



*The World Leader in Polymer Technology
For Enhanced Oil Recovery*

**Injection of polymer solution
From surface to wellbore**

Mechanical and Chemical degradation

*NPD, Stavanger
30th May, 2011*

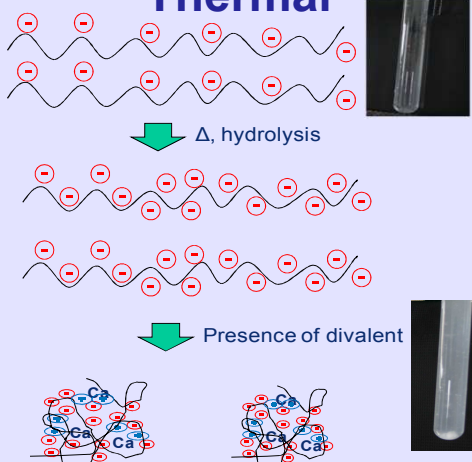
Introduction

- What are the possible degradations and the way to minimize them
- Chemical degradation : problem of Oxygen in presence of Fe 2+ or H₂S
- Mechanical degradation :
 - Where : pump, ICD , perforation
 - How to minimize them

Possible degradations

Factors influencing polymer solution viscosity

Thermal

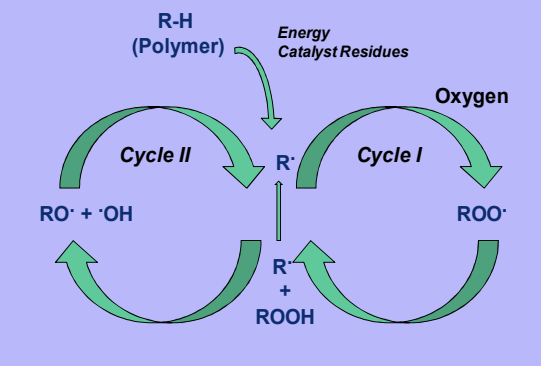


Why : high Temp., pH

Problems : more sensitive to Ca, Mg - viscosity drop, precipitation

Solution : adapt chemistry of polymers, water treatment (softening, anti scaling)

Chemical

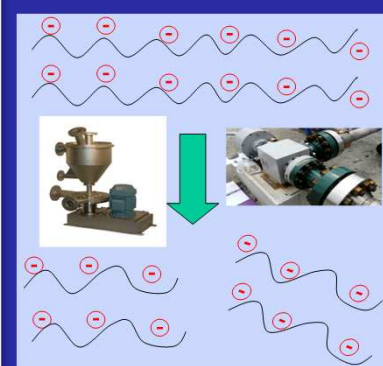


Why : Redox system, Fe^{II}/O_2 , H_2S/O_2 , weak links in the polymer, impurities

Problems : drastic Mw and viscosity drop

Solution : adapt chemistry and production process of polymers, use appropriate protective additives, remove contaminants (H_2S , O_2 , iron)

Mechanical



Why : mixing, transfers through pumps and gates, perforations

Problems : Mw and viscosity drop

Solution : PSU, Use of lower Mw

Biological



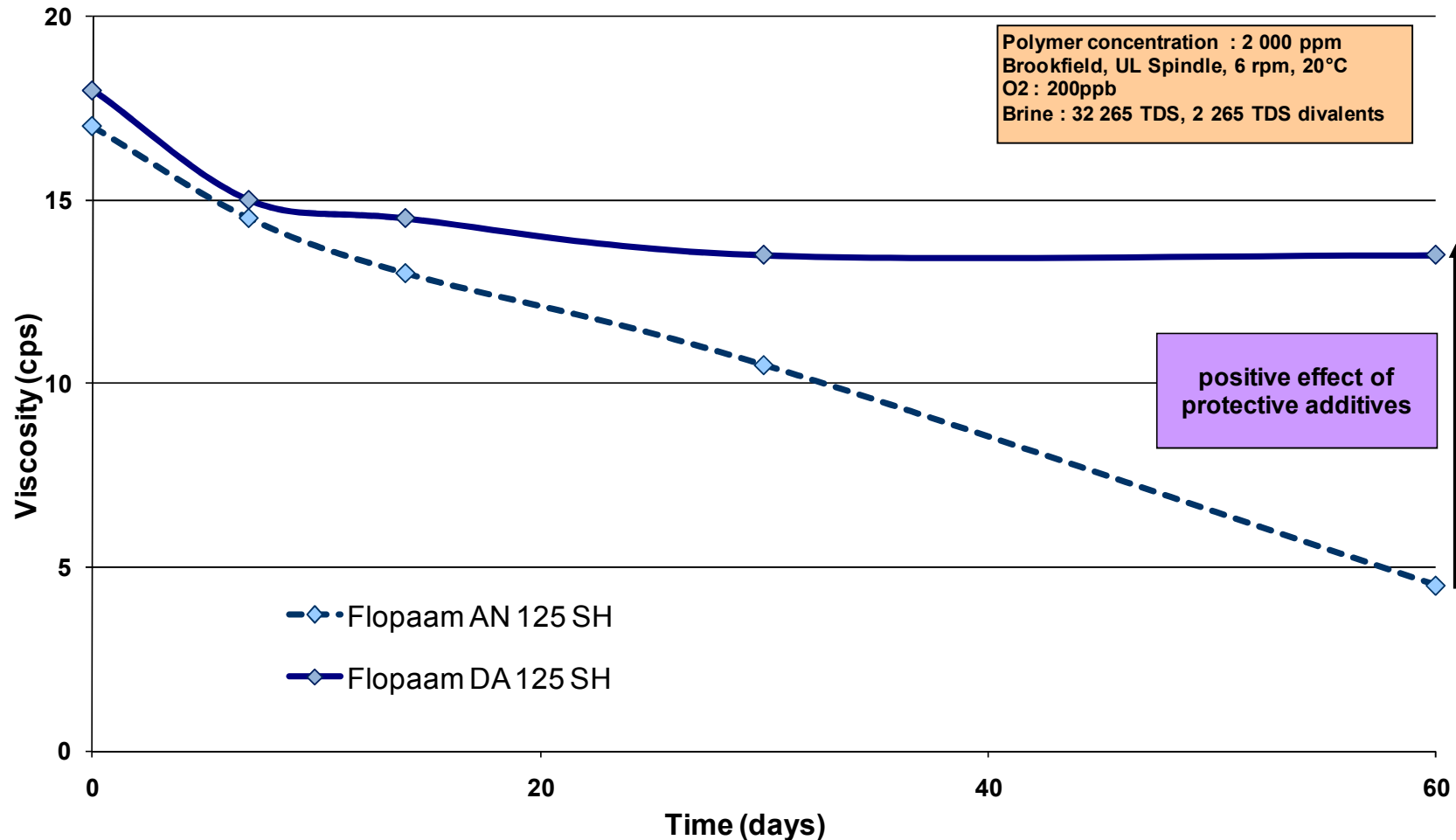
Why : Presence of Bacteria (SRB..)

Problems : Mw and viscosity drop

Solution : Use of biocides compatible with polymer and with deoxygenating system

Impact of presence of oxygen : efficiency of F3P

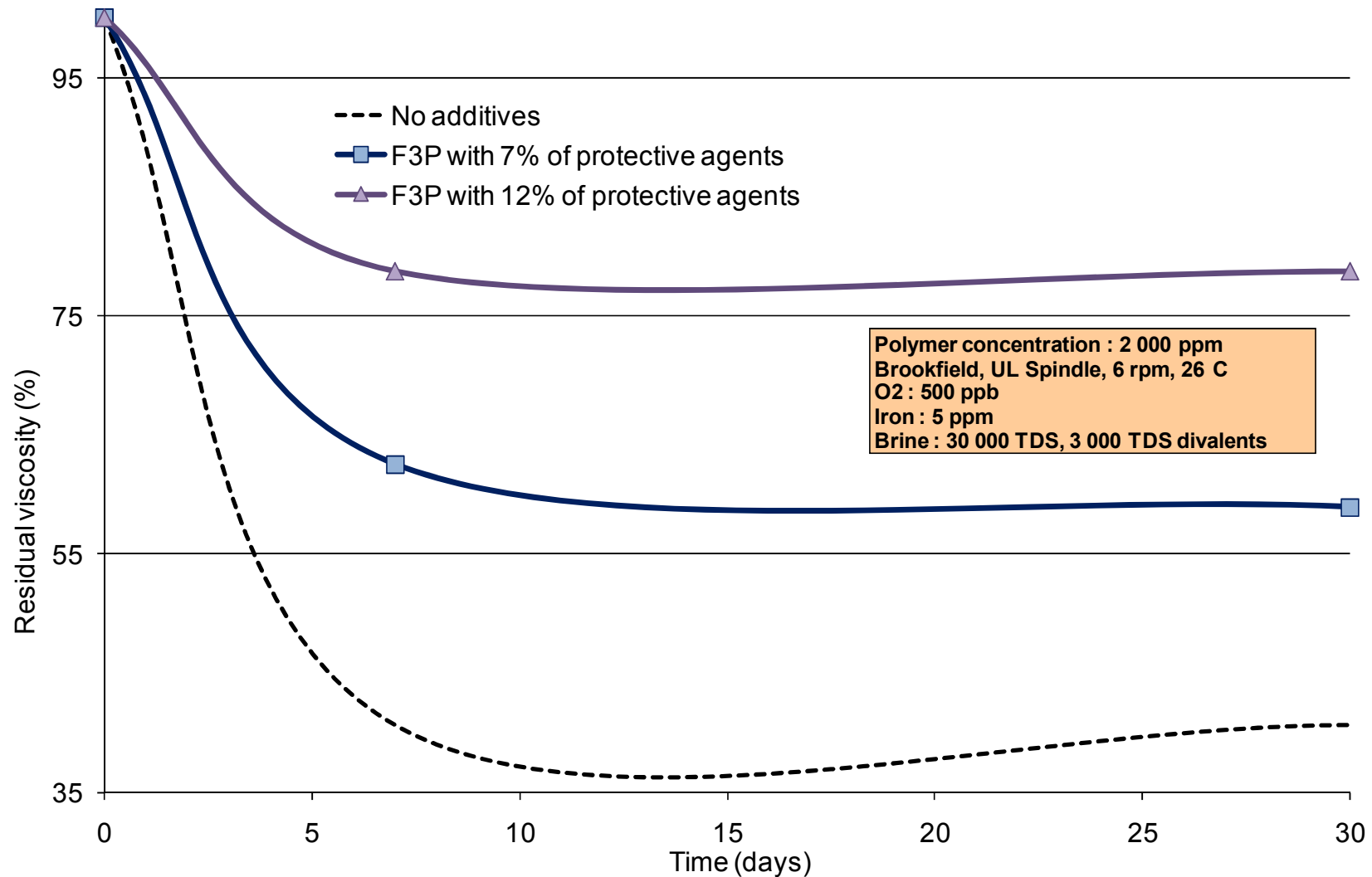
Evolution of viscosity of Flopaam™ AN 125 SH (ATBS/AMD copolymer) and corresponding F3P @ 100°C in presence of divalent cations



Contribution of hydrolysis to viscosity is lower than chemical degradation

The medium term effect of Fe II and O₂ : 30 days

80°C - poly(acrylamide-co-acrylic acid) Flopaam 3630S type
500 ppb O₂, 5 ppm Iron II, synthetic sea water

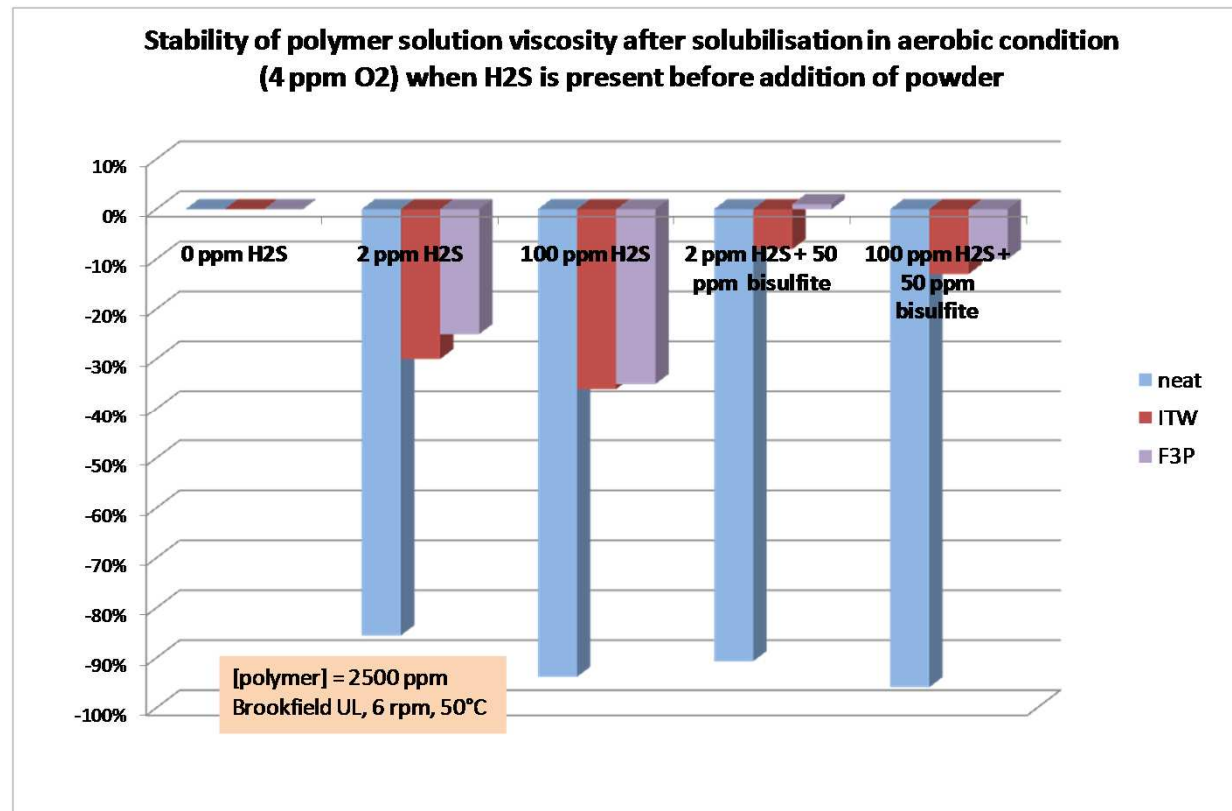


The immediate effect of H₂S and O₂

Impact of O₂ and H₂S

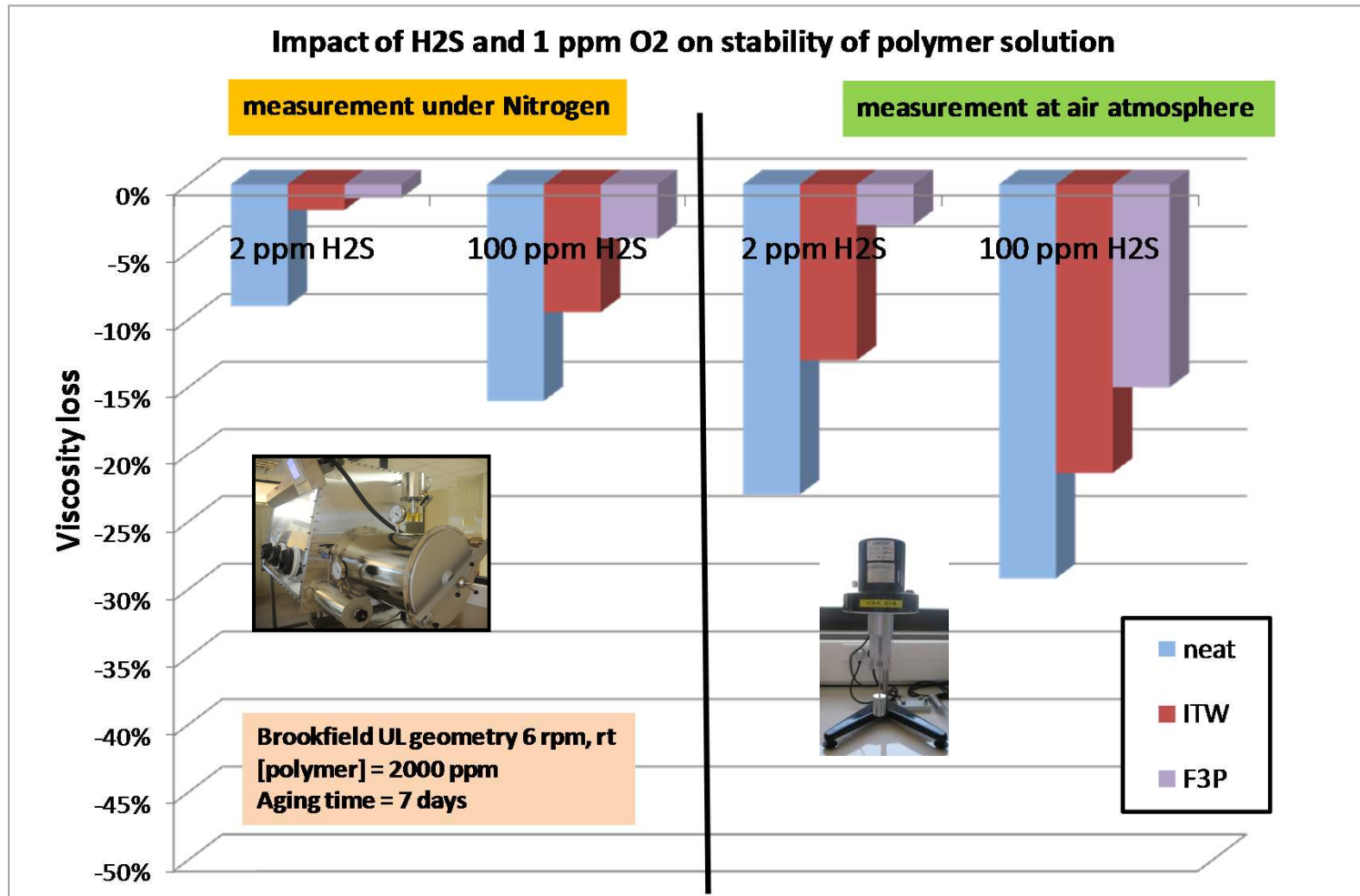
no nitrogen blanketing,
4 ppm of O₂ coming in the line
H₂S : 2 ppm and 100 ppm

dissolution of the powder in a vessel under air atmosphere in presence of H₂S



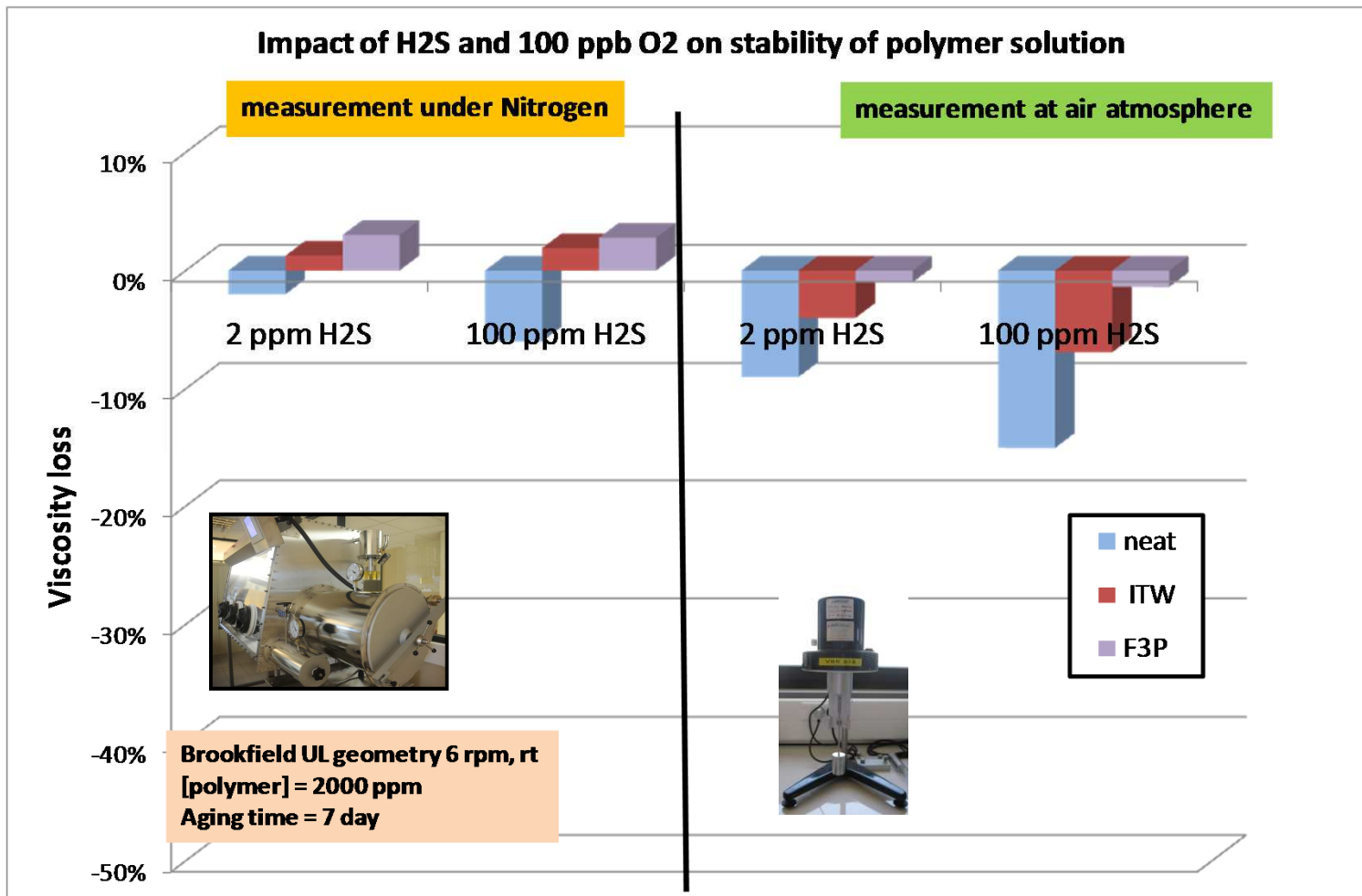
The medium term effect of H₂S and O₂

Aging results : 1 ppm of O₂
H₂S : 2 ppm and 100 ppm



Medium term effect of H₂S and O₂ (2)

Aging results : Low amount of O₂ : 100 ppb of O₂
 H₂S : 2 ppm and 100 ppm



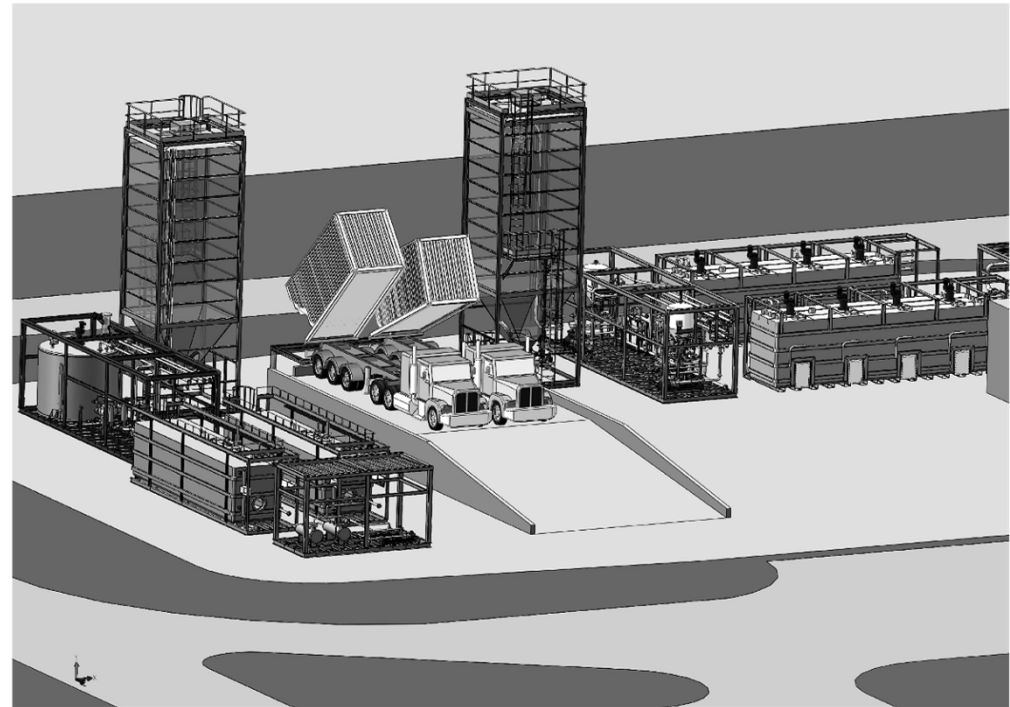
ITW vs. F3P

→ **ITW** (Mixture of isopropanol 15% / Thiourea 7.5% and water 77.5%)

→ Require storage, dosage and separate injection each component

- ITW : HSE issues**
- Harmful
 - Flammability
 - Environment (spills, odor, etc)

ITW is efficient but induces limitations to be implemented in every EOR projects



- F3P are ECONOMICAL**
- Price of additives
 - No limitations Number of additives
 - No additionnal supply chain
 - No additionnal Handling & Storage
 - No additionnal Injection facilities

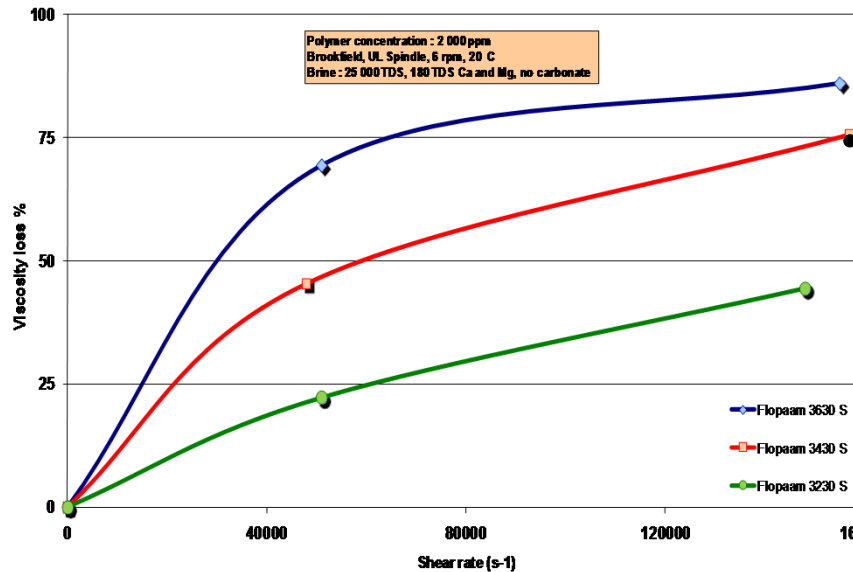
	FP3630S + ITW	F3P
Labeling polymer	none	none
Labeling IPA	Xi, F, R36, R67, Fp = 12°C	
Labeling thiourea	Xn, R40, R63, R51/53	

Mechanical degradation

- Where :
 - Pumps
 - Choke , Manifold
 - Completion : ICD
 - Perforations

Influence of shear rate in function of MW

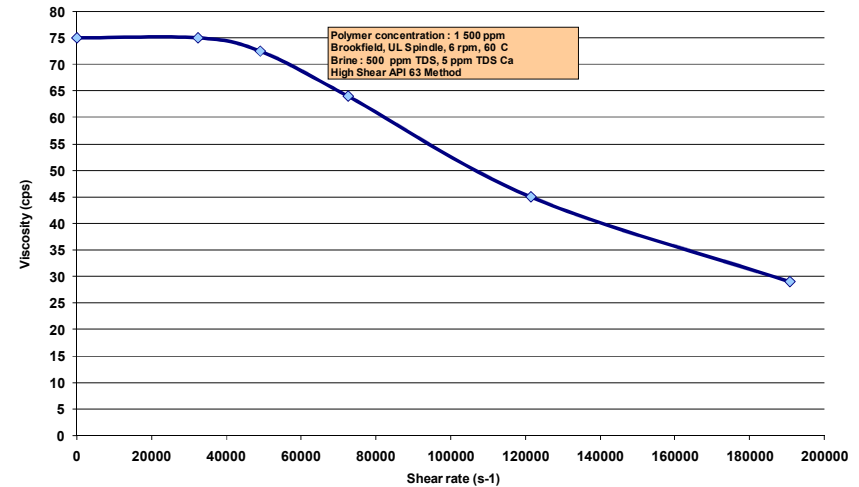
Impact of shear rate on viscosity loss % on poly (acrylamide-co-acrylic acid)
 Flopaam 3630 S - Flopaam 3430 S - Flopaam 3230 S types



The lower is the molecular weight , the lower the degradation is.

The optimum MW is maybe not the highest one in term of recovery and economics.

Impact of shear rate on viscosity on poly(acrylamide-co-acrylic acid)
 Flopaam 3230 S type

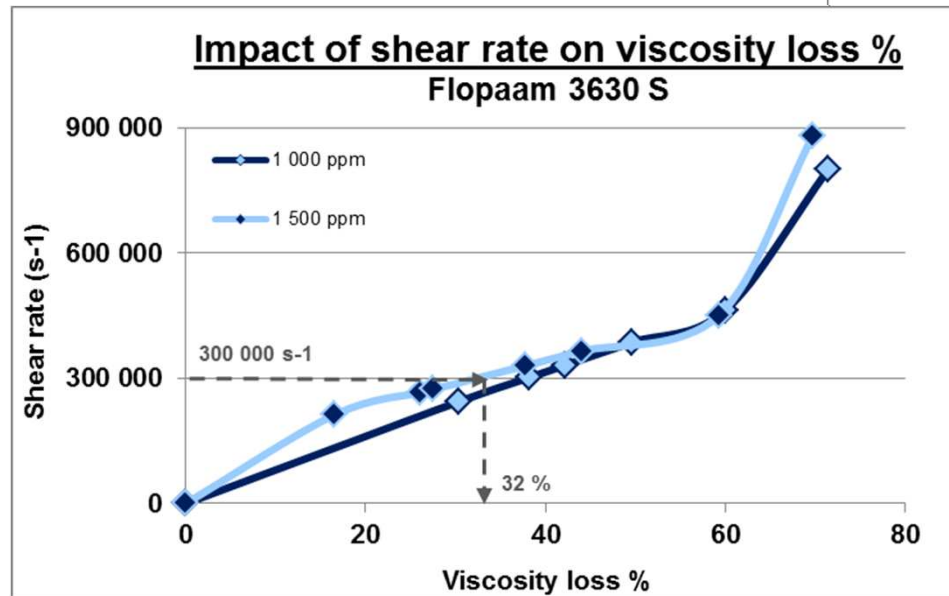
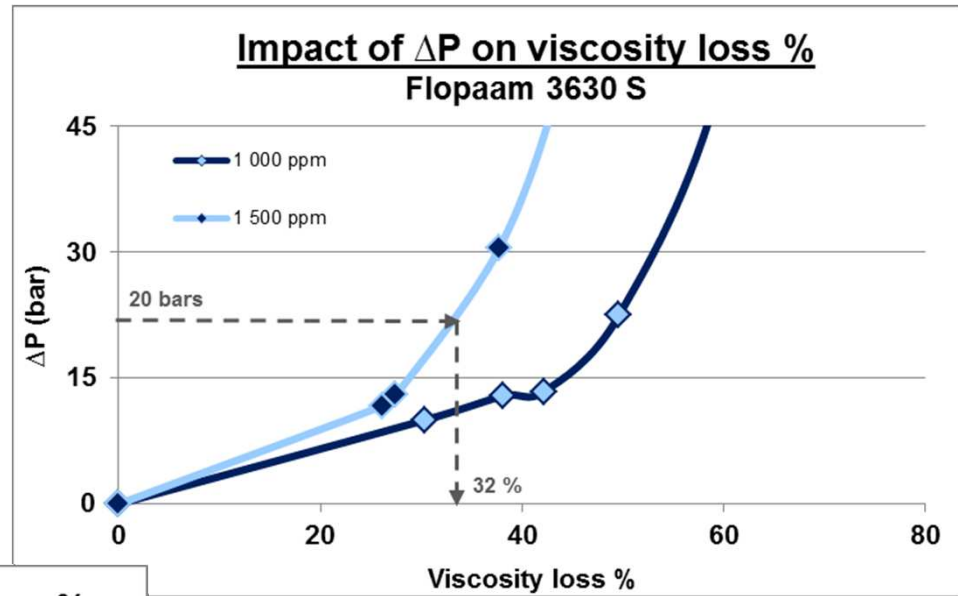


Pumps

- Centrifugal pumps cannot be used for polymer solutions
- Overall degradation of the solution going through the pump and the choke is directly linked to the pressure drop applied to the solutions
- Triplex pump is leading to almost no degradation.
- PCP pumps need to be carefully selected :
 - Degradation is limited (less than 10%) if the correct rotor is used
 - This is due to internal leakage of the solution in the chambers of the pump
 - Internal leakage is specific to each solution and is linked to the discharge pressure drop

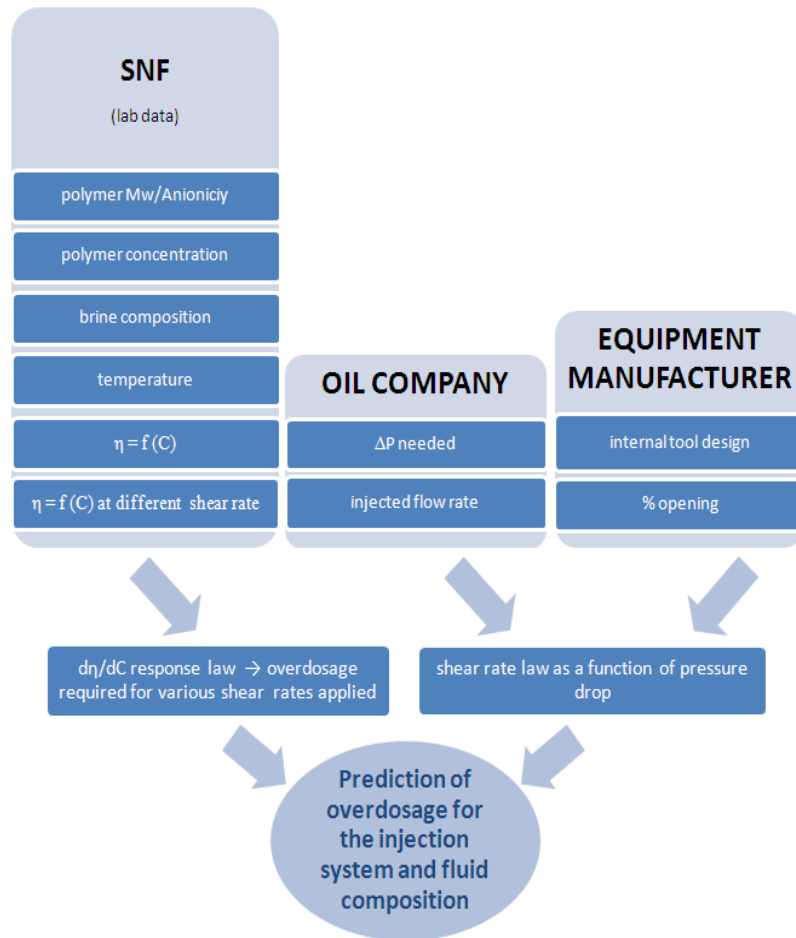
Chokes

Impact of pressure drop on viscosity is very important



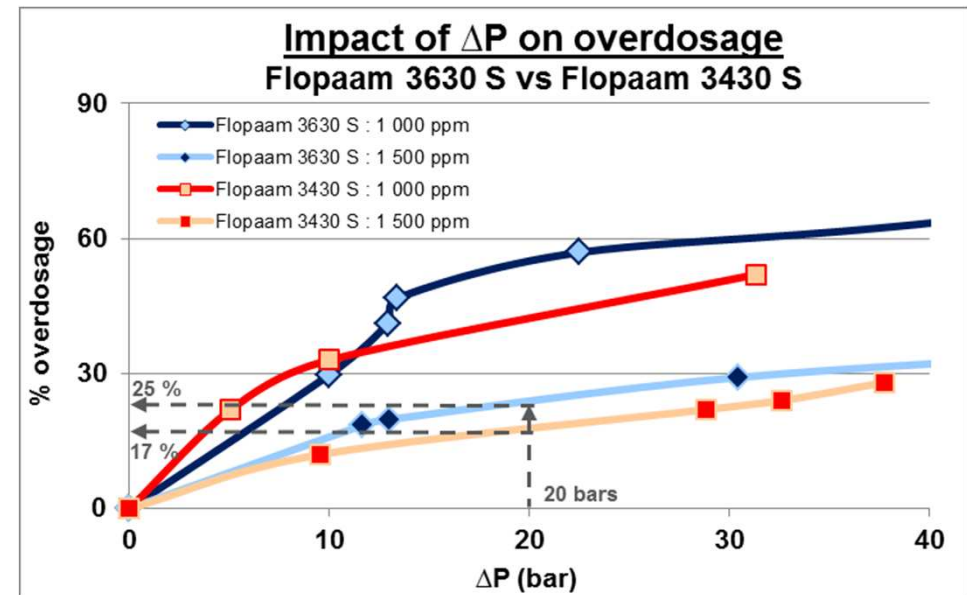
A 300,000 s-1 shear rate leads to a 32% viscosity reduction.

Chokes : Overdosage



Typical data generated with 2 polymers at 2 concentrations, for a given choke design and opening

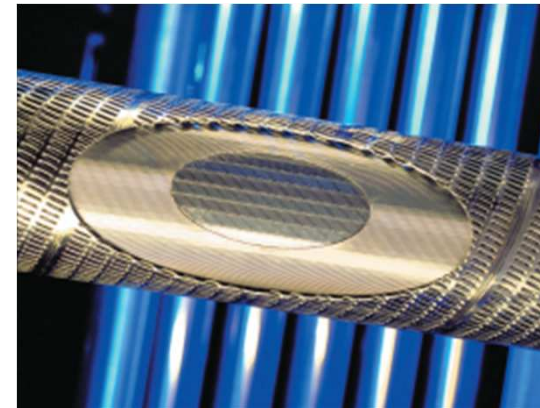
This choke required a 15 to 60% overdosage depending on the pressure drop. The overdosage is reduced for lower MW.



ICD and screen liner

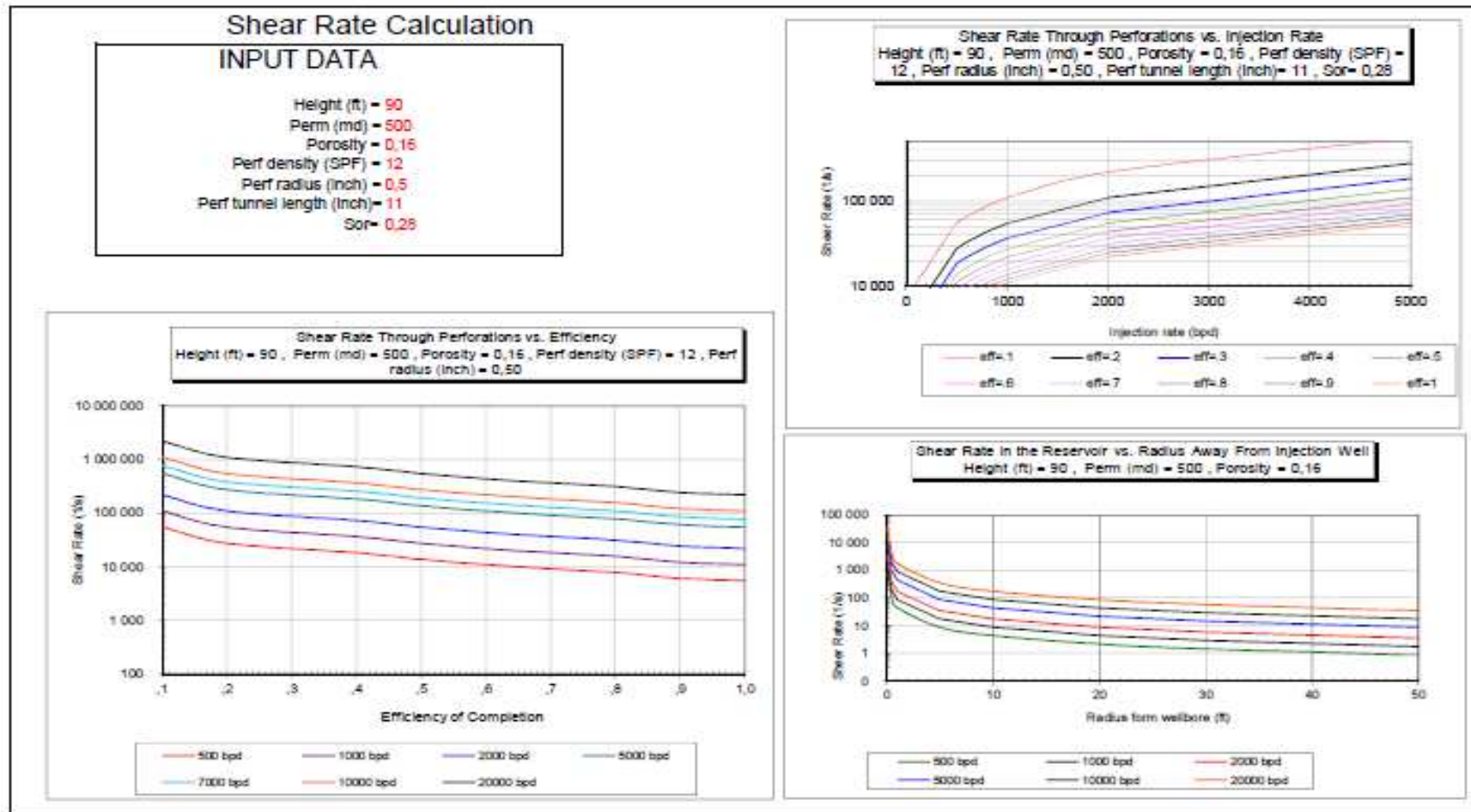
- **An ICD implementation must take into account parameters such as number of nozzle, size of nozzle, flow rate, but is manageable to minimize degradation**
- **Wire wrap liner**

Tests performed indicated no degradation through this completion liner.
Even if flowrate was 35 times the one expected, the degradation was less than 10%



Perforations

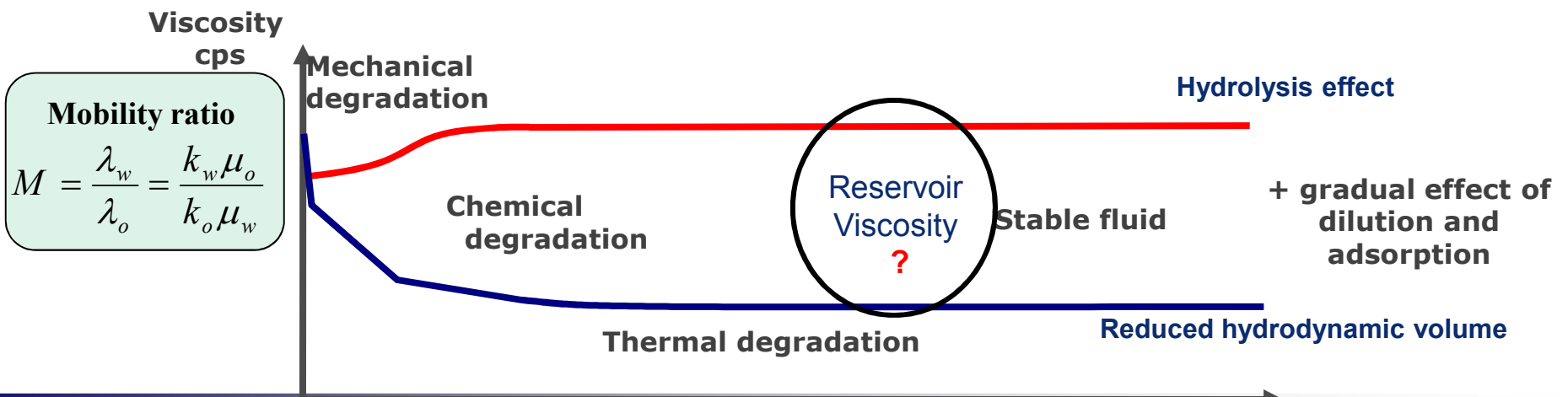
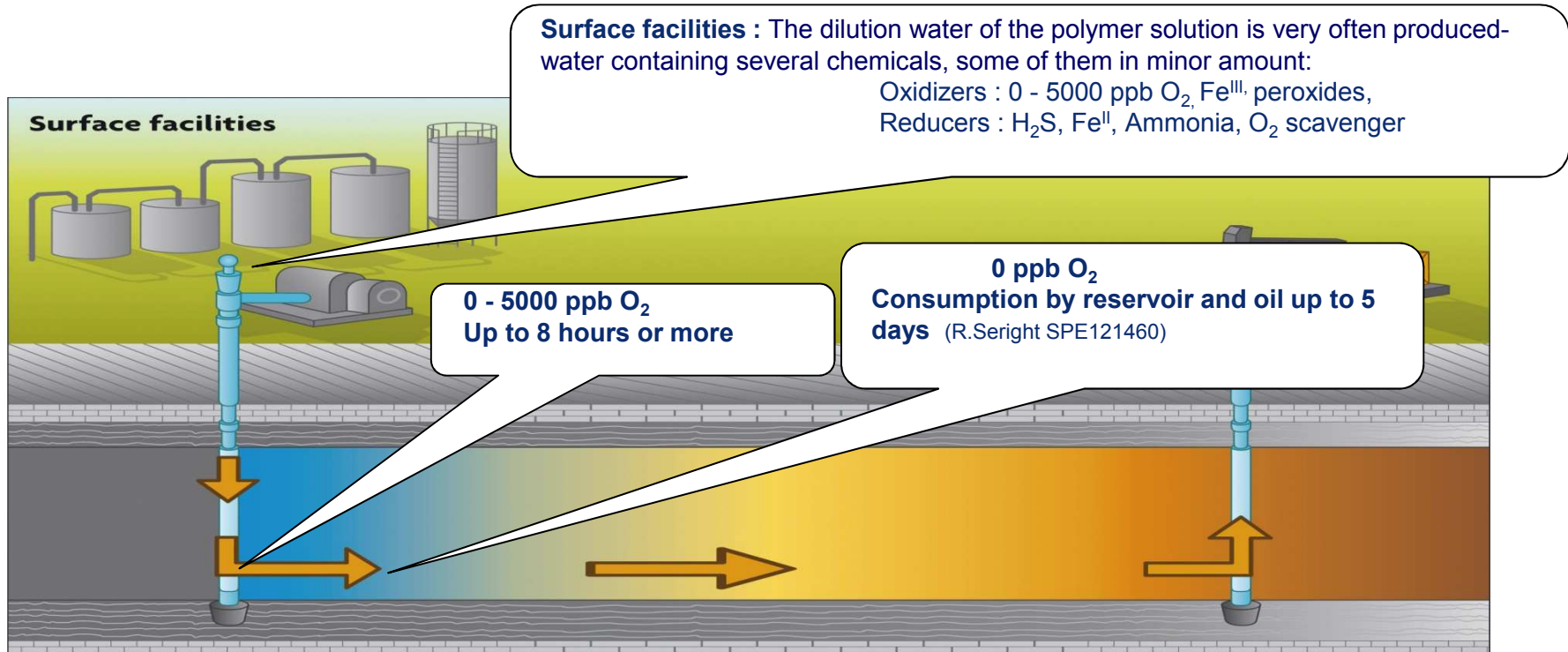
Optimisation of the perforation : use high density shots per meter (20 to 40)



Conclusions

- Chemical degradation and mechanical degradation can be largely minimized
 - Mechanical degradation does not add up
- Choke remains the biggest problem , and if possible should be placed before the introduction of polyme solution
- Surface equipments needs to be design according guidelines such as :
 - Piping : Maximum speed of 2 m/s
 - Agitator : Maximum speed of impellers of 1.5 m/s
 - Triplex pumps : Maximum speed of non-return valves of 3 m/s
 - Choke : Limited diameter pipe before the choke ; Choke with one orifice only
 - Low shear valves

What is the real viscosity in the reservoir ?



Thank you