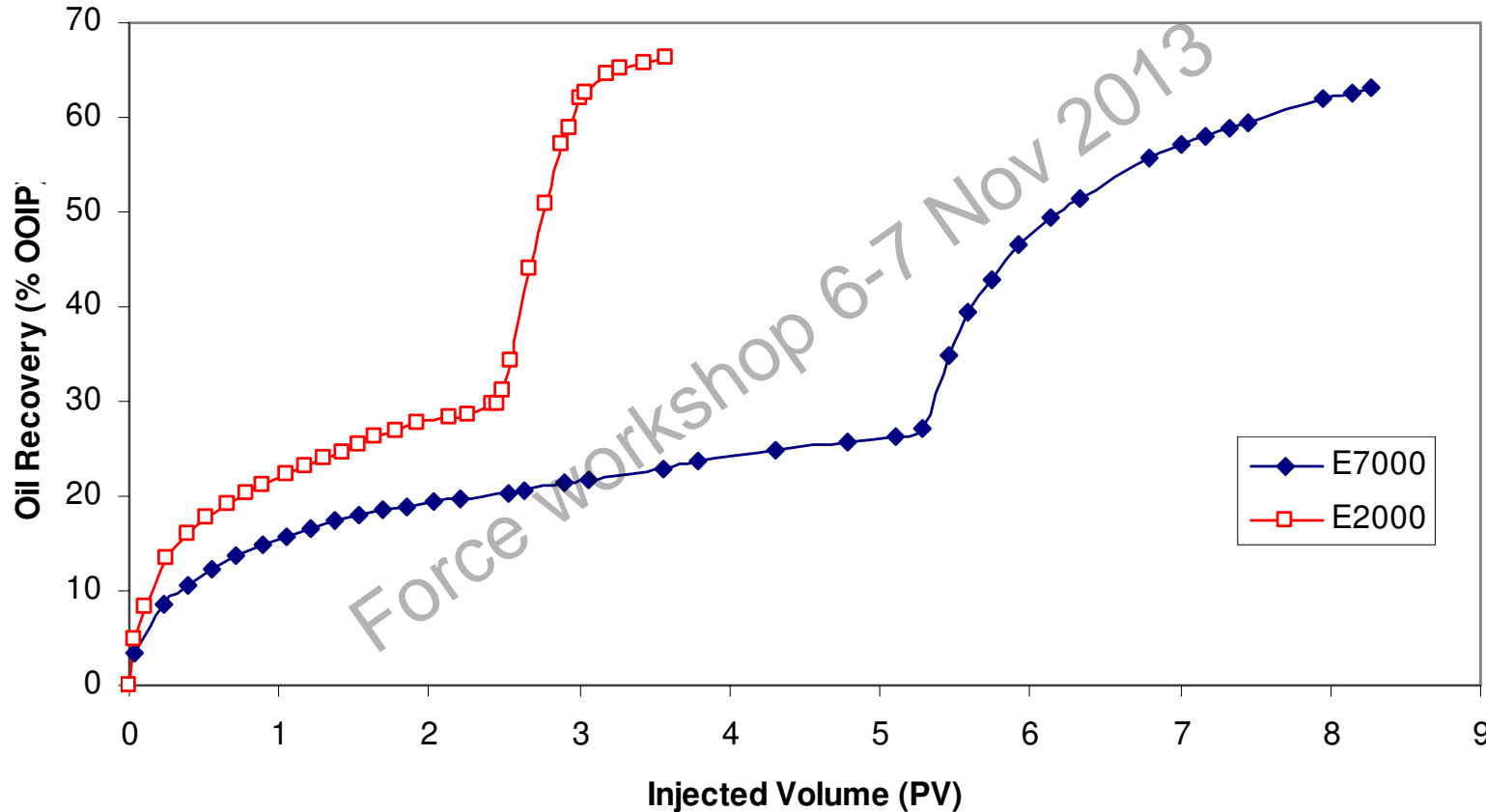


Figure 4. Fingers during water flood with  $\mu_r = 10,000$ ; 80  $\mu$ l injected

Mohanty et al 2012

Skauge, A., Ormehaug, P:A., Gurholt, T., Vik, B., Bondino, I., and Hamon, G., 2-D Visualisation of Unstable Waterflood and Polymer Flood for Displacement of Heavy Oil, SPE 154292, paper prepared for presentation at the Eighteenth SPE Improved Oil Recovery Symp. Tulsa, 2012

# Water- and polymer flood of viscous oils



Skauge, A., Ormehaug, P:A., Gurholt, T., Vik, B., Bondino, I., and Hamon, G., 2-D Visualisation of Unstable Waterflood and Polymer Flood for Displacement of Heavy Oil, SPE 154292, paper prepared for presentation at the Eighteenth SPE Improved Oil Recovery Symp. Tulsa, 2012

# Losal – Designer water – Smart water, etc

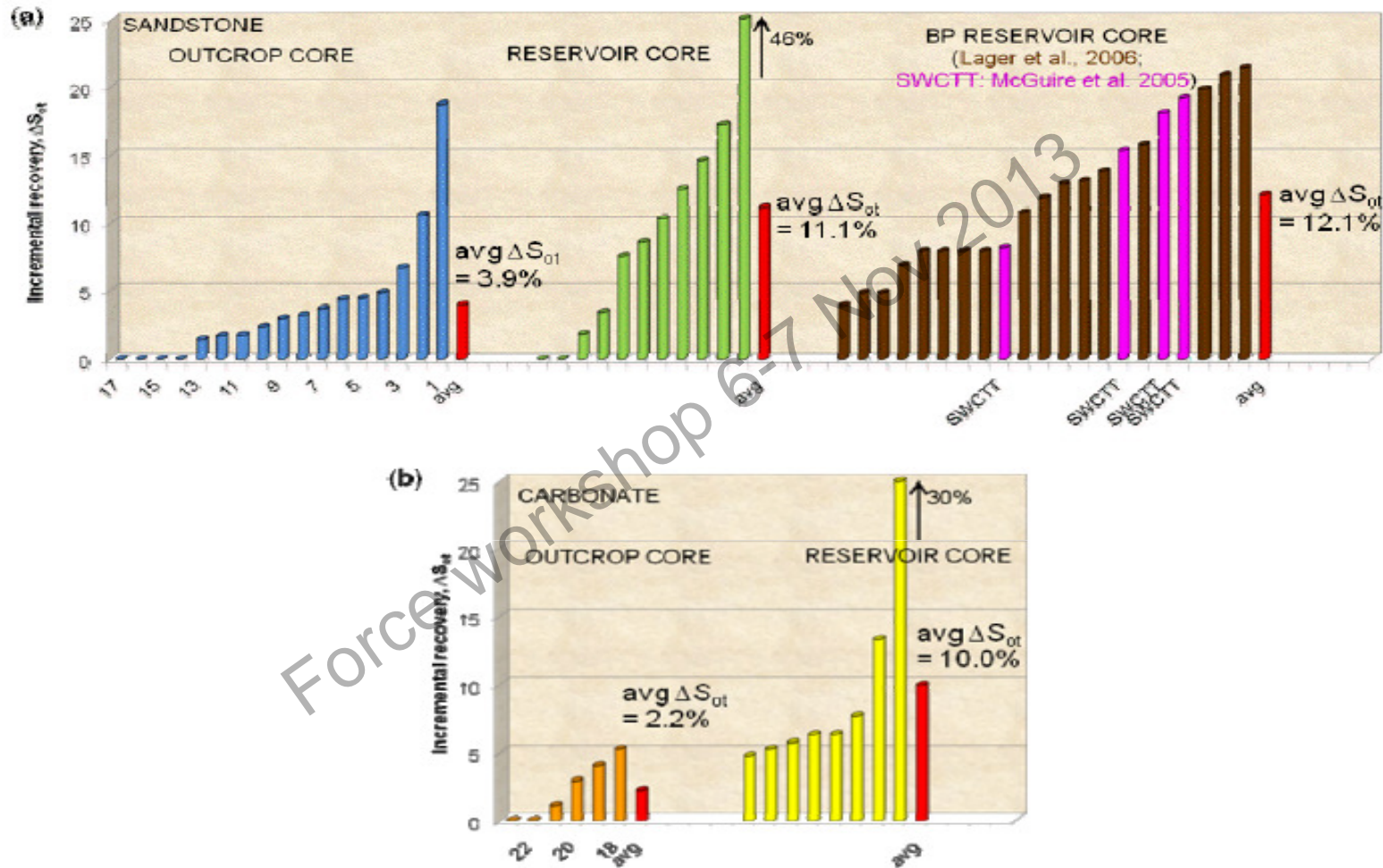


Fig. 6 Incremental tertiary recovery ( $\Delta S_{ot}$ ) by low salinity waterflooding: (a) sandstones and (b) carbonates. Average of 17 outcrop sandstones was 3.9%, for 11 reservoir sandstones was 11.1%, and 12.1% for literature data for reservoir cores or well tests. For outcrop carbonates the average was 2.2% compared to 10.0% for reservoir carbonates.

From Morrow et al paper SPE 154209, Tulsa 2012

# Low salinity waterflood

The key parameters or factors claimed to explain low salinity mechanisms for sandstones are:

*Multicomponent ion exchange*

*Double layer expansion*

*Fines migration*

*Wettability alteration*

*Microscopically diverted flow*

*Impact of alkaline flooding*

*pH driven wettability change*

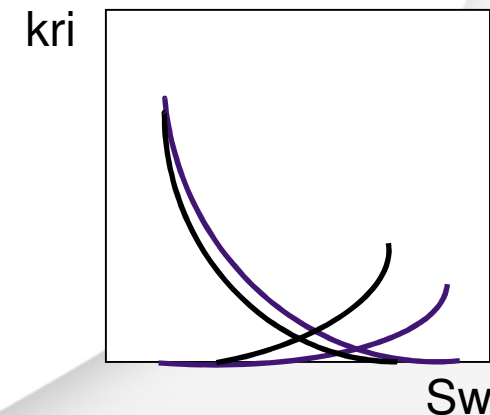
*Plus about 20 other suggestions in the literature*

# Low Salinity Simulation Approach: Eclipse

- **Brine Tracking option**
  - Salinity can modify brine properties
- **Low Salinity option**
  - Two sets of relative permeability and capillary pressure curves
  - $F_1$  and  $F_2$  is weighting factor

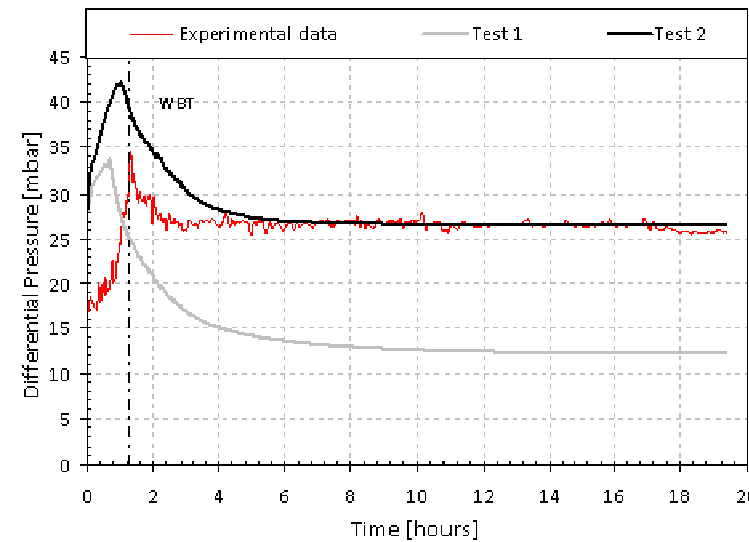
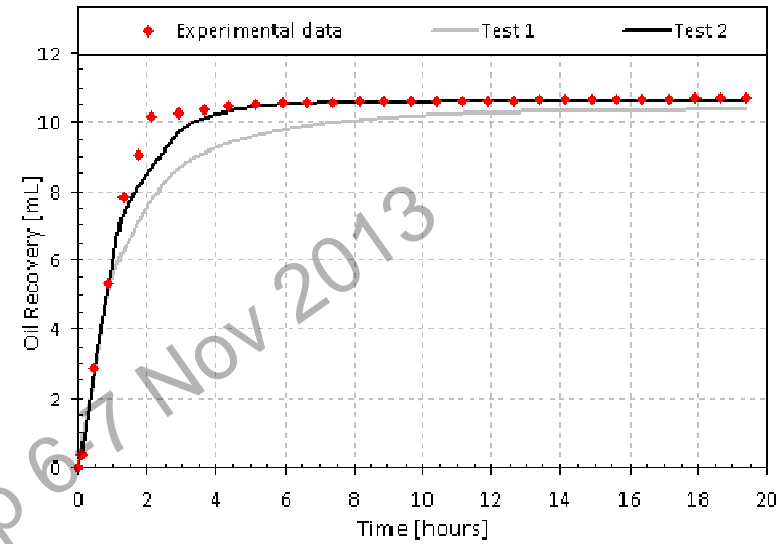
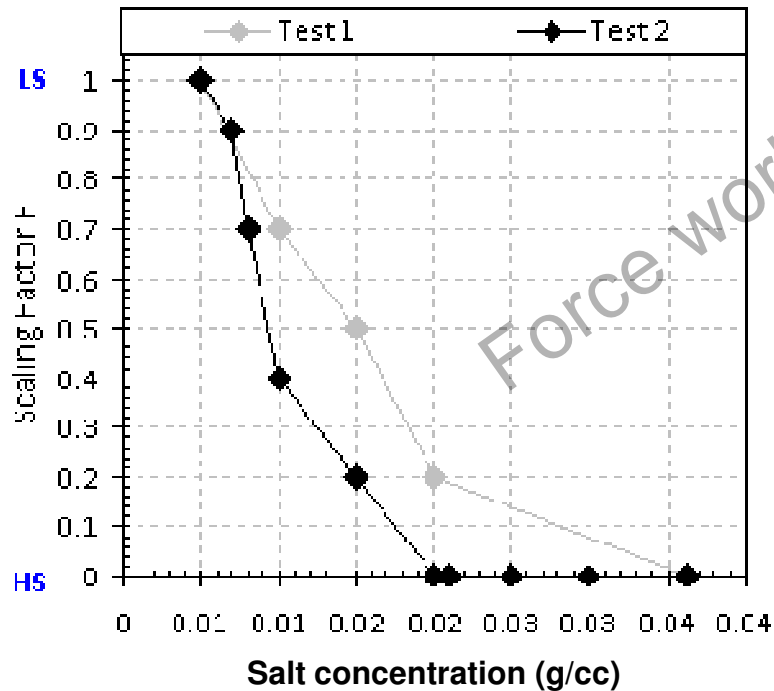
$$k_{ri} = F_1 k_{ri}^L + (1 - F_1) k_{ri}^H$$

$$P_{cij} = F_2 P_{cij}^L + (1 - F_2) P_{cij}^H$$



# Sensitivity tests on the rel perm F<sub>1</sub> - factor

$$k_{ri} = F_1 k_{ri}^L + (1 - F_1) k_{ri}^H$$





## **New combination of EOR methods**

**Low salinity waterflood may give only modest improved oil recovery for many sandstone reservoirs**

**Cost of reducing water salinity may be a show stopper**

**Recent research has made a combined low salinity and surfactant flooding a way of boosting oil recovery and improve the economy of this EOR process**

### **Source:**

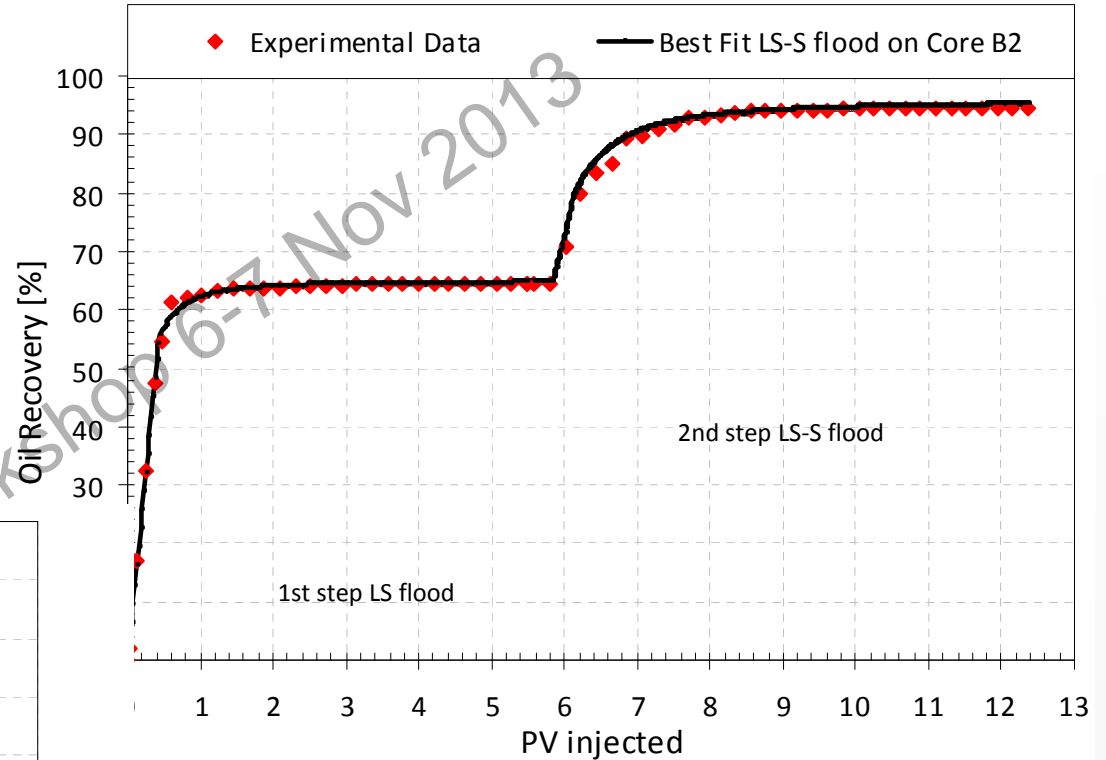
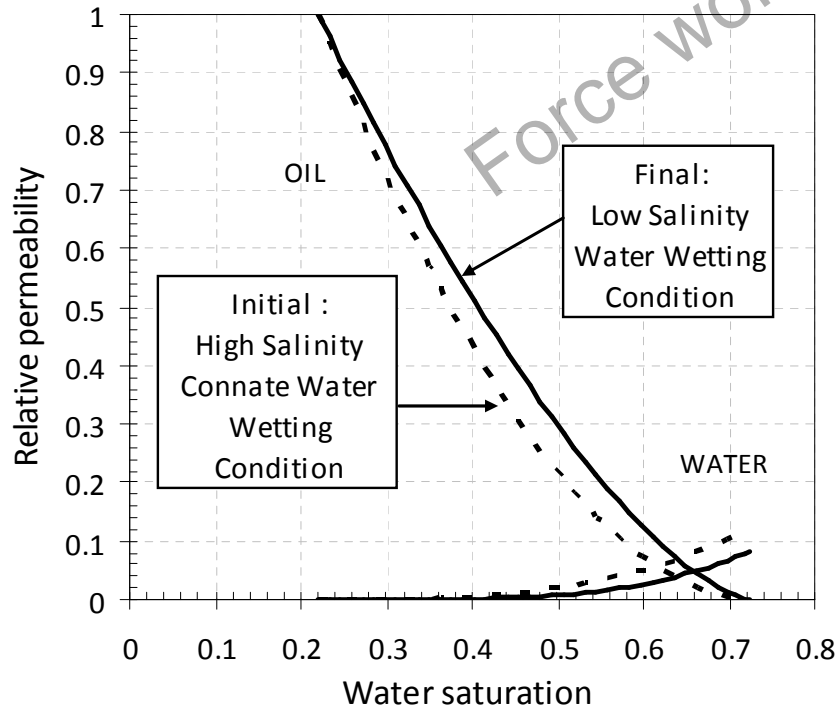
**Alagic and Skauge (CIPR): “Change to Low Salinity Brine Injection in Combination with Surfactant Flooding,” presented at 15th European Symposium on Improved Oil Recovery — Paris, France, 27 – 29 April 2009**

# Low Salinity Surfactant Flooding

- Surfactants targets the residual oil by reducing IFT
- Advantages in low salinity environment
  - Combined effect (low salinity effects at low IFT)
  - May reduce re-trapping of mobilized oil
  - Reduced adsorption / retention
  - More low cost surfactants available



# UTCHEM Simulations: LS flood → LS surfactant flood



**Good simulation match  
of production data**

Skauge, A., Ghorbani, Z., and Delshad, M., Simulation of Combined Low Salinity Brine and Surfactant Flooding, (Sub ID: 9874), the EAGE IOR Symposium 12th – 14th April 2011 in Cambridge, UK.



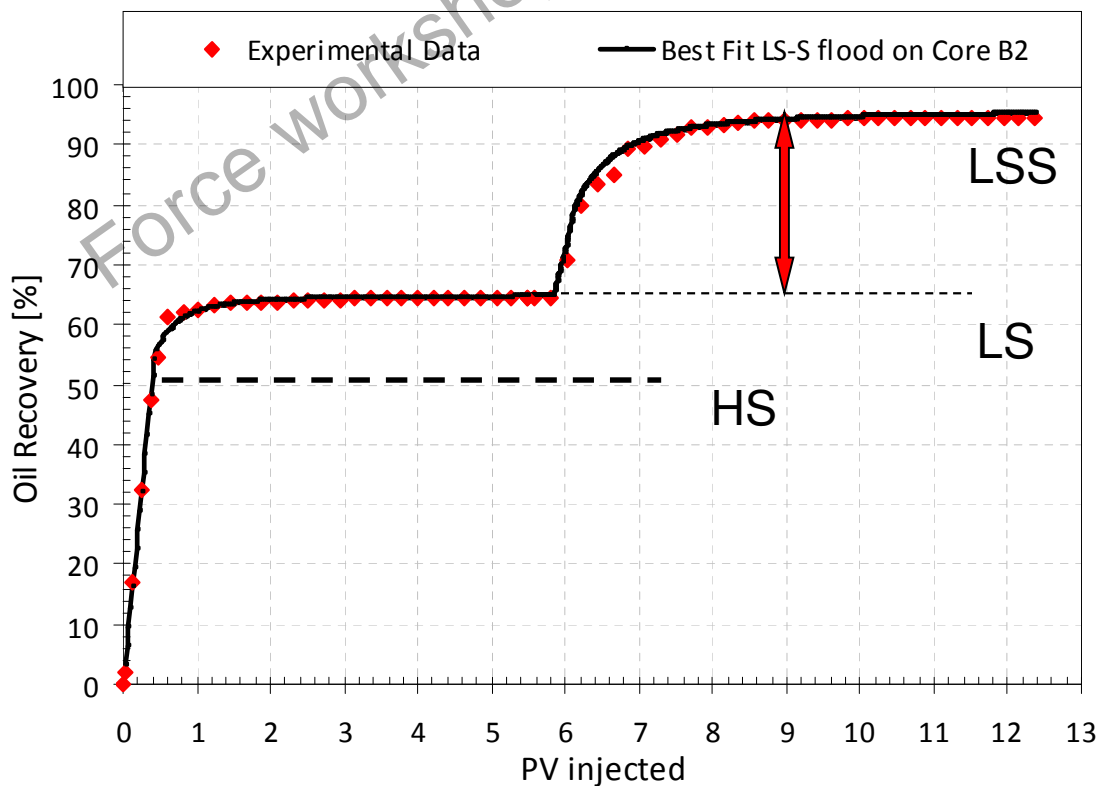
# Advantage of the combined EOR methods

Low salinity reduces surfactant retention

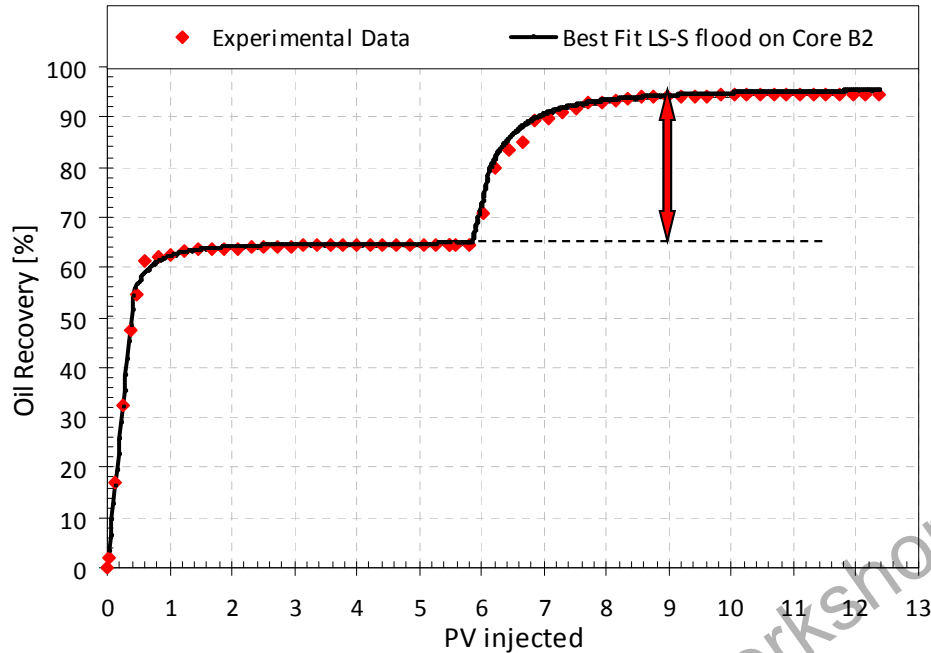
The combined process can mobilize most of the oil in place in lab core flood experiments

Low cost surfactants can be used at these salinities

Low sal surfactant

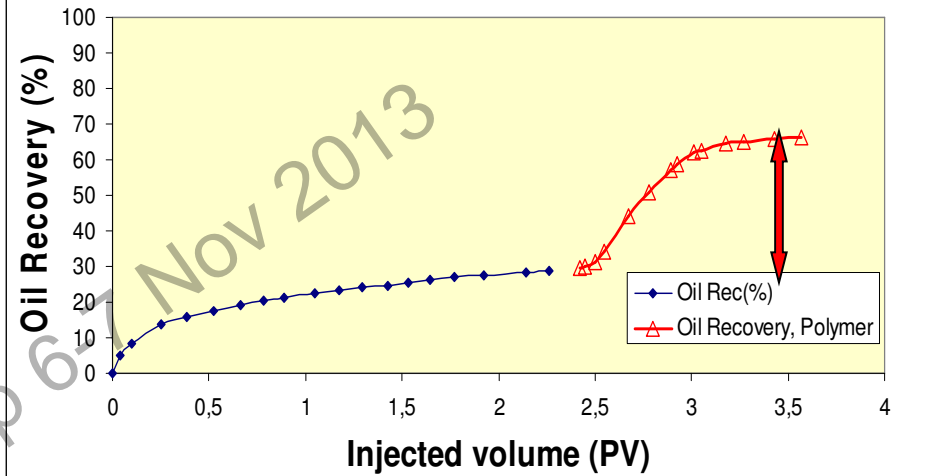


## Low sal surfactant

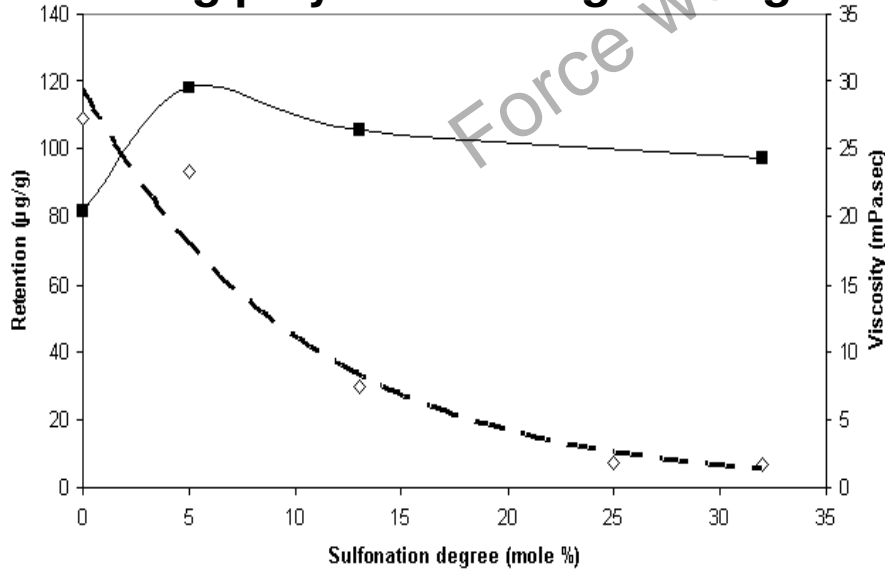


## Polymer for heavy oil recovery

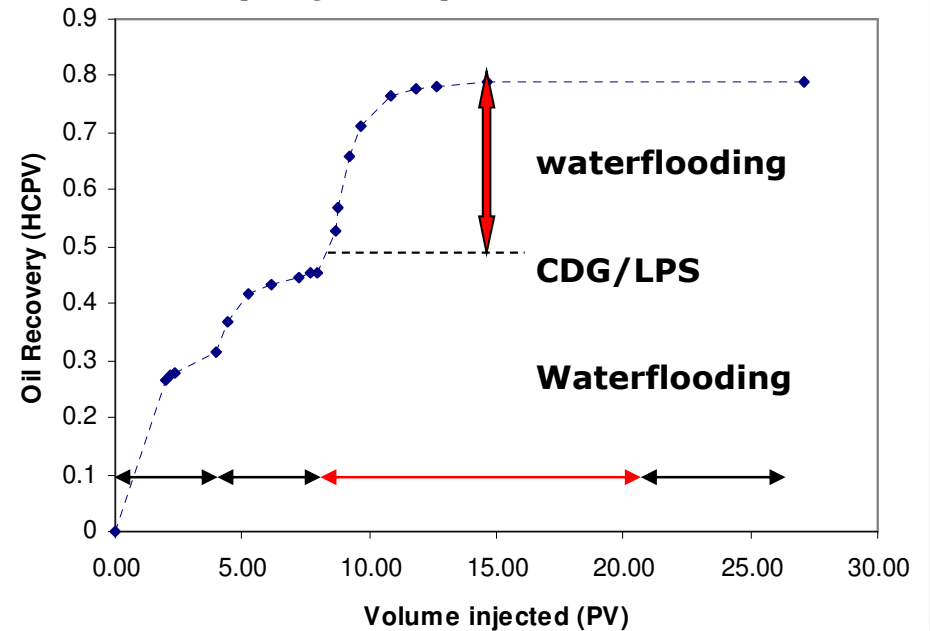
### Oil recovery from water and polymer injection



## Extending polymers for high sal og temp



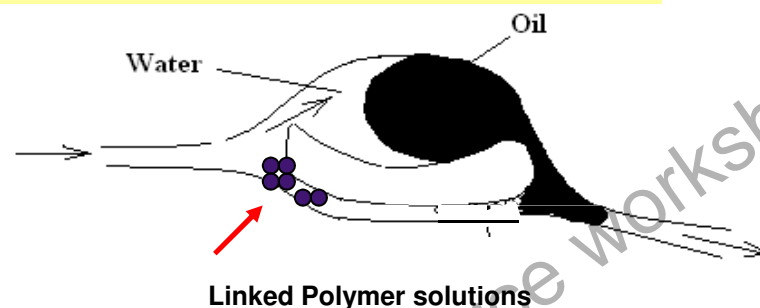
## Nano polymer particles for EOR



Nano particles mechanisms sweep improvement, but also..



**Microscopic diversion**



**Spherical particles**

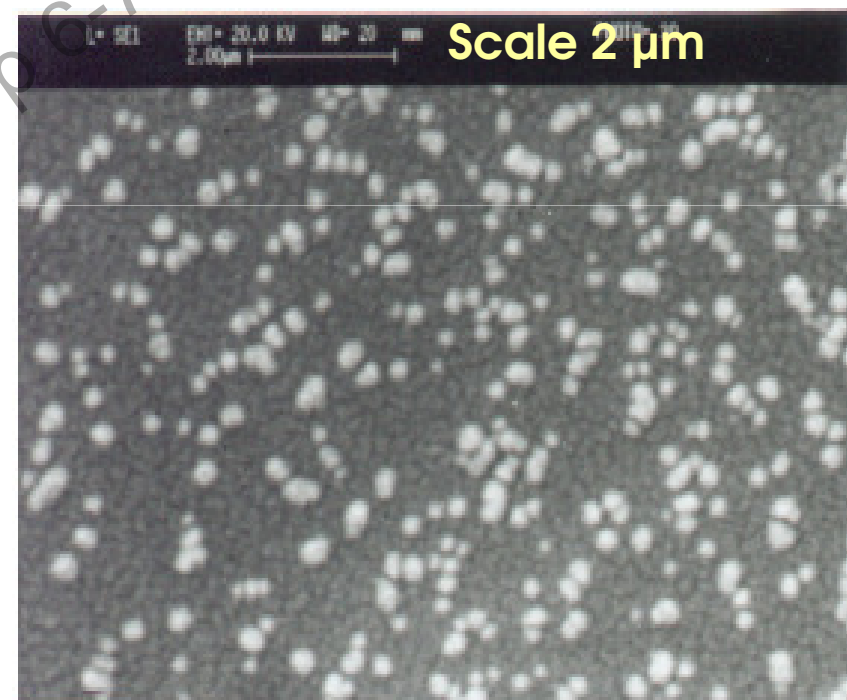
**Typical size 50-100 nm**

**Pre-generated particles;**

1. Less likely to be adsorbed
2. Expect less chromatographic separation

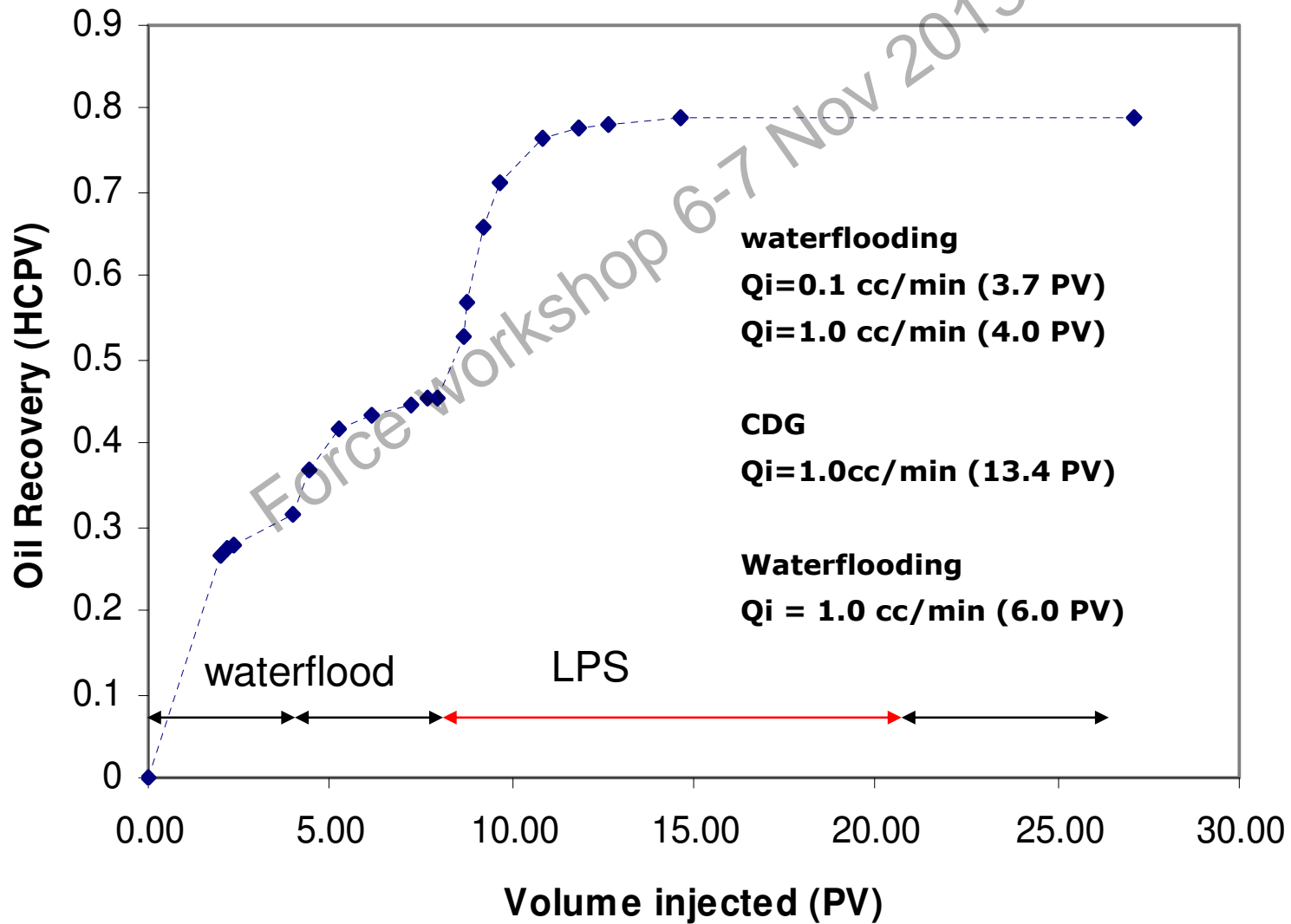


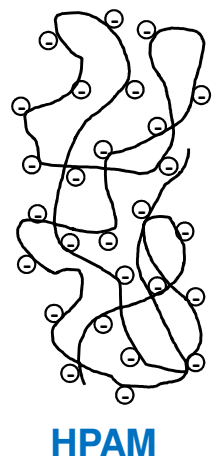
**SEM photograph of CDG particles**



# LPS in core flood

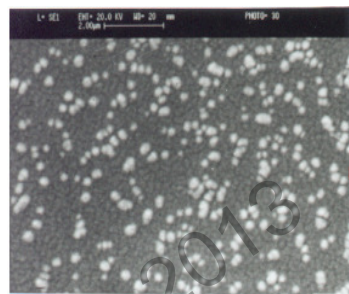
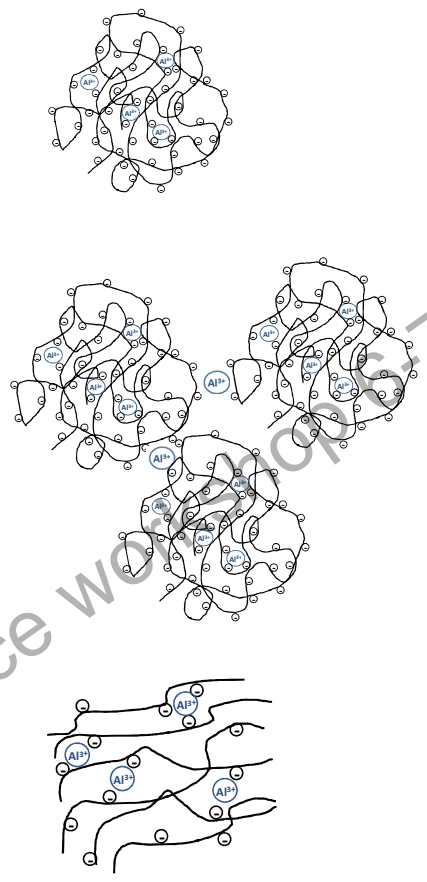
Sandstone reservoir core (fresh core),  $K=900$  mD



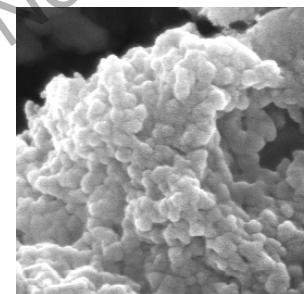


Intra-molecular

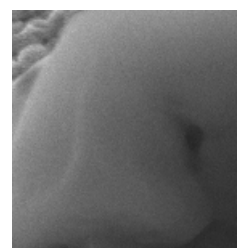
Inter-molecular



Coiled polymer (LPS) particles



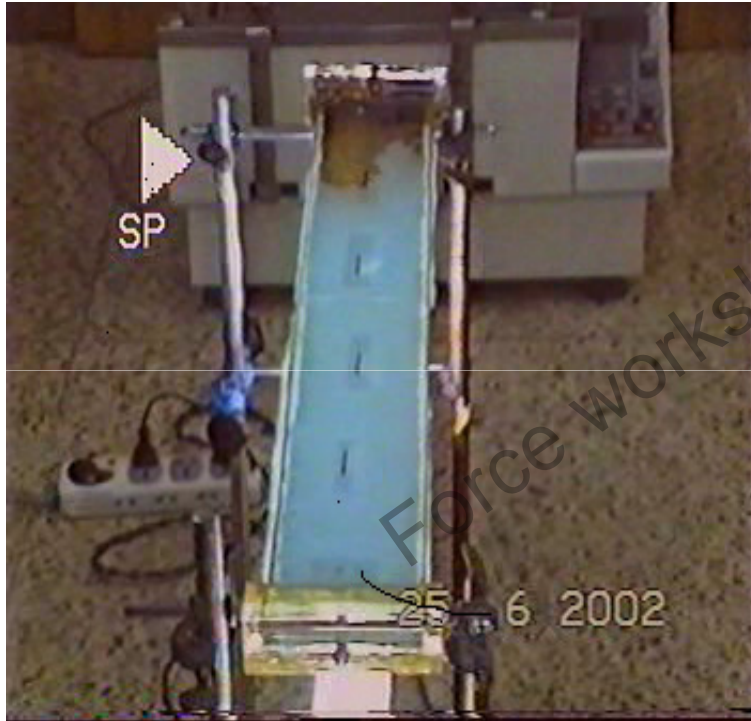
Coil Aggregates



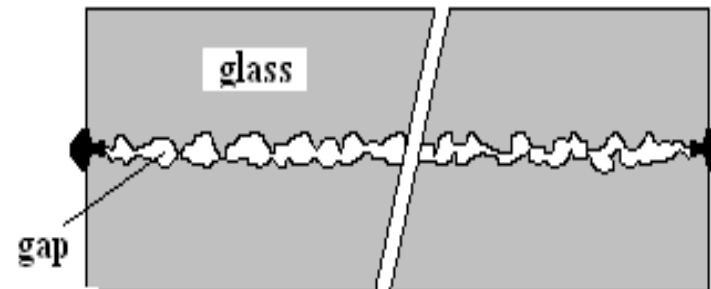
Polymer gel

**Intra-molecular aggregate is preferred**

# LPS flooding in a glass model



Heterogeneous etched pores on glass plates



L: 625 mm W: 100 mm Gap: 50-100  $\mu\text{m}$

**Experiments show that water after LPS injection is following new pathways and is mobilising bypassed oil**

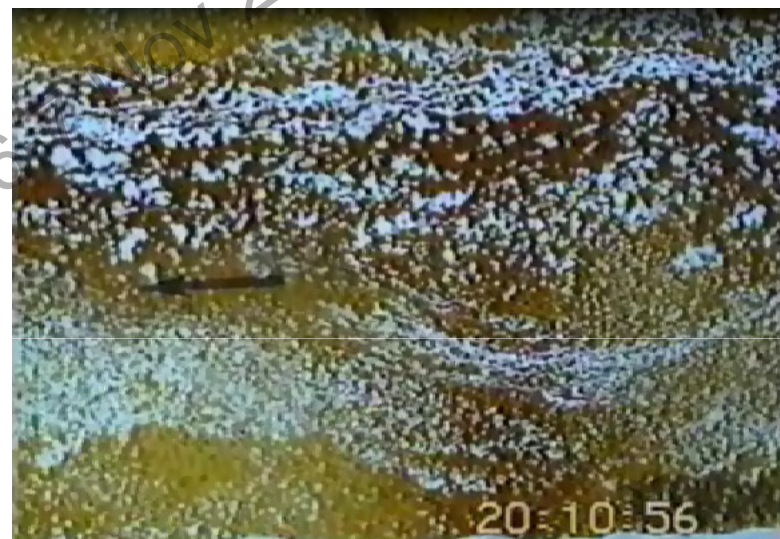




Waterflooding at adverse mobility ratio



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After LPS injection water is contacting  
Initially bypassed pores



# Way forward

We will see more advanced flood sequences...

- Polymer - new development and possibilities (Yes)
- Low salinity (?)
- Classical surfactant flooding (?)

Hybrid EOR – **YES**

- Low Salinity Surfactant – Low Salinity Polymer even LSASP  
– Low Salinity Low Tension Gas - Nano particle polymers
- Foam/Polymer – Nano stabilized foam- Low Tension Gas –  
WAG – Foam Assisted WAG (FAWAG) and more.....

# Thank you

Nov 2013

